

LA-6250

0.3

CIC-14 REPORT COLLECTION
**REPRODUCTION
COPY**

UC-45

Issued: December 1976


**The MES Code: Chemical-Equilibrium
Detonation-Product States of Condensed Explosives**

by

Wildon Fickett



los alamos
scientific laboratory
of the University of California
LOS ALAMOS, NEW MEXICO 87545



An Affirmative Action/Equal Opportunity Employer

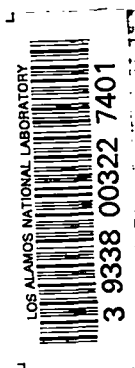
UNITED STATES
ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION
CONTRACT W-7405-ENG. 36

Printed in the United States of America. Available from
National Technical Information Service
U.S. Department of Commerce
5285 Port Royal Road
Springfield, VA 22161
Price: Printed Copy \$6.00 Microfiche \$3.00

This report was prepared as an account of work sponsored by the United States Government. Neither the United States nor the United States Energy Research and Development Administration, nor any of their employees, nor any of their contractors, subcontractors, or their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights.

CONTENTS

Units and Energy Zero	iv
Terms	iv
Symbols	v
I. INTRODUCTION	1
II. INPUT	2
III. OVERVIEW	7
A. State Point	7
B. Components of the State-Point Calculation	8
1. Ideal Thermodynamic Functions	8
2. Solid Equation of State	8
3. Gas Equation of State	10
4. Mixture	11
5. Chemical Equilibrium	11
6. Derivatives	13
C. Controls for Particular Loci	13
1. Contours of Constant T , v , s , or e	13
2. Detonation Hugoniot	14
3. Chapman-Jouguet Locus	14
IV. EQUATIONS	14
A. Ideal Thermodynamic Functions	14
B. Solid Equation of State	16
C. Gas Equation of State	19
1. Ideal Gas	19
2. LJD (Lennard-Jones-Devonshire Cell Theory)	19
3. KW (Kistiakowsky-Wilson)	26
D. Mixture	27
1. Ideal Mixing	27
2. LH Mixing	27
3. CS Mixing	28
4. One-Fluid Mixing	29
E. Chemical Equilibrium	30
1. Initial Calculation	30
2. Main Calculation	32
F. Miscellaneous	34
V. PROGRAM	35
A. Equilibrium Iteration	35
B. Iterations	38



CONTENTS (contd)

C. LJD Gas EOS Integration	40
D. FROOT-Solve $f(x) = 0$ by Iteration	41
VI. SAMPLE INPUT/OUTPUT AND TEST	45
APPENDIX: A. CHEMICAL EQUILIBRIUM EXAMPLE	54
B. QUASI-STATIC WORK	56
C. PROGRAM	59
D. COMMON STORE	117

Units and Energy Zero

The primary units are centimeters, grams, microseconds, K (pressure in Mbar, specific energy in Mbar - cm³/g), but the mole and the system mass M_0 (specified by the user) are also used as the mass unit. The energy unit kcal, prevalent in the literature at the time the code was made, is used for a few input and output quantities.

Energies are relative to elements in their standard states (as defined by the NBS) at $T = 0$. For elements which are gaseous under ordinary conditions, such as oxygen, the typical standard state is the molecular form (O_2) in the hypothetical ideal gas state at a pressure of one atmosphere. For elements which are solid under ordinary conditions, such as carbon, the typical standard state is the most common crystalline form (graphite) at zero pressure.

Terms

- Contour - Locus of constant T , e , v , or s
- CJ - Chapman-Jouguet
- CS - Conformal-solution mixture rule
- EOS - Equation of state
- Ideal (part) - Translation plus internal part of the EOS
(Secs. III.B and IV.C)
- Imperfection (part) - Configurational part of the EOS (Secs.
III.B and IV.C)
- KW - Kistiakowsky-Wilson (EOS)
- LJD - Lennard-Jones-Devonshire (EOS)
- LH - Longuet-Higgins mixture rule
- Lattice (in LJD) - The cold ($T = 0$) state with all molecules
fixed on their lattice sites
- NBS - National Bureau of Standards
- Pure-Fluid - Pure species (gas EOS)
- Unreacted Material - The unreacted (in general metastable,
as in an explosive) material in the
initial state (p_0, T_0)

Symbols

Intensive thermodynamic functions

p, T, μ - pressure, temperature, chemical potential

Extensive thermodynamic functions

$V, E, H, A, F, S, C_p, C_v$ - molar volume, internal energy, enthalpy, Helmholtz free energy, Gibbs free energy, entropy, constant-pressure and constant-volume heat capacities

$v, e, h, a, f, s, c_p, c_v$ - corresponding specific quantities (per unit mass) [equal to (n/M_0) times molar]

Composition

n - total number of moles per M_0 grams of system

n_g - number of moles of gas per M_0 grams of system

n_s - number of moles of solid per M_0 grams of system

n_i - number of moles of species i per M_0 grams of system

x_i - mole fraction of species i in the gas phase = n_i/n_g

x_s - n_s/n

Intermolecular potential

r^*, T^* - minimum-energy radius and well depth

$V^* = (N/\sqrt{2})(r^*)^3$ - molar volume of fcc lattice with molecules at distance r^*

n, m - repulsive and attractive indices

Chemical equilibrium calculation

c - number of elements

s - number of species

Q - empirical-formula coefficients

α - species-formulae coefficients

a - renumberings

\hat{s} - supersaturation index

Other

D - detonation velocity

Δ - ΔH_f (NBS)

Symbols (cont)

Other (cont)

\tilde{F} - "free energy" for equilibrium constants; solid: $\tilde{F}_s = F_s$;
gas: $F_i = \mu_i - RT \ln x_i$ (Sec. IV.E)

γ - $(-\partial \ln p / \partial \ln v)_s$ - adiabatic exponent

Γ - $v(\partial p / \partial e)_v$ - Grüneisen coefficient

\hat{H} - $[H^0(T) - H^0_0]$ (NBS)

M_0 - system mass

N - Avogadro's number

q - heat of reaction, Sec. IV.F

R - molar gas constant

ρ - density

Σ - sum over all species

Σ_g - sum over gas species

u - particle velocity

z - pV/RT

Superscript or over

i - ideal

' - imperfection

* - NBS tabular function (translation plus internal)

- - average

\sim - (1) function (as distinguished from a variable) e.g. $\tilde{p}(T,v)$,
used only when needed to make this distinction

(2) decoration, as in \tilde{F}

Subscript or under

i - species index

o - unreacted material in the initial state

g - gas

s - solid

λ - lattice (cold curve) function for the LJD EOS

H - Hugoniot

other subscripts - partial derivative

$\vec{\quad}$ - vector

$\underline{\quad}$ - matrix

THE MES CODE: CHEMICAL-EQUILIBRIUM
DETONATION-PRODUCT STATES OF CONDENSED EXPLOSIVES

by

Wildon Fickett

ABSTRACT

The MES code calculates states of the reaction products of detonation in gaseous or condensed explosives under the assumption of thermal and chemical equilibrium. The products may consist of any number of gaseous species and one solid species. The condition of equilibrium includes the number of phases: the solid may or may not be present depending on the current state. In addition to the primary calculation of the Chapman-Jouguet state at a specified set of initial densities, the detonation Hugoniot, and contours of constant temperature, density, energy, or entropy, each at a specified set of pressures may be obtained. All of the first derivatives (e.g., sound speed and heat capacity) are calculated at each point.

The solid equation of state is one constructed from a given shock Hugoniot under the assumption of constant Gruneisen coefficient. For the gas, either the ideal gas, the Kistiakowsky-Wilson, or the LJD (Lennard-Jones-Devonshire cell theory) equation of state may be used. Several choices of "mixture rules" for extending the last one, a pure-fluid equation of state, to mixtures are offered. For LJD, the input data are the parameters defining the intermolecular potentials of the species.

I. INTRODUCTION

The MES code, which performs the calculations described in Refs. 1 and 2, was made some years ago, became dormant when the IBM 7094 became obsolete, and has just been reactivated "as is" in response to a request. I make no apology for things I would now do differently. The only significant changes made in the code are: (1) the replacement of the original machine-language equilibrium routine with an equivalent FORTRAN version, (2) the replacement of several relatively small machine-language I/O routines by approximately equivalent FORTRAN versions, and (3) a new scheme of diagnostic printing.

II. INPUT

The data are entered in packs, each pack preceeded by a CON card. The CON cards have 2A6 format; only the first two fields are data; the user may enter comments on the rest of the card. The first two fields, each left justified, are the word CON and the pack name. Each pack consists of one or more strings, numbered sequentially in the write-up; each string consists of one or more cards. Strings are described by listing their fields; alphameric items are underlined. A few strings, such as the table of initial densities for the CJ locus, and initial pressures for the Hugoniot and contours, are of indefinite length; these must be terminated by a zero. Most of the formats are 6E12.7. A few are 12I6 or 12A6; these are marked (I) or (A).

Data for a job (a batch-type submission) are divided into runs. Each run begins with a CON, PAS card and ends with a CON, REND card. The job ends with a CON, JEND card following the last CON, REND. Each run has two parts. Part 1 (preliminary), beginning with CON, PAS, generally enters parameters of the constitutive relations. In Part 2, beginning with the first CON, SAM card, the packs CJ, TED, and PV each specify a complete calculation to be performed immediately after the pack is read; the user may often want to have more than one of these packs within a run, as well as additional SAM packs. With a few obvious exceptions, the packs of either part may be entered in any order.

The input program reads one pack at a time. It expects to find a fixed number of strings in each pack (even though, under some options, not all of them are used). If the first card of a pack is not a CON card (usually because the user has gotten the wrong number of strings in the previous pack), the program reports an error and skips to the next CON, PAS card and begins reading there. In describing the input data, the phrase "not used" means that the data of the field or string in question is not used by the program under the specified conditions. It will, nevertheless, be read by the program; the user may enter anything, but a blank field(s) is suggested. The only exception is that if an entire pack is not used, it may be omitted.

•Remarks

1. Alphameric constants in the input are given in caps, underlined.
2. Except for the equilibrium calculation, which has its own special order, the first slot of all composition arrays is the number of moles of solid.
3. There are no prestored defaults. Many standard values must be supplied by the user under CON, FOB; the standard pack is given in the sample input,

Sec. VI. CON, SWIT, q.v., does have a mechanism for preserving previously entered items when it reappears.

A. Part 1

•CON, PAS, run label - begin Part 1. The run label becomes part of the standard output header.

•CON, blank, comment.

•CON, SWIT - switches.

(I) diff, fix diff, gas, solid, mix, eq, CJ, PV, PVC.

diff	- 0 - no action
	1 - calculate equilibrium-composition derivatives at each point
fix diff	- 0 - no action
	1 - fixed-composition derivatives similarly
gas	- 0 - ideal-gas EOS
	1 - LJD EOS
	9 - KW EOS
solid	- 0 - incompressible
	1 - Grüneisen EOS
mix	- 0 - none (pure fluid); omit <u>XIP</u> pack
	1 - ideal mixing
	2 - LH mixing
	3 - CS (conformal solution) mixing
	4 - One-Fluid mixing
eq	- 0 - fixed composition
	1 - equilibrium composition
CJ	- 0 - equilibrium CJ condition
	1 - frozen CJ condition
PV	- 1, 2, 3, 4 for T, v, s, e constant on contours (see <u>CON</u> , <u>PV</u>)
PVC	- 0 - no action
	1 - under <u>CON</u> , <u>PV</u> , use last T, p from previous calculation instead of input T_C , p_C

Two of the switches are set (or reset) elsewhere: the mix switch under CON, XIP and the PVC switch under CON, PV.

This pack may also be entered one or more times in Part 2 to change switch settings between calculations. A negative item means: "don't store this item" [use currently stored (last previously entered)] value.

•CON, TIP - ideal thermodynamic functions

1. (I) number of species, degree of fit n.
2. T_{\min} , T_{\max} .
3. a_0 , a_1 , a_2 , ..., a_n , d, ΔH_f^0 , $\Delta H_f(T_0)$, $[H_0(T_0) - H_0^0]/RT_0$.

Polynomial fit coefficients for $[H^0(T) - H_0^0]/RT$, enthalpy integration constant d, heats of formation, and enthalpy at T_0 . One such string for each species.

•CON, SEP - solid EOS

1. Γ , C_p/R , α , V_0 , T_0 , E_0/RT_0 .
Grüneisen coefficient, heat capacity, thermal-expansion coefficient (K^{-1}), initial volume ($cm^3/mole$), initial temperature (K), initial energy. For incompressible solid, only V_0 is used.
2. blank, c_0 , c_1 , c_2 , c_3 , c_4 .
Hugoniot fit coefficients:
$$P_H(v) = \sum_{i=0}^4 c_i (v/v_0)^i$$

•CON, GEP - gas EOS (omit pack for ideal gas), LJD EOS

1. (I) potential index (1, 2, 3 for LJ, MCM, MR).
2. n, m, A_n , A_m , r^* , T^* .
repulsive/attractive exponents, multipliers, well radius r^* ($\text{\AA} = 10^{-10}m$), well depth T^* (K); r^* and T^* not used for a mixture.

•KW EOS

1. (I) 9.
2. α , β , θ .

•CON, XIP - Mixture (omit if SWIT mix = 0), LJD EOS

1. (I) number of (gas) species, type.
type - 1, 2, 3, 4 for ideal, LH, CS, One-Fluid;
2. s_r , s_T , r_r^* , T_r^* , n, m.
 s_r , s_T - scale factors: multiply all input r^* by s_r and all input T^* by s_T .
 r_r^* , T_r^* - reference r^* , T^* (LH only).
n, m - potential n and m (One-Fluid only); ordinarily same as n, m in
CON, GEP [omit if SWIT gas = 0 (ideal gas)]
3. μ^* - one for each (gas) species.
4. $\bar{\mu}^*$ - one for each (gas) species.

•KW EOS

1. (I) 9.

2. s_r^* , κ .

3. k .

Here $k_i \equiv [r_i^*/(N/\sqrt{2})]^{1/3}$, where k_i is the usual KW covolume and N is Avogadro's number.

4. blank.

•CON, EQP - equilibrium (omit pack for fixed composition)

1. (I) c, s, p, ϕ , p' .

c - number of elements

s - number of species

p - number of phases minus 1; used only if $\phi = 0$

p' - first guess for p when $\phi = 1$

$\phi = 0$: fixed number of phases (p + 1)

1: equilibrium number of phases (one or two);

2. Q - system empirical-formula coefficients (number of gram-atoms of each element).

3. (A) blank, element symbols, A1, A0.

A print label; all fields right-justified.

4. α - species-formulae coefficients.

This consists of s strings, one for each species, so that each string is a row of α . The first field, format A6, is the right-justified element symbol, and the remaining fields, format I6, are the coefficients. (For example, with elements C, H, O, and N, the string for carbon dioxide is: C02, 1, 0, 2, 0).

5. (I) a^1 - species renumbering for two-phase system ($\phi=1$) or given system ($\phi=0$).

6. (I) a^0 - species renumbering for one-phase system ($\phi=1$); not used for $\phi=0$.

Dimensions are all fixed once c and s are given:

$$Q(c), \alpha(s \times c), a^1(c), a^0(c).$$

In α the species may be listed in any order. The a 's specify renumberings. If k is the number of a species as originally entered in α , then its new number is a_k . The a_k must be chosen so that after renumbering the following conditions are satisfied: the formula coefficients of the first c species must be linearly

independent; the danger of convergence failure will be minimized by choosing for them those species expected to be present in largest amounts. Two special requirements simplify the program: For $\phi=0$, $p=1$ (two phases), the solid species must be number c. For $\phi=1$, the user must supply two possible systems: Two phase (solid present) and one phase (solid absent); the program chooses the correct one at each T and p. For the two-phase system the solid must be number c. For the one-phase system it must be (nominally) present as number s; here the program assigns it a large free energy so that its calculated mole fraction is negligibly small.

For details and examples see Secs. IV.E and VI, and Appendix A.

•CON, FOB - knobs

1. FROOT ϵ 's.
2. FROOT r 's.
3. $1/2 \Delta \ln p$, $1/2 \Delta T$, ϵ_{outer} , ϵ_{inner} .
4. FROOT bounds.

The FROOT items are in the order given in Sec. V.B, Table III; the bounds are in pairs (min, max). The Δ 's are the displacements for the numerical differentiation, Sec. II.B. The ϵ 's in string 3 are for the outer and inner equilibrium iterations, Sec. V.A.

•CON, DEBUG - print store

Do the standard error print (mainly the entire common store) at this point.

B. Part 2

•CON, SAM, material label - initial state and begin Part 2

1. ρ_0 (g/cm³), p_0 (Mbar), T_0 (K), M_0 (g), $\Delta H_f(T_0)$ (kcal/mol).
 M_0 - system mass; must agree with empirical formula under CON, EQP.
 $\Delta H_f(T_0)$ - enthalpy of formation of unreacted material at p_0 , T_0 relative to elements in standard states at T_0 .
2. n - number of moles of each species (for system of M_0 grams). First field is for solid. For equilibrium composition, these are guesses for the first iteration.

We have picked T_0 for the heat of formation because $\Delta H_f(T_0)$ is the quantity usually listed for explosives, and because it is needed for the calculation of the heat of reaction q as usually defined (Sec. IV.F). An alternative, which may be more convenient for some cryogenic materials, is to enter in place of $\Delta H_f(T_0)$ the enthalpy of formation at T_0 from elements at $T=0$. If this is done, the CON, TIP input must also be changed by entering ΔH_f^0 in place of $\Delta H_f(T_0)$ and setting

$[H^0(T_0) - H_0^0]/RT_0$ for each species to zero. This has the advantage of making the TIP input simpler and independent of T_0 . The disadvantage is that the value of q printed out will have a small error (which does not affect on any other calculated quantity).

•CON, TED - detonation Hugoniot at given p
 p - pressure table.

•CON, PV - contour of constant T , v , s , or e at given p

1. (I) k , PVC.

k - 1, 2, 3, 4 for constant - T , v , s , e

PVC - PVC switch (see CON, SWIT)

2. T_c , p_c - initial point (not used if $PVC \neq 0$).

3. p - pressure table.

First calculate the point (T_c, p_c) , then use the value of T , v , s , or e from this point as the constant value for the locus. Use T and p from last previously calculated point for T_c , p_c instead of input values if $PVC \neq 0$.

•CON, CJ - CJ locus at given ρ_0
 ρ_0 - initial-density table.

•CON, REND - end of run

•CON, JEND - end of job

III. OVERVIEW

In this section we give an overview of the problem and program, including the principal equations. Some of these equations are schematic or just serve as definitions; Sec. IV gives the detailed equations implemented by the program. Section V, together with comments in the program, provides a more detailed description of the program itself.

We define the term state point and some related symbols in Sec. A, the main components of the state-point calculation in Sec. B, and the higher level part of the program which uses the state-point calculation in Sec. C. Principal routine names are given in parentheses with some of the section headings.

A. State Point (MES)

A state point is the usual set of thermodynamic variables V , E , H , A , F , S , and some of their derivatives, the chemical potentials μ_i , the mole fractions x_i , and the total number of moles n (per system mass M_0) at given T and p . Recall that we have at most one solid species, and the convention that it is the first listed.

The mole numbers and mole fractions are given by (see symbol sheet)

$$n = \sum n_i = n_s + n_g$$

$$n_g = \sum_g n_i$$

$$x_1 \equiv x_s = n_s/n$$

$$x_g = n_g/n$$

$$x_i = n_i/n_g, \quad i > 1 (\text{gas}) \quad .$$

Note that $x_i, i > 1$ is the mole fraction in the gas phase. The composition may be either fixed (specified) or equilibrium (recalculated at each state point).

Because the equations defining the equilibrium state are implicit and complicated, we obtain derivatives by numerical centered differencing over carefully chosen intervals, rather than attempting to use the very lengthy analytic expressions.

Routine MES calculates a state point at given T and p, using the five packages whose generic names are given in the subheadings of the next section. These packages constitute the bulk of the program.

B. Components of the State-Point Calculation

An extensive quantity for the system is the linear mole fraction sum of those for the two phases, e.g.,

$$E = x_s E_s + x_g E_g \quad .$$

It is convenient to separate functions like E_g and E_s into ideal and imperfection parts. The ideal part, superscript i, represents translation plus the internal partition function; the imperfection part, denoted by a prime, represents the configuration integral.

Descriptions of the five main components of the EOS calculation follow.

1. Ideal Thermodynamic Functions (TIM). We use superscript * to denote the portion of the ideal part that represents the internal partition function; most of the work is in getting this number (for the solid it is the whole value). These functions are tabulated by the NBS and others; they are represented to the program by polynomial fits. The tabulations refer each species to itself at $T = 0$. The program adds the heats of formation at $T = 0$ to refer all to the same reference, namely elements in their standard states at $T = 0$. The physical state corresponding to the tabulation is the given T and $p = p^*$ (1 atm for a gas and zero for a solid), with the stipulation that a gaseous species is in the hypothetical ideal-gas state at T and p^* . For the gas phase, we define the ideal part as that for an ideal gas at the same T , p , and x , so that

$$E^i(T, p, x) = \sum_g x_i E_i^*(T) ,$$

$$S^i(T, p, x) = \sum_g x_i S_i^*(T) - R \ln p/p^* + R \sum_g x_i \ln x_i , \text{ and}$$

$$\mu_i^i(T, p, x_i) = F_i^*(T) + RT \ln p/p^* + RT \ln x_i .$$

2. Solid Equation of State (SEM). For the extensive thermodynamic functions we have

$$E(T, p) = E^i(T, p = 0) + E'(T, p) , \text{ etc.}$$

With the equation of state in the often-used form $p(T, V)$, the imperfection quantities may be defined as the integrals along the isotherm:

$$E'(T, p) = \int_{V(T, p=0)}^{V(T, p)} (T p_T - p) dV ,$$

$$S'(T, p) = \int_{V(T, p=0)}^{V(T, p)} p_T dV , \text{ and}$$

$$\mu' (T, p) \equiv F' = E' + pV - TS' .$$

The EOS used takes the form of equations for T and p along an isentrope through an unknown point T_1, V_1 on $p = 0$, and incorporates simple approximations to the ideal functions on $p = 0$. The equations can be put into a form such that for given T and p the point T_1, V_1 at the foot of the isentrope can be eliminated and the complete EOS at T, p can be obtained by iterative solution of one equation in one unknown. After this is done, the approximate ideal part is subtracted to give the imperfection part (with the correct ideal part, calculated by TIM, added later).

3. Gas Equation of State (GEM). Here we have

$$E (T, p, x) = E^i (T, p, x) + E' (T, p, x) , \text{ etc.}$$

For the usual form $p(T, V)$ the imperfection functions are given by the integrals along the constant-composition isotherm

$$E' (T, p, x) = \int_{RT/p^*}^{V(p, T)} (T p_T - p) dV \text{ and}$$

$$S' (T, p, x) = \int_{RT/p^*}^{V(p, T)} (p_T - R/V) dV ,$$

in which the term R/V in the second integral subtracts off the ideal gas part. Also

$$H' = E' + (z-1) ,$$

$$A' = E' - T S' , \text{ and}$$

$$F' = H' - T S' ,$$

For the chemical potentials we have

$$\mu_i' = (n F')_{n_i} \Big|_{n=1} ,$$

where the partial derivative is at constant T , p , and n_j , $j \neq i$, of the gas phase.

Both of our imperfect-gas equations of state, the LJD and the KW, have the form $p(T, V, x)$, and are not explicitly invertible to $V(T, p, x)$. At given T , p , x we must then first solve the equation

$$\tilde{p}(T, V, x) = p$$

(where \tilde{p} on the left distinguishes the pressure function from the given value of pressure on the right) for V and then calculate the imperfection functions at the given T and this V .

The KW EOS is a simple one, and includes the composition dependence. The LJD EOS is much more complicated, requiring for its calculation the numerical evaluation of several definite integrals. In its original form it applies to only a single, pure species. Here it is extended to apply to the gas mixture through one of several mixture rules, described next.

4. Mixture (XIM). The program offers several options for describing the gas mixture. The first is the general one of ideal mixing, for which each mixture property is a linear mole-fraction sum of those of the individual species

$$E'(T, p, x) = \sum_g x_j E_j'(T, p) , \text{ etc.}$$

This may, of course, be applied to any (pure-species) EOS.

The other mixture rules assume that the pure-species EOS is based on an intermolecular potential function and express the mixture properties as expansions in the potential functions or potential-function parameters of the individual species. In some cases the outcome of this expansion is that the mixture is represented by a fictitious fluid with a certain mean potential whose parameters depend on the composition.

5. Chemical Equilibrium (EQM). The composition of the system can be expressed in terms of the progress variables of J independent reactions (ordinarily

J is the number of species minus the number of elements). We symbolize these reactions by

$$\sum_i v_{ij} X_i = 0, \quad j = 1, \dots, J,$$

where X_i represents one mole of species i , so that v_{ij} is the (molar) stoichiometric coefficient of species i in reaction j . The equilibrium composition is the solution of

$$\sum_i x_i \alpha_{ik} = Q_k \quad k = 1, \dots, k$$

$$\sum_i v_{ij} \mu_i (T, p, n_j) = 0 \quad j = 1, \dots, J$$

with the α_{ik} , the chemical formula coefficients (number of moles of element k in one mole of species i), and the Q_k , the empirical-formula coefficients of the system (total number of moles of element k in the system; total of k elements). The first set of equations represents mass conservation, one equation for each element; the second represents the usual "equilibrium-constant" relations for the reactions. The second equations are put in the form

$$\sum_i v_{ij} \ln x_i = - \sum_i v_{ij} \tilde{F}_i (T, p, \underline{x})/RT, \quad j = 1, \dots, J$$

with \tilde{F}_i defined as

$$\tilde{F}_i = \mu_i - RT \ln x_i \quad \text{for a gas species and}$$

$$\tilde{F}_i = \mu_i = F_s \quad \text{for the solid.}$$

The advantage of this procedure is that, for the ideal gas, the \tilde{F}_i are independent of x , so the x -dependence is confined to the $\ln x_i$ terms. For the real gas the \tilde{F}_i

do depend on \underline{x} , but this dependence is small enough so that the equations can be solved by a direct iteration method based on a procedure that solves the ideal-gas problem: Guess \underline{x} , calculate \tilde{F}_i for this \underline{x} , find the ideal gas x for the \tilde{F}_i fixed at this value, recalculate the \tilde{F}_i from the new \underline{x} , and repeat to convergence.

6. Derivatives (GAMM). The first partial derivatives (for the complete system) are calculated by centered difference from symmetrical displacements in $\ln p$ and T of carefully chosen size. Three derivatives are approximated by centered differences

$$c_p \equiv (\partial h / \partial T)_p = \Delta h / \Delta T \quad ,$$

$$(\partial \ln p / \partial \ln v)_T = \Delta \ln p / \Delta \ln v \quad ,$$

$$(\partial \ln v / \partial T)_p = \Delta \ln v / \Delta T \quad ,$$

where Δ denotes a difference between the two symmetrically displaced points in p or T . The remaining derivatives are then obtained from these

$$c_p / c_v = 1 + (pv / c_p T) (-\partial \ln p / \partial \ln v)_T [T(\partial \ln v / \partial T)_p]^2 \quad ,$$

$$\gamma = (c_p / c_v) (-\partial \ln p / \partial \ln v)_T \quad , \text{ and}$$

$$\Gamma = \gamma (pv / c_p T) T (\partial \ln v / \partial T)_p \quad .$$

C. Controls for Particular Loci

The rest of the program uses the (T, p) state-point routine (MES) to calculate points on various thermodynamic loci. The routines are given in the section titles.

1. Contours of Constant $T, v, s,$ or e (PV, MESC). The locus is specified by a given value of the desired variable. Thus for constant e , for example, it is the solution of

$$\tilde{e}(T, p) = e_c \quad ,$$

with e_c the given value of e , specified either as the values of T_c and p_c at which the program is to calculate e_c , or taken from a previously calculated point. Under control of PV, the program calculates points on the locus for each of the set of specified values of p , using MESC to calculate each point.

2. Detonation Hugoniot (TED, HUG). This procedure works the same way, with TED the control and HUG the Hugoniot-point calculator. In this case the equation solved is the Hugoniot equation

$$h - h_0 = \frac{1}{2} (p - p_0) (v_0 - v) .$$

3. Chapman-Jouget Locus (CJ). A CJ point is located by iterative solution of a form of the CJ condition

$$u + c = D ,$$

with u and D given by the shock conservation relations, over a set of points on the Hugoniot, with each Hugoniot point calculated by HUG. The CJ points are determined for the specified set of initial densities.

IV. EQUATIONS

In this section we give the remaining equations in essentially the form used by the program.

A. Ideal Thermodynamic Functions (TIM)

The system is defined by a matrix of constants, one row for each species. Each row contains

$$a_0, a_1, \dots, a_h, d, \Delta^0, \Delta(T_0), \hat{H}(T_0)/RT_0 .$$

Here we have defined, in terms of the NBS notation

$$\Delta^0 = \Delta H_f^0 = \Delta H_f(0), \quad \Delta(T_0) = \Delta H_f(T_0) ,$$

$$\hat{H}(T) = H^0(T) - H_0^0 ,$$

where ΔH_f^0 and $\Delta H_f(T)$ are the heats of formation from the elements in their standard states at $T = 0$ and $T = T$. The standard state is defined as the standard form at the temperature of interest and pressure p^* (1 atm for a gas, 0 atm for a solid), with a gaseous form in the hypothetical ideal gas state. For elements carbon, hydrogen, oxygen, and nitrogen (CHON), the standard forms are solid graphite, and gaseous H_2 , O_2 , and N_2 , respectively. The symbol $H^0(T) - H_0^0$ denotes the enthalpy at T relative to that of the same substance at $T = 0$. The constants a_0 through a_n are the coefficients of a polynomial fit of degree n to $\hat{H}(T)/RT$, and d is the integration constant for the entropy. Recalling our convention that the solid always be species 1, we define

$$\delta_{i1} = 0 \quad \text{if } i \neq 1 \text{ and}$$

$$\delta_{i1} = 1 \quad \text{if } i = 1 \text{ .}$$

With i the row (species) index, and j the column index, we have

$$H_i^*/RT = \sum_{j=0}^n a_{ij} T^j + \Delta_i^0/RT \quad ,$$

$$G_i^*/RT = \sum_{j=0}^n (j + 1) a_{ij} T^j \quad ,$$

$$S_i^*/R = a_{i0} \ln T + \sum_{j=1}^n [(j + 1)/j] a_{ij} T^j + d_i - (\delta_{i1} - 1) \ln p/p^* \quad , \text{ and}$$

$$F_i^*/RT = H_i^*/RT - S_i^*/R \quad .$$

All these quantities are relative to elements at $T = 0^\dagger$ (entropy at this temperature is zero for all species).

The ideal functions for the gas mixture are then

$$H_g^i/RT = \sum_g x_i H_i^*/RT$$

$$S_g^i/R = \sum_g x_i S_i^*/R - \sum_g x_i \ln x_i, \text{ etc.}$$

The mixture heat of formation from elements at T_0 is

$$\Delta_g(T_0) = \sum_g x_i \Delta_i(T_0) .$$

The total free energy of the gas is not needed, but the F_i^* of the individual species are used in calculating those F_i that determine the equilibrium composition.

The program uses the fits only over the range of T_{\min} to T_{\max} from the input. Outside this range, the results are an extrapolation using the assumption that the heat capacity is constant at its boundary value.

B. Solid Equation of State (SEM)

The solid EOS is constructed from a reference curve and the assumption of a constant Grüneisen coefficient to get off the curve. Defining $y = V/V_0$ (with V_0 here the normal volume of the solid at $p = 0$), the reference curve (see Fig. 1) is the shock Hugoniot $p_H(y)$ for $y \leq 1$ and the $p = 0$ line for $y > 1$. We assume a simple form for the ideal functions on $p = 0$, use it to calculate the complete

[†]The Hugoniot calculation uses the enthalpy relative to elements at T ; with this reference state indicated by explicit inclusion of the reference temperature T_0 as a parameter (together with argument T), the quantity supplied by TIM for this calculation is

$$H_i^*(T;T_0)/RT = \sum_{j=0}^n a_{ij} T^j - (T_0/T) [\hat{H}_i(T_0)/RT_0] + \Delta_i(T_0)/RT_0 .$$

Note that for the alternate SAM input (Sec.II.B), this becomes identical to H_i^*/RT above, i.e., the reference temperature becomes zero.

EOS, and then subtract it to get the imperfection part. Using superscript I to denote the isentrope through point y_1 on $p = 0$ and superscript o to denote functions on $p = 0$, we have for this isentrope

$$p^I = p^I(y; y_1) \text{ and}$$

$$T^I = T^I[y; y_1, T^0(y_1)] .$$

On the reference curve $p = 0$ we take

$$T^0 = T^0(y) = (y - 1)/\alpha$$

$$E^0 = E^0(T^0) = C_p(T^0 - T_0)$$

with constant heat capacity C_p and thermal expansion coefficient α . With constant Grüneisen coefficient Γ we find

$$E/V_0 = (y/\Gamma) p + g(y) ,$$

$$g(y) = p_H(y) [1/2(1 - y) - y/\Gamma] + E_0 \quad \text{for } y \leq 1, \text{ and}$$

$$g(y) = \alpha^{-1} C_p (y - 1) \quad \text{for } y > 1 .$$

For p^I and T^I we find

$$p^I(y; y_1) = \Gamma y^{-(\Gamma + 1)} \int_{y_1}^y y^{(\Gamma + 1)} g'(y) dy \quad \text{and}$$

$$T^I(y; y_1) = T^0(y_1) (y_1/y)^\Gamma .$$

If we represent the reference Hugoniot by a power series

$$p_H(y) = \sum_{i=0}^n a_i y^i$$

with coefficients chosen such that

$$p_H(1) = \sum_{i=0}^n a_i = 0$$

(to make the result simpler), the integral can be done analytically and we find

$$p^I = p_1(y) = (C_p/\alpha V_0) \left[\Gamma/(\Gamma-1) \right] \left[(y_1/y)^{\Gamma+1} - 1 \right] \quad \text{for } y > 1 ,$$

$$p^I = p_2(y) + p_1(1) \quad \text{for } y \leq 1 ,$$

$$p_2(y) = - (\Gamma/y)g(y) + (\Gamma^2/y^{\Gamma+1}) [I(y) - I(1)] , \text{ and}$$

$$\begin{aligned} I(y) &= \int y^{\Gamma-1} g(y) dy \\ &= \sum_{i=0}^n \left[\frac{1}{2} \left(\frac{a_i}{\Gamma+i} \right) (y^{\Gamma+i-1}) - \left(\frac{1}{2} + \frac{1}{\Gamma} \right) \left(\frac{a_i}{\Gamma+i+1} \right) (y^{\Gamma+i+1-1}) \right] . \end{aligned}$$

To get the EOS for given p and T , we must eliminate (by iterative solution) y_1 from $p^I = p$ and $T^I = T$.

•Computation

Given p , T , the function defining y is

$$T^I(y)/T - 1 = 0 .$$

$T^I(y)$ is calculated (for $y < 1$) by first calculating $p_2(y)$, then solving $p^I(y) = p$ for y_1 to get

$$y_1 = \left[1 + (p - p_2(y))/A \right]^{1/(\Gamma+1)}, \quad A = (C_p/\alpha V_0) \left[\Gamma/(\Gamma+1) \right]$$

and then calculating T^I from the equation above. When y_1 is close to 1 (the usual case) the RHS is expanded in a binomial expansion

$$y_1 = 1 + k x + \frac{1}{2} k (k-1) x^2 + \dots$$

$$k \equiv 1/(\Gamma+1)$$

$$x \equiv \left[p - p_2(y) \right] / A .$$

For $y > 1$, y_1 is

$$y_1 = y (1 + p/A)^{1/(\Gamma+1)},$$

with expansion

$$y_1 = y \left[1 + k x + \frac{1}{2} k (k-1) x^2 + \dots \right]$$

$$x = p/A .$$

C. Gas Equation of State (GES)

1. Ideal Gas. The EOS is

$$V = RT/p ,$$

and the imperfection quantities are all zero.

2. LJD (Lennard-Jones-Devonshire Cell Theory). This EOS is based on an intermolecular potential $u(r)$ (see Fig. 2) with well depth kT^* (k is Boltzmann's constant) and radius r^* . We define a reduced temperature and volume

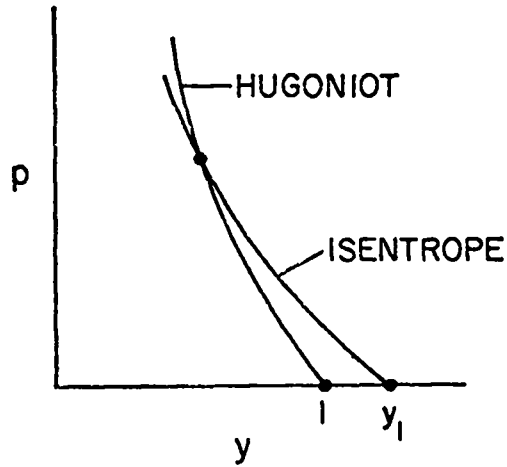


Fig. 1. Solid Hugoniot and isentrope.

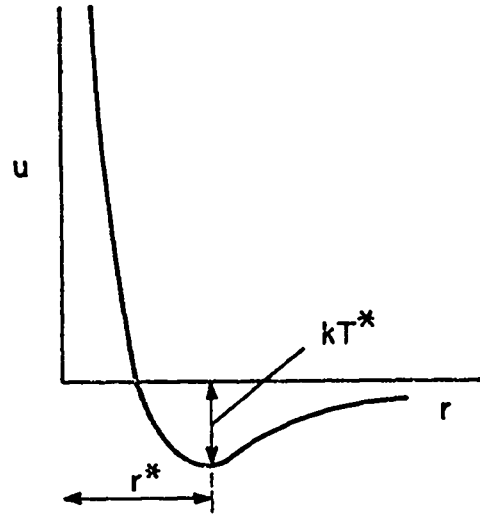


Fig. 2. Intermolecular potential for LJD EOS.

$$\theta = T/T^*, \quad \tau = V/V^*, \quad V^* = 2^{-1/2} N(r^*)^3,$$

with V^* the volume of an fcc lattice with intermolecular separation r^* (N is Avogadro's number). The EOS is a sum of two parts: A lattice ($T = 0$) part, with all molecules fixed on the sites of a regular fcc lattice, and a thermal part, for which the partition function is approximated by a cell integral, in which one molecule moves while all its neighbors remain fixed on their lattice sites.

We first define the lattice and cell-integral functions. We define χ as minus the reduced lattice energy

$$\chi = -\frac{1}{2} Z u(\tau^{1/3} r^*)$$

with Z the coordination number of the lattice for which we use 12, the fcc value. The cell-integral function $G(y)$ is defined as

$$g(y) = \int_0^{b^*} y x^2 e^{-W(\tau, x)/\theta} dx, \quad b^* = 0.55267$$

$$G(y) = g(y)/g(1) .$$

Here the integration variable x is the distance from the cell center in units of the nearest neighbor distance at the given τ , b^* is the distance of the cell boundary from the center, and W is the cell potential relative to its value at the cell center, the potential of a molecule at a given distance from the cell center, in the field of its 12 nearest neighbors smeared into a uniform spherical shell (at the nearest neighbor distance). The cell potential is given by the spherical-smoothing integral

$$W(x, \tau) = \int_{1-x}^{1+x} x' \left[u\left(\tau^{1/3} r^* x'\right) - u\left(\tau^{1/3} r^*\right) \right] dx' .$$

For the two types of potential-function terms we consider (power and exponential) the smoothing integral can be done analytically, but the cell integral cannot.

The cell integrals come from the canonical ensemble, with independent variables T and V . The natural imperfection quantities are thus those relative to ideal gas at the same T and V . Elsewhere, we have used imperfection quantities relative to the ideal gas at the same T and p . The two are the same for all except the entropy and free energies, which are related by

$$S'(T, p)/R = S'(T, V) + \ln z ,$$

$$A'(T, p)/RT = A'(T, V)/RT - \ln z , \text{ and}$$

$$F'(T, p)/RT = F'(T, V)/RT - \ln z ,$$

with the argument p or V denoting imperfection with respect to ideal gas at the same p or V , respectively. In the following, we mark A' with respect to V by argument V (we will refer to it later); all quantities without an argument are with respect to p .

The imperfection thermodynamic functions are

$$z \equiv pV/RT = 1 + \theta^{-1} \left[\tau \chi_{\tau} - G(\tau W_{\tau}) \right] ,$$

$$E'/RT = \theta^{-1} [-\chi + G(W)] ,$$

$$H'/RT = E'/RT + (z-1) ,$$

$$A'(T,V)/RT = 1 - \chi/\theta - \log 2\pi^{1/2} g(1) ,$$

$$A'/RT = A'(T,V)/RT - \ln z ,$$

$$F'/RT = A'/RT + z-1 , \text{ and}$$

$$S'/R = E'/RT - A'/RT .$$

The derivatives, with partials written for $p(T,V)$, $E'(T,V)$ [and $z(\tau,\theta)$, $E'(\tau,\theta)$] are

$$(V/R)p_T = (z\theta)_\theta = 1-\theta^{-2} \left[G(W\tau W_\tau) - G(W) G(\tau W_\tau) \right] ,$$

$$(V^2/RT)p_V = \tau z_\tau - z = \tau(\tau\chi_\tau)_\tau/\theta + \theta^{-2} \left[G^2(\tau W_\tau) g(1) - G^2(\tau W_\tau) - G((\tau W_\tau)_\tau) \right] , \text{ and}$$

$$C'_V/R \equiv R^{-1} E'_T = (E'/RT)_\theta = \theta^{-2} \left[G(W^2) - G^2(W) \right] .$$

The potential functions may be written in the form

$$u(r)/kT^* = (n-m)^{-1} \left[mf(r,n) + nf(r,m) \right]$$

$$f(r,q) = (r^*/r)^q \text{ or } e^{q(1-r/r^*)}, \quad (q = n \text{ or } m) .$$

The three potential forms are

<u>Potential</u>	<u>Repulsive Term</u>	<u>Attractive Term</u>
LJ	power	power
MCM	exponential	exponential
MR	exponential	power

(The symbols α and β have been previously used instead of n and m for the exponential form). To write χ and W , define coefficients a for χ , and b for W for repulsive and attractive terms as follows:

<u>Coefficients</u>		<u>Repulsive</u>	<u>Attractive</u>
a	=	$-1/2 A_n Z_n / (n-m)$	$-1/2 A_m Z_m / (n-m)$
b	=	$Z_n / (n-m)$	$\delta Z_m / (n-m)$
			$\delta = 0, 1 \text{ for } A_m = 0, A_m \neq 0$

Here the constants A_n and A_m are the Madelung lattice constants for a power-law term and may be regarded as an empirical multiplier for an exponential term. They may also be regarded as switches: $A_n \neq 0, A_m = 0$ gives a one-term (repulsive-only) potential. For a power-law term, the proper value of A_n or A_m takes into exact account the contributions of all neighbors for the lattice contribution; to do this for the exponential form a volume-dependent function would be required. For the b -coefficients, used in the cell integrals, only nearest neighbors are considered, so that the A 's do not appear.

The functions χ and W and their derivatives, are, like the potential, a sum of a repulsive and an attractive term. Using the coefficients a and b defined above, we write the expressions for one term for each of the two forms.

a. Power Form.

$$t \equiv \tau^{1/3}$$

$$\chi = at^{-q}$$

$$\tau \chi_\tau = -(q/3) \chi$$

$$\tau(\tau \chi_\tau)_\tau = (q^2/9) \chi$$

$$W = bt^{-q} \rho(x, q)$$

$$\tau W_\tau = -(q/3) W$$

$$\tau(\tau W_\tau)_\tau = (q^2/9) W$$

$$\ell(x, q) = [2(q-2)x]^{-1} [(1-x)^{-(q-2)} - (1+x)^{-(q-2)}]^{-1}$$

$$= \sum_{i=1}^{\infty} c_i x^{2i}$$

$$c_i = (q-2+2i)! / [(q-2)! (2i+1)!]$$

$$c_{i+1} = c_i [(q+2i)(q+2i-1)] / [(2i+3)(2i+2)]$$

The series is used for computation.

b. Exponential Form.

$$s \equiv q\tau^{1/3}$$

$$\chi = a e^{q-s}$$

$$\tau\chi_\tau = -(s/3) \chi$$

$$\tau(\tau\chi_\tau)_\tau = [(s^2-s)/9] \chi$$

$$W = be^{q-s} f_1(s, x)$$

$$\tau W_\tau = (b/3)e^{q-s} f_2(s, x)$$

$$\tau(\tau W_\tau)_\tau = (b/9) e^{q-s} f_3(s, x)$$

where the functions f_1 , f_2 , and f_3 all have the form

$$f_i(s,x) = \alpha_i(s) (sx)^{-1} \sinh(sx) + \beta_i(s) sx \sinh(sx) + \gamma_i(s,x) \cosh(sx) + \delta_i(s)$$

with the coefficients α_i , β_i , γ_i , δ_i given in Table I.

•Computation of the g-integral

The 16-point Gauss method is used:

$$\int_0^{b^*} f(x) dx \cong \frac{1}{2} b^* \sum_{i=1}^{16} a_i f(x_i)$$

$$x_i = \frac{1}{2} b^* (1-y_i) ,$$

where the a_i and y_i are the weights and arguments of the method. These are symmetric about the center of the interval $(0, b^*)$

$$y_1 = y_{16} \cong 0.99$$

⋮

$$y_8 = y_9 \cong 0.1$$

$$a_1 = a_{16} \cong 0.03$$

⋮

$$a_8 = a_9 \cong 0.19 .$$

TABLE I

COEFFICIENTS FOR THE EXPONENTIAL FORM

i	$\alpha_i(s)$	$\beta_i(s)$	$\gamma_i(s,x)$	$\delta_i(s)$
1	$1+s^{-1}$	0	$-s^{-1}$	-1
2	$-(s+2+2s^{-1})$	-1	$2(1+s^{-1})$	s
3	$s^2+2s+4+4s^{-1}$	$2+3s$	$-(3s+4+4s^{-1}+sx^2)$	$s-s^2$

In the region of interest, the integrands often effectively vanish for x significantly less than b^* . The program allows for this by, in effect, choosing the numerically appropriate upper limit each time, as described in Sec. V.C.

3. KW (Kistiakowsky-Wilson). The KW EOS has its own built-in mixture rule in the form of a linear mole-fraction sum of covolumes k_i

$$k = \kappa \sum_g x_i k_i .$$

Its reduced variable x :

$$x = k/V(T+\theta)^\alpha$$

for $\theta = 0$, would be that corresponding to a repulsive-only potential with

$$k \propto (r^*)^3 (T^*)^\alpha .$$

(actually θ is fixed at 400 K). The equations are

$$z \equiv pV/RT = 1 + xe^{\beta x} ,$$

$$E'/RT = [\alpha T/(T+\theta)](z-1) ,$$

$$F'/RT = (e^{\beta x} - 1)/\beta + z - 1 - \ln z , \text{ and}$$

$$\mu'_i/RT = (e^{\beta x} - 1)/\beta - \ln z + (\kappa k_i/k)(z-1) .$$

The derivatives are, with partials of $p(T,V)$ and $E'(T,V)$

$$(V/R)p_T = z - (1+\beta x)E'/RT ,$$

$$(V^2/RT)p_V = - (1+\beta x)(z-1) - z , \text{ and}$$

$$C'_V/R = \{2 - [1+\alpha(1+\beta x)]T/(T+\theta)\}E'/RT .$$

D. Mixture (XIM)

All the following forms except ideal mixing require the intermolecular potential functions for all binary interactions. To get these from the given potentials for each species, we use the combining rules for r^* and T^*

$$r_{ij}^* = \frac{1}{2} (r_i^* + r_j^*) \text{ and}$$

$$T_{ij}^* = (T_i^* T_j^*)^{1/2} ,$$

and assume the same functional form for all (including common values of the repulsive and attractive exponents n and m).

All of the sums in this section, of course, extend only over the gas species.

1. Ideal Mixing. The properties of the mixture are just linear mole fraction sums of the properties of the components, each calculated as a pure fluid at the given T and p . Thus

$$V(T,p) = \sum x_i V_i(T,p) ,$$

and similarly for the other extensive variables. The chemical potential of each component is just equal to its Gibbs free energy at the given T and p

$$\mu_i(T,p)/RT = F_i(T,p)/RT .$$

2. LH Mixing. This is based on an expansion about the properties of a fixed specified reference fluid (subscript r) in powers of $r_i^* - r_r^*$ and $T_i^* - T_r^*$. All the pure species are assumed to be described by the same reduced EOS $p(\tau_i, \theta_i)$, $\tau_i = V/V_i^*$, $\theta = T/T_i^*$. The partial derivatives are those of the reference-fluid functions with T and V as independent variables: $p(T,V)$, $E'(T,V)$. The equations are

$$f = \sum_{j,k} x_j x_k f_{jk}$$

$$g = \sum_{j,k} x_j x_k g_{jk}$$

$$f_{jk} = r_{jk}^*/r_r^*$$

$$g_{jk} = T_{jk}^*/T_r^*$$

$$z = z_r \left\{ 1 - \left[T/V(-p_T/p_V) + (p/V)/p_V \right] (f-1) + 3 \left[1 + (p/V)/p_V \right] (g-1) \right\}_r$$

$$H'/RT = \left\{ H'/RT + \left[E'/RT - C_V/R - R^{-1} (Tp_T - p)(-p_T/p_V) \right] (f-1) \right\}_r$$

$$F'/RT = \left[F'/RT + (E'/RT)(f-1) + 3(z-1)(g-1) \right]_r$$

$$\begin{aligned} \mu_i'/RT = & \left\{ F'/RT + E'/RT \left[2 \left(\sum_j x_j T_j^*/T_r^* - 1 \right) + (f-1) \right] \right. \\ & \left. + 3(z-1) \left[2 \left(\sum_j x_j r_j^*/r_r^* - 1 \right) + (g-1) \right] \right\}_r, \end{aligned}$$

with all of the thermodynamic functions and their derivatives on the right evaluated for the reference fluid at the given T and V .

3. CS Mixing. This is an improvement over the LH form, with a composition-dependent reference fluid chosen to make $f = g = 1$. The same assumptions apply. The reference fluid is defined by

$$r_r^* = \bar{r}^* = \sum_{i,j} x_i x_j r_{ij}^* \quad \text{and}$$

$$T_r^* = \bar{T}^* = \sum_{i,j} x_i x_j T_{ij}^* .$$

The thermodynamic functions are all just those of this reference fluid except for the chemical potentials, which are the same as those for LH but with r_r^* and T_r^* as defined here and $f = g = 1$:

$$\mu_i^*/RT = \left\{ F'/RT + E'/RT \left[(n/\bar{T}^*) \frac{\partial \bar{T}^*}{\partial n_i} \right] + 3(z-1) \left[(n/\bar{r}^*) \frac{\partial \bar{r}^*}{\partial n_i} \right] \right\}_r ,$$

$$n/\bar{T}^* \frac{\partial \bar{T}^*}{\partial n_i} = 2 \left(\sum_j x_j T_{ij}^*/\bar{T}^* - 1 \right) , \text{ and}$$

$$n/\bar{r}^* \frac{\partial \bar{r}^*}{\partial n_i} = 2 \left(\sum_j x_j r_{ij}^*/\bar{r}^* - 1 \right)$$

These partials are at constant n_j , $j \neq i$.

4. One-Fluid Mixing. This is similar to the CS form, except that the expansion variable is taken to be the potential function itself instead of its parameters r_i^* and T_i^* . It yields a tractable result only for a power-law potential. The reference fluid is defined by the mean parameters

$$s_q = \sum_{i,j} x_i x_j T_{ij}^* (r_{ij}^*)^q, \quad q = n \text{ or } m ,$$

$$\bar{r}^* = (s_n/s_m)^{1/(n-m)} , \text{ and}$$

$$\bar{T}^* = s_m^{n/(n-m)} / s_n^{m/(n-m)} .$$

Again the thermodynamic functions are those of the reference fluid. The chemical potentials are those of the CS form but with

$$(n/\bar{T}^*) \frac{\partial \bar{T}^*}{\partial n_i} = \left[2/(n-m) \right] \left(S_{ni}/s_n - S_{mi}/s_m \right) ,$$

$$(n/\bar{r}^*) \frac{\partial \bar{r}^*}{\partial n_i} = \left[2 + 2/(n-m) \right] \left(mS_{ni}/s_n - nS_{mi}/s_m \right) , \text{ and}$$

$$S_{qi} = \sum_j x_j T_{ij}^* (r_{ij}^*)^q , \quad q = n \text{ or } m .$$

E. Chemical Equilibrium

Recall the definitions given in the input description:

- c = number of independent species
- = number of elements
- s = total number of species
- $p+1$ = Number of phases ($p=0$: gas only, $p=1$: gas + solid)
- Q_i = empirical-formula coefficients
- α_i = species-formulae coefficients ,

and that, for a complete equilibrium calculation, the user supplies two possible systems: a one-phase system with the solid only nominally present as species number s , and a two-phase system with the solid present as species number c .

Symbols newly defined here are

- q_i = number of moles of each species for a system prepared from independent species only,
- v_i = stoichiometric (chemical reaction) coefficients of the dependent species (independent species have coefficient 1),
- $$v_k = \sum_{j=1}^{c-p} v_{kj} = \text{change in number of moles of gas in reaction } k,$$
- n^s = number of moles of solid,
- n^g = number of moles of gas,
- x_i = (gas) mole fraction n_i/n^g except $x_c = n^s/n^g$ for solid present, and
- K_k = equilibrium constant for reaction k .

We change to superscript s and g here for solid and gas to avoid confusion with indicial subscripts.

1. Initial Calculation. The initial calculation generates constants for the main calculation. Mathematically, it consists of a change of basis from (moles of) elements to (moles of) independent species. In the new basis each dependent species is expressed as a linear combination of independent species, with coefficients that are just the independent-species stoichiometric (chemical reaction) coefficients for the reaction producing one mole of the given dependent species from the independent ones. The system could, of course, be prepared from q_i moles of each independent species i ($i = 1$ to c) instead of Q_i moles of each element.

We now define some index conventions to simplify writing the equations. Divide the α -matrix into independent (c by c) and dependent (s - c by c) parts. Number the complete columns, and the rows of the independent part, with i or j. Number the rows of the dependent part with k. (See Fig. 3.) The ranges are

i and j: 1 to c

k: c+1 to s,

and denote by Σ_i or Σ_j a sum over i or j from 1 to c and by Σ_k a sum over k from c+1 to s. Then α and ν are solutions of the linear equations

$$\sum_i \alpha_{ij} q_i = Q_j, \quad j = 1 \text{ to } c \text{ and}$$

$$\sum_i \alpha_{ij} \nu_{ki} = \alpha_{kj}, \quad j = 1 \text{ to } c, k = c+1 \text{ to } s.$$

The dimensions of ν are the same as the dependent part of α and we retain the same usage and range of indices for it. (See Fig. 4.)

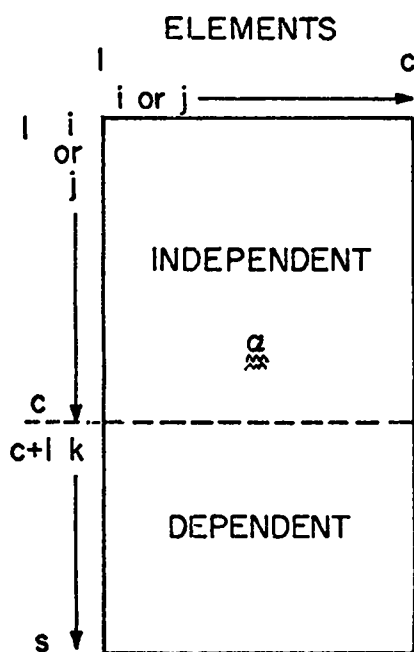


Fig. 3. The α -matrix.

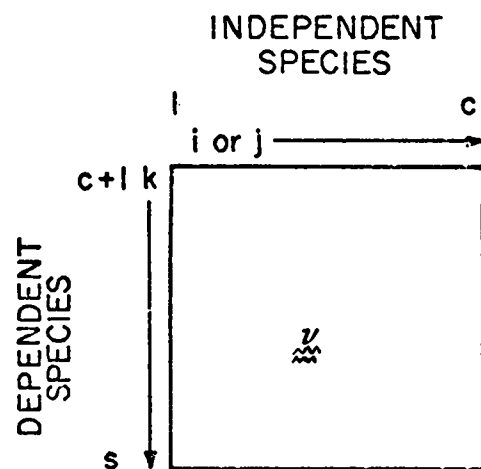


Fig. 4. The ν -matrix.

2. Main Calculation. We retain the above index conventions except that now in all sums except that in the definition of K_k the ranges of i and j are

$$i \text{ and } j: 1 \text{ to } c-p,$$

and we use primes to denote sums or products over this range.

The equations can be reduced to a set of $c-p$ equations in $c-p$ unknowns; the remaining mole fractions are determined in the process of solving these or are calculated afterward. The equations are obtained by expressing the dependent species in terms of the independent ones, writing out the first derivatives, and applying the Newton-Raphson method of iteration. Letting superscript (n) number the iteration step, the result is

$$x_i^{(n+1)} = (1 + h_i^{(n)}) x_i^{(n)}, \quad i = 1 \text{ to } c - p$$

(with super (n) understood in the following equations). The increments $h_j^{(n)}$ are the solutions of the linear set

$$\sum_j' A_{ij} h_j = \tilde{F}_i, \quad i = 1 \text{ to } c - p$$

$$A_{ij} = x_i \delta_{ij} + \sum_k x_k v_{kj} G_{ki}$$

$$F_i = -\bar{q}_i + x_i + \sum_k x_k G_{ki}$$

$$G_{ki} = v_{ki} - (v_k - 1) \bar{q}_i$$

$$v_k = \sum_j' v_{kj}$$

$$\bar{q}_i = q_i / \sum_j' q_j$$

$$x_k = K_k \prod_j x_j^{v_{kj}}$$

$$-\ln K_k = \tilde{F}_k - \sum_j v_{kj} \tilde{F}_j .$$

The first equation is a linear system for the h_j . In the second equation δ_{ij} is the Kronecker delta, the x_i 's are the independent-species mole fractions, and the x_k 's are the dependent-species mole fractions, expressed in terms of the mole fractions of the first $c - p$ species through the next-to-the-last equation, which is just the set of equilibrium-constant relations for the reactions. Finally \bar{q}_i is the normalized q_i and v_k the (gas) mole change in reaction k . The K_k and \bar{q}_i are independent of the x 's and are calculated at the beginning.

The x_k 's, $k = c+1$ to s , are found in the process of solving this system. The number of moles of gas is

$$n^g = \left(\sum_j q_j \right) / \left[1 + \sum_k (v_k - 1) x_k \right] .$$

When the solid is present ($p = 1$) the c th equation is decoupled from the first $c - p$ equations because, although each of the first $c - p$ equations contains in general all of the first $c - p$ x_i (by virtue of the presence of the x_j in the equilibrium-constant relations), none contain x_c (by virtue of its absence from the same). Thus, in this case, only the first $c - p$ equations are solved iteratively, and then x_c is determined from the c th equation evaluated for this solution.

As mentioned earlier, in the complete equilibrium case, when a solid may or may not be present, the program carries two possible systems, one with and one without the solid. It begins by solving the case found to be correct on the previous entry, then tests to see if it has the correct one and switches to the other if necessary. If the two-phase system is solved, the test is the sign of the number of moles of solid; if it is positive, the choice was the correct one. If the one-phase system is solved, the test is as follows. Find the first reaction in the two-phase system that involves the solid. Call this the test reaction. In the two-phase system the mole fractions involved in it would have to

satisfy

$$K_k = x_k / \prod_j x_j^{\nu_{kj}} .$$

(with K and the ν 's, of course, from the two-phase system). Define a saturation index \hat{s} for the test reaction as

$$\hat{s} = (x_k / \prod_j x_j^{\nu_{kj}}) / K_k$$

and evaluate \hat{s} for the x 's (of the species involved) from the one-phase solution. If $\hat{s} < 1$ the system is unsaturated with respect to deposition of solid, and the one-phase choice was the correct one.

F. Miscellaneous

The actual Hugoniot and CJ iteration functions are given in Sec. V.B. (Table III). Note that the Hugoniot function uses enthalpy relative to T_0 and that h_0 is for the unreacted material.[†]

The "heat of reaction" q is defined, for products at given T, p , as the energy released by reaction of the unreacted material in the initial state (T_0, p_0) to products at the same temperature and pressure (but having the composition calculated at the given T, p)

$$Q = [x_g \Delta_g(T_0) + x_s \Delta_s(T_0)]_{\text{products}} - [\Delta(T_0)]_{\text{unreacted}} - RT_0$$

$$q = (n/M_0)Q .$$

The particle velocity u and detonation velocity D are given by

$$u^2 = (p-p_0)(v_0-v)$$

[†]If the alternative procedure (heat of formation at $T = 0$ entered under CON, SAM, Sec. II) is followed, then the Hugoniot energies will be relative to $T = 0$. The value of Q will be that at $T = 0$, with the term $(-RT_0)$ incorrectly subtracted.

$$\rho_0^2 D^2 = (p-p_0)/(v_0-v) .$$

On the isentrope, the particle velocity u , which would require evaluation of the Riemann integral, is not calculated. For the isentrope whose initial point is a CJ point, the quasi-static work done by the explosive in expansion of the products to the given pressure, described in Appendix B,

$$W(p) = e_j - \frac{1}{2} u_j^2 - e_i(p)$$

is printed in the u -slot.

V. PROGRAM

The program listing, Appendix C, contains a list of all routines and common data blocks, with a one-line description of each. It also contains, with each routine, comments giving the routine's specifications. In most cases, the logic is simple enough that suitably placed internal comments suffice to describe it. The exceptions are collected here, in order of decreasing logical level in the program. A detailed list of the contents of all common data blocks is given in Appendix D.

A. Equilibrium Iteration - EQM

To calculate a state point at given T and p , MES calls TIM for the ideal free energies (F_i^i at the given T), and then SEM for the solid free energy $\mu_s^i \equiv F_s^i(T, p)$. It then calls EQM, which calls XIM for the gas mixture EOS in the process of finding the equilibrium composition. Finally it calls TIM for the complete set of ideal functions at the new composition, and then COUT for the complete state.

Because of the multiplicity of EOS and mixture-rule options, EQM and XIM are the most complex routines of the program. EQM is outlined in Table II. Subscript i means all species; for example, $\hat{x}_i \leftarrow x_i$ means save all gas mole fractions. Also, only the most important input and output items of routines XIM and EQMS are indicated. In words, the solid \tilde{F}_i is calculated once at the start because it depends only on T and p , which are here fixed. First, the mixture routine XIM(1) is called for the imperfection chemical potentials. These are then added to the ideal ones (calculated earlier by TIM) to get the \tilde{F}_i which are the input to the (ideal, i.e., constant- \tilde{F}_i) equilibrium routine EQMS. The current

TABLE II
THE EQUILIBRIUM-EOS ROUTINE EQM

	$\tilde{F}_S \leftarrow F_S^i + F_S^i$	solid \tilde{F} , depends on T, p only
α	$\mu_i^i, r^* \leftarrow \text{XIM}(1)$	gas μ_i^i (r^* for LH & One-Fluid only)
β	$\tilde{F}_i \leftarrow F_i^i + \mu_i^i$	(F_i^i from TIM earlier)
	$\hat{x}_i \leftarrow x_i$	save old x_i
	$x_i \leftarrow \text{EQMS}(\tilde{F}_i, \tilde{F}_S)$	new x_i at constant F_i
	if $(\sum x_i - \hat{x}_i < \epsilon)$: go to γ	done?
	$x_i \leftarrow 1/2 (x_i + \hat{x}_i)$	next guess: mean of new and old
	$\tilde{F}_i, \bar{r}^* \leftarrow \text{XIM}(2)$; go to β	(CS or One-Fluid only)
γ	if [(CS or One-Fluid) and ($ \bar{r}^* - r^* < \epsilon$)]: go to α	outer done?
	(gas state) $\leftarrow \text{XIM}(3)$	final state

composition is saved for later use in the convergence test and in getting the next guess, and then EQMS is called to calculate the composition implied by the current \tilde{F}_i and \tilde{F}_S . If the resulting composition change is small enough, this finishes the iteration for other than the CS or One-Fluid mixture rules (used only with LJD EOS). If not, the next guess for the composition is taken as the mean of the new and old values, new \tilde{F}_i are computed by XIM(2), and the cycle is repeated starting at β . For the CS and One-Fluid mixture rules the completion of the above (inner) iteration is one step of an outer iteration whose convergence test is that the value of \bar{r}^* from XIM(2) after the inner iteration is complete be close enough to its value furnished by XIM(1) at the start at α . This is discussed in more detail below.

We next describe the action of XIM, which is different for the different equations of state and mixture rules. Here GEP is the gas EOS routine, which

gives the ideal-gas, LJD, or KW equations of state (according to the gas switch from CON, SWIT) and XIM chooses the mixture rule from this switch and the mix switch, which we here call k, from CON, SWIT or CON, XIP. For the LH, CS, and One-Fluid mixture rules, XIM calls XIMS for the detailed computations. The notation $XMT \leftarrow GM$ indicates that the pure-fluid state in the GM array is moved to the mixture state in the XMT array. Also, T^* and V^* are to be understood in addition wherever r^* is indicated. The numbers (1), (2), and (3) refer to action taken at the $XIM(i)$ calls, $i = 1, 2, 3$. The options are as follows:

•KW EOS

Recall that GEP calls HKW, which calculates the complete (mixture) EOS.

(1), (2), (3) HKW via GEP supplies the state, including the μ_i' .

•k=0: No-mix [normally used only for a pure fluid (single species)]

(1) GEP supplies the pure-fluid EOS for the input r^* . The μ_i' are all set to the pure-fluid F_g' , and $XMT \leftarrow GM$.

(2) No action.

(3) $XMT \leftarrow GM$.

•k=1: Ideal mix

(1) For each species, set r^* to r_i^* , call GEP for the pure-fluid EOS, and set μ_i to F_g' .

(2) No action.

(3) Calculate all mixture imperfection quantities as linear mole-fraction sums of those for the individual species.

•k=2: LH mix

(1) Set r^* to the input reference-fluid value, then call GEP for the pure-fluid EOS, and call XIMS for the μ_i' .

(2) Call XIMS for the μ_i' .

(3) Call GEP for the final state, then $XMT \leftarrow GM$. (Why any action is needed here is no longer clear to me.)

•k=3: CS mix, and k=4: One-Fluid mix

(1) Call XIMS to get \bar{r}^* , set r^* to \bar{r}^* and call GEP for the EOS, then XIMS for the μ_i' . (XIMS calculates both \bar{r}^* and the μ_i' , using the reference-fluid state. Here two calls on it are necessary, the first gets r^* , which is needed for the reference-fluid state. There are actually two entries to XIMS that are not distinguished here; the first calculates only \bar{r}^* , the second both \bar{r}^* and the μ_i' .)

- (2) Call XIMS for the μ_j^i and \bar{r}^* .
- (3) No action.

The outer iteration described earlier is necessitated by a time-saving device introduced in GEP. A second entry GEP(2) calculates the approximate gas EOS (for LJD) by the quick route of the LH expansion from the reference state currently stored. This time-saving entry is used by XIMS to get the gas state required for the calculation of the μ_j . Where the mean r^* depends on composition as for the CS and One-Fluid mixture rules, the validity of this expansion is ensured by the outer iteration.

B. Iterations

The iterations are tabulated in Table III. All except that for the equilibrium composition described above can be written as a function of a single variable and are controlled by FROOT. Note that the gas and solid EOS iterations, independent and on the same level, must both be completed as part of the equilibrium iteration, which must in turn be completed as part of the calculation of the function for the Hugoniot or constant-v, s, or e iterations. Finally the Hugoniot iteration must be completed as part of the calculation of the function for the CJ iteration. This stacking requires careful adjustment of the convergence criteria for a reliable system. The functions chosen are not too nonlinear and their magnitudes and slopes are reasonable size (the factor of 20 in the Hugoniot function is introduced for this reason). In general there are slots in CON, FOB for several constants for each FROOT iteration: (1) The convergence criterion ϵ , (2) The "guess-constant" r , in most cases the ratio of the second to first guess, and (3) upper and lower bounds for the iteration variable or the related physical quantity. Not all of (2) and (3) are used in every case. Under "Bounds", subscripts min and max denote (3), other bounds are computed as indicated. Finally, we use subscripts 1 and 2 in the "Guesses" column to denote iteration steps 1 and 2. Remarks on some of the iterations follow.

•CJ

For the second guess, a constant- γ isentrope is a sufficiently good approximation to the CJ locus. For the lower bound, we use the constant- γ approximation to the constant-volume detonation pressure. In the function, γ is evaluated for either fixed or equilibrium composition according to the setting of the input switches; thus either a frozen or equilibrium CJ point may be obtained.

TABLE III

Iteration for ^a	FROOT C-array	In Routine	ITERATIONS		Independent Variable x	Function f(x)
			Guesses	Bounds		
Chapman-Jouguet	CC	CJ	$p_1 = \text{previous (0.3)}$ ^b $p_2 = p_1 (v_1/v_2)^{\gamma_1}$ $v_2 = g(p_1)$	$p > \frac{1}{2} (\gamma-1) \rho_0 q \approx p_H(\rho_0)$	p	$j(p) - 1$ $j(p) = \left[\frac{v/v_0}{\gamma(\gamma+1 - p_0/p)} \right]^{-\gamma}$
Hugoniot	CH	HUG	$T_1 = \text{previous (3000)}$ $x_2 = x_1 - f_1/f_1'$ ^c	$T > T_{\min}$ $T < T_{\max}$	T/1000	$20 \left[\frac{h(T;T_0) - h_0(T_0;T_0)}{(p-p_0)v_0} - \frac{1}{2} \left(1 + \frac{v}{v_0} \right) \right]$ ^d
Contour (constant- v, s, or e)	CM	MESC	$T_1 = \text{previous}$ $T_2 = r T_1$	none	T	v: $v-v_c$ s: $e^{s/s_c} - 1$ e: $e-e_c$
Gas EOS	CG	GEP	$x_1 = \text{previous (}\ln 10)$ $x_2 = x_1 - f_1/f_1'$	$V_g > V_{g \min}$ $V_g < V_{g \max}$	$\ln V_g$	$\ln [p(V_g, T)/p]$
Solid EOS	CS	SEMS	$x_1 = \text{previous (0.8)}$ $x_2 = r x_1$	$x > x_{\min}$ $x < 1 + \alpha(T-T_0)$	V_s/V_{s0}	see Sec. IV
Equilibrium composition	See Sec. V.A.					

^aThe order given is that of the CON, FOB input corresponding to that of the C-arrays in store. Logically, the equilibrium-composition iteration be-
just above that for the gas EOS, and the gas and solid EOS are on the same level as are the Hugoniot and the contour.

^bThe value in parentheses is used on first entry.

^cOn first entry, $f' = r$.

^dThe energy zero for h is T_0 ; see Sec. IV.A.

•Hugoniot

The value of f' for the second guess is that calculated by numerical difference on the last step of the iteration for the previous point. On the first time through it is the input guess-constant r .

•Gas

The derivative f'_1 for the second guess is calculated from the derivative $(\partial p/\partial V_g)_T$ furnished by the gas EOS routine GEM.

•Solid

The function, given in Sec. IV.B, is based on the isentrope relation. The quantity α in the upper bound is the thermal-expansion coefficient.

C. LJD Gas EOS Integration (In GES)

As shown in Fig. 5 the problem is to evaluate to prescribed accuracy for any α an integral

$$\int_0^{b^*} f(x;\alpha) dx ,$$

with the integrand depending on α in such a way that for some α it effectively vanishes at some x appreciably less than b^* . We use the 16-point Gauss approximation (Sec. IV.C); its straightforward application to this case would waste those points lying in the region of $f(x) \cong 0$. (Actually all seven integrals are done at the same time; for simplicity the description here is for one.)

The method is to check for the vanishing of the integrand and to perform the integration in segments if necessary. Because α changes little between most of the entries, this turns out to be reasonably efficient. The part of GES that does the integration consists of a control code, which chooses and adds the segments, and a procedure that integrates over a segment and reports how soon the integrand becomes negligible, if at all. All segment lengths are $b^*/2^n$, n integral.

The segment integration procedure $\tilde{I}(b_1, b_2)$ evaluates $\int_{b_1}^{b_2} f(x;\alpha) dx$ by the 16-point Gauss method and reports three conditions for the size of the integrand near the end of the interval. Let i ($i = 1$ to 16) be the Gauss point at which the integrand first becomes negligibly small. Then I reports that the upper limit b_2 is

"too small" for no such i ($LD = 1$),

"just right" for $14 \leq i \leq 16$ ($LD = 3$), or

"too large" for $i < 14$ ($LD = 2$),

LD being the Fortran variable that reports the condition. (The actual test is that the condition $|f(x_i)/\sum_{j=1}^i a_j f(x_j)| < \epsilon$ be satisfied for each of the seven integrals). The algorithm which evaluates the complete integral using the segment procedure $\tilde{I}(b_1, b_2)$ is given in Table IV.

D. FROOT-Solve $f(x) = 0$ by Iteration

Number the successive steps in the iteration 1, 2, 3, ..., n, ... with nth (function) argument x^n and function $f^n \equiv f(x^n)$. The complete current state of the iteration is contained in FROOT's argument array c

- c 1 ϵ - convergence: $|f^n| < \epsilon$
- 2 x^n
- 3 f^n
- 4 x^{n-1}
- 5 f^{n-1}
- 6 x^{n-2}
- 7 f^{n-2}
- 8 n - step number
- 9 k - branch index:
 - 1 - finished ($|f^n| < \epsilon$)
 - 2 - continue
 - 3 - error 1: $\tilde{x}^n = x^n$ (see below)
 - 4 - error 2: $f^n = f^{n-1}$.

Each time it is called, FROOT bumps n by 1, finds the new x^n and returns to the user, who calculates $f^n = f(x^n)$ and calls FROOT again. The user exits from this loop on convergence via the branch number k. The prototype program is (ϵ pre-stored)

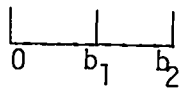
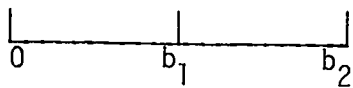
$$n \leftarrow 0, \quad x^n \leftarrow x_g^2, \quad x^{n-1} \leftarrow x_g^1$$

TABLE IV
ALGORITHM FOR THE CELL INTEGRAL

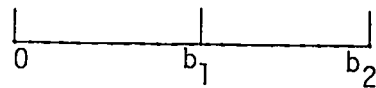
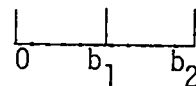
α $b_2 \leftarrow b'$, $b_1 \leftarrow b'/2$	b' is upper limit from last entry
$I \leftarrow \tilde{I}(0, b_1)$	first segment
if (b_1 just right): done	
if (b_1 too large): $\langle b' \leftarrow b^*/2$, go to $\alpha \rangle$	halve and start again
if (b_1 too small):	
$\langle \beta$ $I \leftarrow I \pm \tilde{I}(b_1, b_2)$	add 2nd segment
if (b_2 too large or right): done	
if (b_2 too small): $\langle b' \leftarrow 2b'$, $b_2 \leftarrow b'$, $b_1 \leftarrow b'/2$, go to $\beta \rangle \rangle$	double

The upper limit b' (not shown is that b' is bounded $\leq b^*$) is saved each time and used as the first guess on the next entry. The successive segments look like

b_1 too large



b_1 too small



```

α CALL FROOT
   GO TO (β, γ, δ1, δ2) k

γ calculate fn ≡ f (xn)
   GO TO α

δ1, δ2 error handling

β done, proceed

```

Here n , x^n , etc., refer to slots in \underline{c} as indicated above. The user starts the iteration by setting the step index n to zero and supplying x_g and x_g^2 , the first two guesses for x . The iteration then proceeds through the α - γ loop to convergence. Because all the current state is in \underline{c} (and none of it is stored in FROOT), one copy of FROOT can simultaneously control any number of interdependent iterations (i.e., the calculation of $f(x)$ for some iteration may itself require an iterative solution involving FROOT).

The algorithm is the secant method

$$x^1 = x_g^1 ,$$

$$x^2 = x_g^2 ,$$

$$x_n = x^{n-1} - f^{n-1} (x^n - x^{n-1}) / (f^n - f^{n-1}) ,$$

with a refinement wherein \tilde{x}^n is a provisional value of x^n subject to modification. In the normal case it is accepted and the store is stepped down as follows:

$$(x, f)^{n-2} \leftarrow (x, f)^{n-1} ,$$

$$(x, f)^{n-1} \leftarrow (x, f)^n ,$$

$$x^n \leftarrow \tilde{x}^n .$$

The modification replaces \tilde{x}^n if, roughly, it does not lie in the range of previous x 's and if two f 's of opposite sign are on hand. Precisely, if

(1) \tilde{x}^n is not between x^n and x^{n+2} , and

(2) $(\text{sign } f^n = \text{sign } f^{n-1})$ and $(\text{sign } f^n \neq \text{sign } f^{n-2})$

then \tilde{x}^n is recalculated (before the step-down) with point $(n-2)$ instead of $(n-1)$

$$\tilde{x}^n = x^n - f^n (x^n - x^{n-2}) / (f^n - f^{n-2}) .$$

Also, saving of old points is done in such a way that once two f 's of different sign are on hand, the step-down will never result in three f 's of the same sign. Precisely, if condition (2) is satisfied, then the step-down is preceded by

$$(x, f)^{n-1} \leftarrow (x, f)^{n-2} .$$

We remark that, because \underline{c} specifies the state completely, the user, knowing the program's algorithm, may wish to change it in flight. A common case is that a lower bound x^* is known for x , and FROOT at some step supplies $x^n < x^*$. The user might replace x^n by x^* whenever this happens.

As an example (see Fig. 6), we write the code to solve $f(x) = x^{1/2} - A = 0$. The secant recipe can easily give a negative x as the next guess; we prevent this by introducing a fixed lower bound $x = x^*$, x^* small.

```

DATA C(1)/1.0 E-8/
DIMENSION C(9), KC(2)
EQUIVALENCE (KC, C(8))
KC(1) = 0
C(4) = 1.
C(2) = 1.2
α CALL FROOT (C)
GO TO (β, γ, δ, δ) KC(2)

```

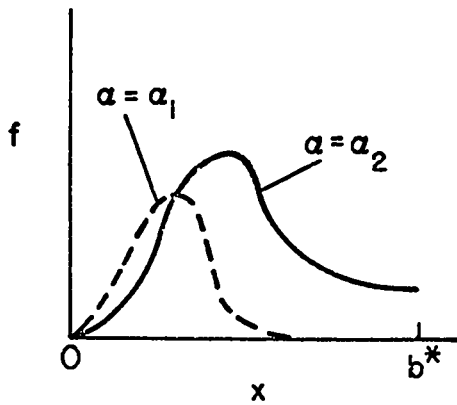


Fig. 5. Integrands for the LJD cell integral.

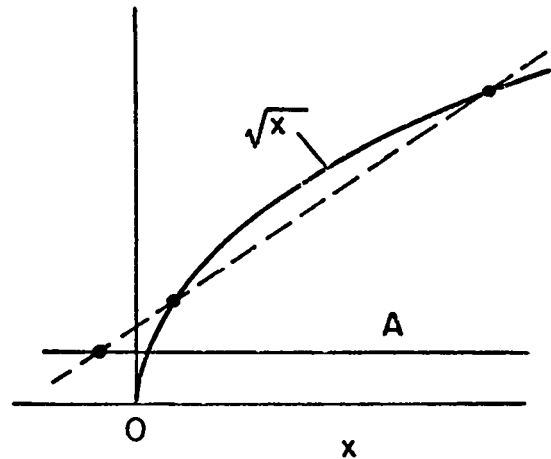


Fig. 6. Iterative solution of $f(x) = x^{1/2} - A = 0$ by FROOT.

```

      γ IF (C(3) < x*) C(3) = x*
      C(3) = SQRT (C(2)) - A
      GO TO α

      δ CALL ERR

      β CONTINUE
  
```

VI. SAMPLE INPUT/OUTPUT AND TEST

Tables V and VI are a key to the output labels and a sample calculation, which also serves as a fairly complete test of the program. The calculation is a chemical equilibrium calculation for the explosive RDX with the LJD EOS and the CS mixture rule. Part 2 of the input defines the following:

- (1) A state point at $T = 2000$, $p = 0.3$.
- (2) Detonation Hugoniot points at $p = 0.3$ and 0.2 .
- (3) CJ points for $\rho_0 = 1.6$ and 1.8 .
- (4) CJ isentrope points at $p = p_{CJ}$, 0.3 , and 0.2 .

A CON, DEBUG print follows item (1). The point printed here is the last slightly displaced one used in the finite-difference calculation of the derivatives.

TABLE V
OUTPUT KEY

<u>Line</u>							
1	p	v/v ₀	T	u or W	D	ρ ₀	q
2	v	e	s	n _g	n _s	n	(ln \hat{s} or - \hat{n}_s)
3	V	E/RT	S/R	z	n ₁	n ₂	n ₃
4	V _g	E' _g /RT	S' _g /R	z' _g	n ₄	n ₅	n ₆
5	V _r	E' _r /RT	S' _r /R	z' _r	n ₇	n ₈	n ₉
6	V _s	E' _s /RT	S' _s /R	z' _s	n ₁₀	n ₁₁	n ₁₂
7	\bar{r}^*	\bar{T}^*	\bar{V}^*	γ	α	β	c

Notes

1. Lines 1-3 are for the complete system. For lines 4-6 the first four items are for the gas phase, the gas-phase reference fluid, and the solid phase, respectively. The reference fluid differs from the gas phase only for the LH mixing rule (Sec. IV.D.2).
2. The last item in line 2 gives the state of super- or undersaturation of the system with respect to the solid phase; $\ln \hat{s}$ (the saturation index, Sec. IV.E) is printed if a single-phase system was specified and it wants to precipitate solid, and $-\hat{n}_s$ (the number of added moles of solid which would just saturate the system) is printed if a two-phase system was specified and no solid is present.
3. All mole numbers are moles per mole of system (one mole of system = M₀ grams, with M₀ from the SAM input pack).
4. The "u or W" slot in line 1 is the particle velocity for the Hugoniot or CJ point, the quasi-static expansion work (Sec. IV.F and Appendix B) for the CJ isentrope, and meaningless otherwise.
5. All other symbols are defined in the symbol list. Recall that $z \equiv pV/RT$ (and $z' = pV/RT - 1$) and that a prime denotes an imperfection quantity (Secs. III.B.1-3). Molar quantities for the system are per mole of system and for the phases are per mole of phase. All quantities divided by RT are dimensionless.

TABLE VI
SAMPLE CALCULATION

Input Data

```

CON PAS MES1 = SHORT TEST * CJ, HUG, ISENTROPE
CON SWIT DIFF
1
CON 1
  FOB
  5.0 E+05 2.0 E+06 1.2 E+05 7.0 E+07 1.0 E+07 0.0
  0.0 1.0 1.1 0.0 9.7 E+01 0.0
  1.01 1.01 E+02 1.0 E+05 2.0 E+06 0.0 0.0
  1.0 F+03 1.0 E+06 5.0 E+02 8.0 E+03 4.3 E+01 0.0
  0.0 0.0 0.0 0.0 0.0 0.0 0.0
CON 2
  GEP
  1.0 E+01 6.0 E+00 1.0 E+00 1.0 E+00 4.4365 E+00 7.54837E+01
CON 3
  SEP
  1.056 E+01 2.5 8.03 E+06 5.333 2.9816E+02 4.246 E+01
  0.0 3.2751 -7.9015 6.6656 =2.0392 0.0
CON 4
  TIP
  1.0 E+03 6.0 E+03
  4.8761 E+01 1.4947 E+03 -4.2896E+07 6.2644 E+11 -3.4991E-15 -2.81 E+00
  0.0 E+00 0.0 E+00 4.2457 E+01
  3.1499 F+00 3.8718 E+04 -1.3665E+07 1.6756 E+11 -8.2278E+16 4.673 E+00
  0.0 E+00 0.0 E+00 3.4975 E+00
  3.1818 E+00 5.9459 E+04 -1.4065E+07 1.7307 E+11 -8.07 E-16 5.2157 E+00
  -2.7222E+01 -2.6416E+01 3.4979 E+00
  3.2022E+00 1.18370E+03 -2.1492E+07 2.28400E+11 -1.0874E-15 3.19230E+00
  -5.7107E+01 -5.7798E+01 3.99610E+00
  3.377 E+00 5.80470E+04 -1.5608E-07 2.04140E+11 -1.0944E-15 5.93 E+00
  2.1477 E+01 2.16 E+01 3.7032 E+00
  3.2375 E+00 2.3187 E+04 5.0938 E+09 -3.9631E+12 2.931 E-16 -2.8804E+00
  0.0 E+00 0.0 E+00 3.4157 E+00
  3.7308 E+00 1.9444 E+03 -5.121 F+07 6.8031 E-11 -3.5368E-15 3.4656 E+00
  -9.3969E+01 -9.4052E+01 3.7772 E+00
  3.4234 E+00 4.55 E+04 -8.0583E+08 9.4557 E-12 -4.8556E-16 4.862 E+00
  0.0 E+00 0.0 E+00 3.4934 E+00
CON 5
  XIP
  M2 = BEST MCM SET FROM OTHER SOURCES ,GMX=10=54,P43
  7
  2
  1.0 E+00 1.0 F+00 3.80012E+00 1.41744E+02 6.0 E+00 1.2 E+01
  4.05 E+00 4.05 E+00 3.35 E+00 3.56 E+00 3.34 E+00 4.2 E+00
  3.73 E+00
  1.2 E+02 1.2 E+02 1.38 E+02 1.31 E+02 3.7 E+01 2.0 E+02
  1.32 E+02
CON 6
  EQP
  4
  3.0 8 1 0 1 1
  6.0 0.0 6.0 6.0
  C(S) C H O N A1 A0
  M2 1 0 0 0
  CO 0 0 0 2
  H20 1 0 1 0
  NO 0 0 1 1
  H2 0 2 1 0
  
```

```

C02 1 0 2 0
02 0 0 2 0
4 1 6 3 5 2 8
8 1 2 3 4 6 7
CON SAM RDX, RHO=1.8, CO2=ARBITRARY COMPOSITION GUESS
8
1.8 E+00 0.0 E+00 2.9816 E+02 2.2213 E+02 1.471 E+01
1.5 E+00 3.0 E+00 0.0 E+00 3.0 E+00 0.0 E+00 0.0 E+00
1.5 E+00 0.0 E+00
CON PV
1 0
2.0 E+03 3.0 E+01
0.0 E+00 0.0 E+00
CON DEBUG
CON TED DETCNATION HUGONIOT
0.3 0.2 0.0
CON CJ CJ LOCUS
1.0 1.8
CON PV CJ ISENTROPE
3 1
0.0 0.0
0.3 0.2
CON REND
CON JEND

```

Calculation

```

MES1 = 744.620 MES1 = SHOOT TPST = CJ* HUG. ISENTROPE
TFICKE13N. .004 SEC ON RUN. .056 SEC ON JOB

```

```

CON SWIT DIFF
DIFF: FX DIFF: GAS. SOLID. MIX. EO: CJ: PV
1 -0 -0 -0 -0 -0 -0 -0 -0 -0 -0

```

```

CON FOR
FRODT FPSICCC*CH*CM*CG*CS*CI / RATIOS/ DP*DT*EPSIN*OUT/ FRODT HOUNDS
5.00000E-05 2.00000E-06 1.20000E-05 7.00000E-07 1.00000E-07
0. 0. 1.00000E+00 1.10000E+00 0.
9.70000E-01 0. 1.01000E+00 1.01000E-02 1.00000E-05
2.00000E-06 0. 0. 1.00000E-03 1.00000E-06
5.00000E-02 8.00000E-03 4.30000E-01 0. 0.
0. 0. 0. 0. 0.

```

```

CON GEP
0 PGT (1-LJ+2-MCM+3-MR) *W (NOW 1) / N*M*AN*AM*R*+T*
2 1
1.00000E+01 6.00000E+00 1.00000E+00 1.00000E+00 4.43650E+00
7.54837E+01
V* .37.2000000

```

```

CON SEP
CX G. CPH. AL. V0. T0. FOR / C0. C1. C2. C3. C4
1.45600E-01 2.50000E+00 8.03000E-06 5.33300E+00 2.98160E+02
4.24600E-01 0. 3.27510E+00 -7.90150E+00 6.66560E+00
-2.03920E+00 0.

```

CON TIP
 K5,K6 / T BOUNDS/ FIT COEFFS. =A1 TO AN.D,DEL.HF.HR...

8
 1.40000E+03 6.00000E+03
 4.87610E-01 1.49490E-03 -4.28960E-07 6.26440E-11 -3.49910E-15
 -2.91000E+00 0. 0. 4.24570E-01
 3.14990E+00 5.87180E-04 -1.36450E-07 1.67540E-11 -8.22780E-16
 4.67300E+00 0. 0. 3.49750E-00
 3.18180E+00 5.94590E-04 -1.40650E-07 1.73070E-11 -8.47000E-16
 5.21570E+00 -2.72020E-01 -2.64160E+01 3.49720E+00
 3.22220E+00 1.14370E-03 -2.14920E-07 2.22490E-11 -1.08740E-15
 3.19230E+00 -5.71070E+01 -5.77980E+01 3.99610E+00
 3.32700E+00 5.80470E-04 -1.50080E-07 2.04140E-11 -1.09440E-15
 5.93000E+00 2.14770E+01 2.16000E+01 3.70320E+00
 3.23750E+00 2.31470E-04 5.09380E-09 -3.96310E-12 2.93100E-16
 -2.22040E+00 0. 0. 3.41570E+00
 3.73080E+00 1.94440E-03 -5.12100E-07 6.80310E-11 -3.53680E-15
 3.46550E+00 -9.39640E+01 -9.40520E+01 3.77720E+00
 3.42340E+00 4.56000E-04 -8.05830E-08 9.45570E-12 -4.85560E-16
 4.86200E+00 0. 0. 3.49340E+00

CON AIP M2 - BEST MCM SFT FROM OTHER SOURCES .GMX-10-54,P43
 KR,KAL / SCR,SCT,R*PFF,T*PFF,N*P / (R*) / (T*)

7
 1.00000E+00 1.00000E+00 3.80012E+00 1.41744E+02 6.00000E+00
 1.20000E+01
 4.05000E+00 4.05000E+00 3.35000E+00 3.56000E+00 3.34000E+00
 4.20000E+00 3.73000E+00
 1.20000E+02 1.20000E+02 1.38000E+02 1.31000E+02 3.70000E+01
 2.00000E+02 1.32000E+02

CON EGP
 C,S,P,-,PP,PHI / CAP Q

4
 R . I 0 j 1
 3.00000E+00 6.00000E+00 6.00000E+00 6.00000E+00

	C	H	O	N	A1	A0
C(S)	1	0	0	0	4	8
M2	0	0	0	2	1	1
CO	1	0	1	0	6	2
M20	0	2	1	0	3	3
M0	0	0	1	1	7	5
M2	0	2	0	0	5	4
CO2	1	0	2	0	2	6
O2	0	0	2	0	8	7

QBAR .3333333E+00 .3333333E+00 .3333333E+00 0.

NU MAT .5000000E+00 0. .1000000E+01 -.1000000E+01
 2 0. .1000000E+01 .1000000E+01 -.1000000E+01
 3 0. 0. .2000000E+01 -.2000000E+01
 4 0. .1000000E+01 -.1000000E+01 .1000000E+01

QBAR .4000000E+00 .2000000E+00 .4000000E+00

NU MAT 0. -.5000000E+00 .1000000E+01 .5000000E+00
 2 0. .5000000E+00 0. .5000000E+00
 3 .5000000E+00 .5000000E+00 0. -.5000000E+00
 4 0. .1000000E+01 0. -.1000000E+01

CON SAM RDX, RHO=1.8, CO2=ARBITRARY COMPOSITION GUESS

50

MES1 = 76411620
 TFICKETIGN* .055 SEC ON RUN*
 NS/ RHO, P0, T0, M0, HFE/ NI

MES1 = SHORT TEST = CJ, HUG, ISENTROPE
 .107 SEC ON JOB

09/02/76
 SAM = INPUT PART 2

1.80000E+00 0. 2.98160E+02 2.22170E+02 1.47100E+01
 1.50000E+00 3.00000E+00 0. 3.00000E+00 0.
 0. 1.50000E+00 0.

CON PV

MES1 = 76411620
 TFICKETIGN* .063 SEC ON RUN* .115 SEC ON JOB
 BRANCH (1-T,2-V,3-S,4-E) / TC,PC/ P-TABLE

09/02/76
 LOCUS

2.00000E+03 3.00000E+01
 0.

OUTPUT LABELS

1	P	V/V0	T	U	D	RHO	GCAL	
2	V	E	S	NG	NS	N	SUPSAT	
3	V	E/RT	S/P	PV/RT	N1	N2	N3	
4	NO. FOR GAS				N4, N5, N6			
5	NO. FOR RFF.				N7, N8, N9			
6	NO. FOR SOLID				N10, N11, N12			
7	RRAR*	TBAR*	VRAR*	GAMMA	ALPHA	BETA	C	
POINT 1	1	3.0000000E-01	6.2501147E-01	2.0000000E+03	0.	0.	1.8000000E+01	1.5056345E+00
	2	3.4722859E-01	-6.5145242E-03	5.6504530E-05	7.5019585E+00	1.4980495E+00	9.0000080E+00	1.9968779E-01
	3	8.5699799E+00	-9.6691129E-01	1.6773249E+01	1.5461110E+01	1.4980495E+00	2.9999918E+00	2.5002893E-03
	4	9.5188840E+00	4.8978060E+00	-1.5675174E+00	1.6172668E+01	2.9985825E+00	1.6077797E-05	1.4173827E-03
	5	9.5182069E+00	4.8980736E+00	-1.5673720E+00	1.6171806E+01	1.4994504E+00	6.9640955E-11	0.
	6	3.8190426E+00	1.1026119E+00	-1.4349374E-01	6.8899389E+00	0.	0.	0.
	7	3.9000514E+00	1.4179073E+02	2.3377078E+01	3.1776524E+00	4.7999481E+00	1.8252305E+00	5.7533602E-01

CON DBUG

OUTPUT LABELS

1	P	V/V0	T	U	D	RHO	GCAL	
2	V	E	S	NG	NS	N	SUPSAT	
3	V	E/RT	S/P	PV/RT	N1	N2	N3	
4	NO. FOR GAS				N4, N5, N6			
5	NO. FOR RFF.				N7, N8, N9			
6	NO. FOR SOLID				N10, N11, N12			
7	RRAR*	TBAR*	VRAR*	GAMMA	ALPHA	BETA	C	
POINT 2	1	3.0000000E-01	6.2460797E-01	2.0000000E+03	0.	0.	1.8000000E+00	1.5056645E+00
	2	3.4722859E-01	-6.5145242E-03	5.6504530E-05	7.5017720E+00	1.4982350E+00	9.0000070E+00	1.9971748E-01
	3	8.5644482E+00	-1.0251742E+00	1.6715067E+01	1.5608779E+01	1.4982350E+00	2.9999930E+00	2.2481195E-03
	4	9.5123142E+00	4.9430188E+00	-1.5777047E+00	1.6336280E+01	2.9987042E+00	1.4021508E-05	1.2958093E-03
	5	9.5118041E+00	4.9433074E+00	-1.5775481E+00	1.6335343E+01	1.4995168E+00	5.4543140E-11	0.
	6	3.8183535E+00	1.1149935E+00	-1.4354516E-01	6.9590543E+00	0.	0.	0.
	7	3.9000467E+00	1.4179416E+02	2.3376993E+01	3.1776524E+00	4.7999481E+00	1.8252305E+00	5.7533602E-01

XMU	25.24461R0	25.24461R0	16.4160201	19.3774R4R	12.0422775	29.8665753	21.602004R	0	0	0
APF	120.0000000	120.0000000	128.6856635	125.3774241	66.5333250	154.4193338	125.857061R	0	0	0
XPG	4.0500000	4.0500000	3.7000000	3.8050000	3.6950000	4.1250000	3.8900000	0	0	0
XPR	4.0500000	4.0500000	3.3500000	3.5600000	3.3400000	4.2000000	3.7300000	0	0	0
XPT	120.0000000	120.0000000	138.0000000	131.0000000	37.0000000	200.0000000	132.0000000	0	0	0

CCN TED DETONATION HUGONJOT

MESI = 74AUG20 MES1 = SHORT TEST = CJ, HUG, ISENTROPE 09/02/76
 TFICKET16N, *255 SEC ON RUN, *306 SEC ON JOB TED = HUGONJOT
 P-TABLE
 3.00000E-01 2.00000E-01 0.

OUTPUT LABFLS

	1	P	V/V0	T	U	D	RHO	QCAL
	2	V	E	S	NG	NS	N	SUPSAT
	3	V	E/RT	S/R	PV/RT	N1	N2	N3
	4	DO. FOR GAS				N4, N5, N6		
	5	DO. FOR REF.				N7, N8, N9		
	6	DO. FOR SOLID				N10, N11, N12		
	7	RRAR*	TBAR*	VRAR*	GAMMA	ALPHA	RETA	C
POINT 3	1	3.0030000E-01	6.8209108E-01	4.1800622E+03	2.3018432E-01	7.2405743E-01	1.8000000E+00	1.4490847E+00
	2	3.7893949E-01	3.2889349E-02	7.2737497E-05	7.8132457E+00	1.1953025E+00	9.0085483E+00	1.5298412E-01
	3	9.3437728E-00	2.3334302E+00	2.1571501E+01	8.0654831E+00	1.1953025E+00	2.9914696E+00	4.7909272E-01
	4	1.0178271E+01	2.5983520E+00	-1.0676278E+00	7.7858100E+00	2.8526013E-00	1.7060806E-02	1.4739874E-01
	5	1.0239780E+01	2.5880818E+00	-1.0832547E+00	7.8389102E+00	1.3256048E+00	1.7850473E-05	0.
	6	3.8889734E+00	4.6778127E-01	-1.4269480E-01	3.3569362E+00	0.	0.	0.
	7	3.8054155E+00	1.3674799E+02	2.3476215E+01	2.7005031E+00	3.4377594E+00	1.6433084E+00	5.5407417E-01
POINT 4	1	2.0000000E-01	7.9305378E-01	3.8045213E+03	1.5163781E-01	7.3274016E-01	1.8000000E+00	1.4282619E+00
	2	4.4058543E-01	1.7494021E-02	7.2769549E-05	7.9598912E+00	1.0428837E+00	9.0027748E+00	1.3101733E-01
	3	1.0870786E+01	1.3957523E+00	2.1504852E+01	6.8732248E+00	1.0428837E+00	2.9972708E+00	7.0824972E-01
	4	1.1733924E+01	2.0083885E+00	-1.0222304E+00	6.4189573E+00	2.7884647E+00	5.5375631E-03	2.1153484E-01
	5	1.1814529E+01	1.9896563E+00	-1.0439089E+00	6.4699210E+00	1.2488675E+00	6.0617958E-06	0.
	6	4.2828177E+00	2.4792361E-01	-1.0179699E-01	2.7078785E+00	0.	0.	0.
	7	3.8091047E+00	1.3463469E+02	2.3544560E+01	2.6846183E+00	3.0978413E+00	1.5264149E+00	4.8637510E-01

CON CJ CJ LOCUS

MESI = 74AUG20 MES1 = SHORT TEST = CJ, HUG, ISENTROPE 09/02/76
 TFICKET16N, *583 SEC ON RUN, *634 SEC ON JOB CJ
 CJ RHO=TABLE
 1.60000E+00 1.80000E+00 0.

OUTPUT LABELS

	1	P	V/V0	T	U	D	RHO	QCAL
	2	V	E	S	NG	NS	N	SUPSAT
	3	V	E/RT	S/R	PV/RT	N1	N2	N3
	4	DO. FOR GAS				N4, N5, N6		
	5	DO. FOR REF.				N7, N8, N9		
	6	DO. FOR SOLID				N10, N11, N12		
	7	RRAR*	TBAR*	VRAR*	GAMMA	ALPHA	RETA	C
POINT 5	1	1.9888975E-01	7.2232555E-01	4.0889247E+03	1.8578651E-01	6.6968830E-01	1.6000000E+00	1.4015000E+00
	2	4.5145347E-01	2.3655305E-02	7.4780944E-05	8.1163490E+00	8.8812807E-01	9.0044771E+00	1.0942458E-01
	3	1.1136433E+01	1.7198412E+00	2.2187548E+01	6.5287858E+00	8.8812807E-01	2.9955360E+00	9.4626716E-01
	4	1.1885171E+01	1.9013426E+00	-9.5906179E-01	5.9667285E+00	2.7135671E+00	8.9273000E-03	2.8643254E-01
	5	1.1991605E+01	1.8784433E+00	-9.8744027E-01	6.0291173E+00	1.1656054E+00	1.3430422E-05	0.
	6	4.2979901E+00	2.2279628E-01	-1.0119332E-01	2.5193522E+00	0.	0.	0.
	7	3.8119124E+00	1.3238677E+02	2.3596662E+01	2.8013401E+00	2.9184306E+00	1.5063123E+00	4.8329384E-01

POINT	6	1	2.4894704F-01	7.2997845E-01	3.9844666E+03	1.9324864E-01	7.1567857E-01	1.8000000E+00	1.4418736E+00
		2	4.0554358F-01	2.5069501E-02	7.2607369E-05	7.8696632E+00	1.1353011F+00	9.0049643E+00	1.4426299F-01
		3	1.0003748F+01	1.8666819E+00	2.1540388E+01	7.5174255E+00	1.1353011E+00	2.9950458E+00	5.6811003F-01
		4	1.0858513F+01	2.3172328E+00	-1.0528061E+00	7.1597479E+00	2.8287812E+00	9.9076675E-03	1.7121838E-01
		5	1.0026612F+01	2.3031322E+00	-1.0707144F+00	7.2100219E+00	1.2965897E+00	1.0485669E-05	0.
		6	4.0787016F+00	3.5453600E-01	-1.2246953E-01	3.0649847E+00	0.	0.	0.
		7	3.8070314F+00	1.3593882E+02	2.3506133E+01	2.7034071E+00	3.2774684E+00	1.5822509E+00	5.2242984E-01

CON PV CJ ISENTROPE

MES1 = 76AUG20 MES1 = SHORT TEST = CJ, HUG, ISENTROPE

09/02/76

TFICKET16N, 1.632 SEC ON RUN, 1.684 SEC ON JOB

LOCUS

BRANCH (1-T,2-V,3-S,4-E) / TC,PC/ P-TABLE

3 1
 0. 0.
 3.00000E-01 2.00000E-01 0.

OUTPUT LABELS

		P	V/V0	T	U	D	RHO	OCAL
		V	E	S	NG	NS	N	SUPSAT
		V	E/RT	S/R	PV/RT	N1	N2	N3
		NO. FOR GAS				N4,N5,N6		
		NO. FOR REF.				N7,N8,N9		
		NO. FOR SOLID				N10,N11,N12		
		RRAP	TRAR	VRAR	GAMMA	ALPHA	RETA	C
POINT	7	1	2.4894704F-01	7.2997845E-01	3.9844666E+03	1.9324864E-01	7.1567857E-01	1.4418736E+00
		2	4.0554358F-01	2.5069501E-02	7.2607369E-05	7.8696632E+00	1.1353011F+00	1.4426299F-01
		3	1.0003748F+01	1.8666819E+00	2.1540388E+01	7.5174255E+00	1.1353011E+00	5.6811003F-01
		4	1.0858513F+01	2.3172328E+00	-1.0528061E+00	7.1597479E+00	2.8287812E+00	1.7121838E-01
		5	1.0026612F+01	2.3031322E+00	-1.0707144F+00	7.2100219E+00	1.2965897E+00	0.
		6	4.0787016F+00	3.5453600E-01	-1.2246953E-01	3.0649847E+00	0.	0.
		7	3.8070314F+00	1.3593882E+02	2.3506133E+01	2.7034071E+00	3.2774684E+00	5.2242984E-01
POINT	8	1	3.0000000F-01	6.8133790E-01	4.1506194E+03	-6.2285136E-01	7.1567857E-01	1.4504140F+00
		2	3.7852106F-01	3.2457083E-02	7.2607369E-05	7.8696632E+00	1.2020925F+00	1.5399230F-01
		3	9.3357347F+00	2.3147033E+00	2.1540388E+01	8.0983612F+00	1.2020925E+00	4.6877416F-01
		4	1.0172292F+01	2.6091067E+00	-1.0716390F+00	7.8759305F+00	2.8558995F+00	1.4410009F-01
		5	1.0232402F+01	2.5989927E+00	-1.0869242E+00	7.8780844F+00	1.3296342E+00	0.
		6	3.8882459F+00	4.7078891E-01	-1.4249568F-01	3.3736489E+00	0.	0.
		7	3.8053048F+00	1.3685726E+02	2.3474259E+01	2.7056370E+00	3.4509657E+00	5.5429430F-01
POINT	9	1	2.0000000F-01	7.9167471E-01	3.7817053E+03	-2.6341168E-01	7.1567857E-01	1.4302499F+00
		2	4.3981928F-01	1.7418127E-02	7.2607369E-05	7.9482801F+00	1.0543765E+00	1.3265467F-01
		3	1.0852025F+01	1.3666470E+00	2.1540388E+01	6.9027591E+00	1.0543765F+00	6.9044635F-01
		4	1.1723572F+01	2.0172005E+00	-1.0273858E+00	6.4571326E+00	2.7938894E+00	2.0611114F-01
		5	1.1802214E+01	1.9967990E+00	-1.0485669E+00	6.5071586E+00	1.2551761E+00	0.
		6	4.2819856F+00	2.4994174E-01	-1.0180381E-01	2.7236865E+00	0.	0.
		7	3.8088931F+00	1.3480486E+02	2.3540636E+01	2.6914850E+00	3.1134498E+00	4.8657312F-01

CON REHD

CON JEND

MES1 = 76AUG20 MES1 = SHORT TEST = CJ, HUG, ISENTROPE

09/02/76

TFICKET16N, 2.112 SEC ON RUN, 2.164 SEC ON JOB

JOBEND

DAY-TIME START 21.00.59 , END 21.01.01

COMPLETE TFICKET16N

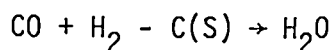
ACKNOWLEDGMENTS

James D. Kershner, T-4, and Jack D. Jacobson, T-4, helped with the programming required to reactivate the code. The equilibrium routine was redone earlier in FORTRAN by Paul Bird, L-3.

APPENDIX A

CHEMICAL EQUILIBRIUM EXAMPLE

We give in Table A-I an example of a system with an equilibrium number of phases (solid carbon may be present or absent). The user must specify two systems, a two-phase system and a one-phase system, and make an appropriate choice of independent species for each. He does this, after defining the species and empirical formula via α and Q , by giving the two renumberings a^1 and a^0 . Recall the definition of a_i : the (original) i th species becomes the a_i th. Take, for example, $i = 4$, $a_4^1 = 1$; CO, originally the fourth species, becomes the first in this the two-phase system. Recall that the solid must be number c in the two-phase system, and number s in the one-phase (where the program assigns it a large F to make its mole fraction negligibly small). The horizontal dashed lines divide the α matrices into independent and dependent parts. The corresponding v and q are given below each α , and the reactions are written out in full below the v 's. The saturation test for the one-phase system is made on the two-phase system reaction



with the saturation index \hat{s} ,

$$\hat{s} = \left(x_{\text{H}_2\text{O}} / x_{\text{C}} x_{\text{H}_2} \right) / K_4 ,$$

evaluated for the mole fractions from the one-phase solution. If $\hat{s} < 1$ the system is unsaturated with respect to deposition of solid carbon, and the one-phase system is the correct choice.

TABLE A-I
EQUILIBRIUM EXAMPLE CH_2O_2 , $c=3$, $s=6$

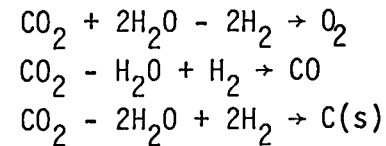
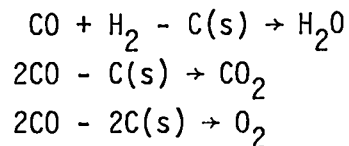
\underline{a} , $\underline{\alpha}$, and \underline{Q} :

\underline{i}	Entry	Two-Phase($p=1$)			One-Phase($p=0$)									
		\underline{C}	\underline{H}	\underline{O}	\underline{a}_i^1	\underline{C}	\underline{H}	\underline{O}						
1	C(s)	1	0	0	3	CO	1	0	1	6	CO_2	1	0	2
2	H_2	0	2	0	2	H_2	0	2	0	3	H_2O	0	2	1
3	O_2	0	0	2	6	C(s)	1	0	0	4	H_2	0	2	0
4	CO	1	0	1	1	H_2O	0	2	1	5	O_2	0	0	2
5	CO_2	1	0	2	5	CO_2	1	0	2	1	CO	1	0	1
6	H_2O	0	2	1	4	O_2	0	0	2	2	C(s)	1	0	0
	\underline{Q}	1	2	2										

\underline{v} and \underline{q} :

\underline{k}		CO	H_2	C(s)		CO_2	H_2O	H_2
4	H_2O	1	1	-1	O_2	0	2	-2
5	CO_2	2	0	-1	CO	1	-1	+7
6	O_2	2	0	-2	C(s)	1	-2	+2
	\underline{q}	2	1	-1	\underline{q}	1	0	1

Reactions:



APPENDIX B
QUASI-STATIC WORK

Summarized here is what might be loosely termed the Carnot cycle for explosives; plus a numerical example. The object is to calculate the maximum energy that can be extracted quasi-statically from an explosive by detonating it. The quasi-static process is that given by Jacobs.³

Confine the explosive in an upright cylinder of unit length and cross section, closed at the top by a rigid cap and at the bottom by a movable piston. Assume that all confining materials including the piston are rigid massless non-conductors of heat. Move the piston into the cylinder with constant velocity u_1 greater than or equal to the Chapman-Jouguet (CJ) particle velocity. As the piston begins to move, instantaneously initiate the detonation at the piston surface. The detonation front will then move upward with complete-reaction wave velocity D_1 determined by u_1 . The detonation products (reacted material) will be in a uniform state with pressure p_1 and particle velocity u_1 . When the detonation wave reaches the upper end of the cylinder, attach the piston to the cylinder at its position at that instant of time and remove the driving force on the piston. Allow the cylinder to move upward under gravity deceleration until its velocity is reduced to zero. Extract work reversibly from the cylinder of product gases in this position by first lowering it slowly to its original position, and then releasing the piston and allowing the products to expand adiabatically and reversibly to some final pressure.

Calculate the net work done on the surroundings in this process. The cylinder has unit volume and contains ρ_0 grams of material. Take work and energy per unit mass of material. The piston moves a distance u_1/D_1 with force p_1 , so the work W_p done by it is

$$W_p = p_1 u_1 / \rho_0 D_1 \quad ,$$

or, using the conservation relation $p = \rho_0 u_1 D_1$ (neglecting p_0),

$$W_p = u_1^2 \quad .$$

The kinetic energy K of the reaction products is

$$K = u_1^2/2 \quad .$$

The work done by the system in expanding to pressure p is

$$I(p) = \int_{v_1}^{v_i(p)} p_i(v) \, dv \quad ,$$

where $p_i(v)$ is the isentrope through the product state (p_1, v_1) . Summing the contributions gives for the net work $W(p)$ on the surroundings for expansion to pressure p

$$\begin{aligned} W(p) &= -W_p + K + I(p) \\ &= I(p) - \frac{1}{2} u_1^2 \\ &= e_1 - \frac{1}{2} u_1^2 - e_i(p) \quad . \end{aligned}$$

We remark that $W(p_0)$ differs little from the heat of reaction q as conventionally defined -- the energy change in the surroundings for reaction to products at T_0, p_0 . To see this and show how the various energy changes enter, we have prepared Fig. B-1, which shows the closed cycle in the p - v plane, and Table B-I, which lists the steps in clockwise traversal beginning at point 0, the unreacted explosive. The numerical example consists of the calculated values for Comp. B from Ref. 2, and is for $T_0 = 300$ K, $p_0 = 1$ atm. For state 2, the calculated temperature is 518 K and the mean γ is 1.25.

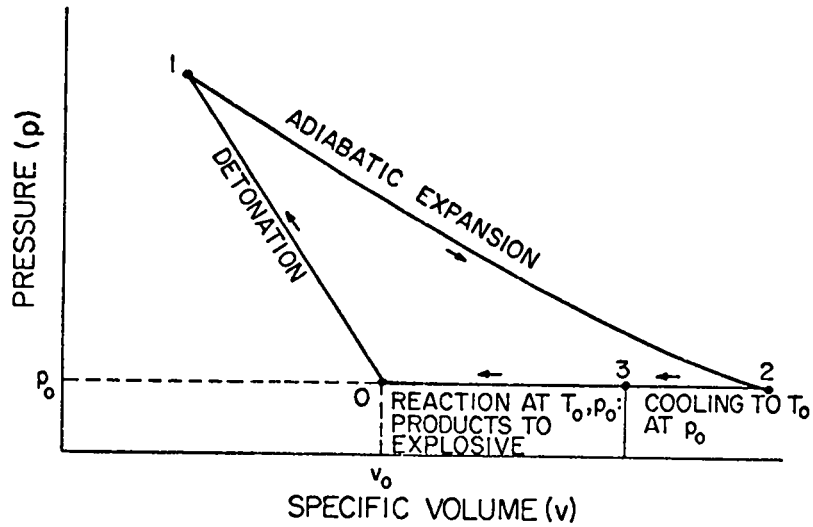


Fig. B-1. Closed cycle of energy changes in the p-v plane.

TABLE B-I

ENERGY STEPS IN CLOCKWISE TRAVERSAL OF FIG. B-1

Process	Energy Change	Comp. B $(\text{mm/s})^2 = \text{Mj/kg}$
Detonation	$e_1 - e_0 = \frac{1}{2} p_1 (v_0 - v_1) = \frac{1}{2} u_1^2$	1.80
Adiabatic expansion	$e_2 - e_1 = -I(p_0)$	-7.56
Cooling at p_0	$e_3 - e_2 = C_p (T_0 - T_2)$	-0.28
Reverse reaction	$e_0 - e_3 = q$	6.04
Thus	$W(p_0) = e_0 - e_2 = q - C_p (T_2 - T_0)$	5.76

APPENDIX C

PROGRAM

I.D. LP-0730

C	AAA	AAA	2
C	CAA	CAA	2
C	MES CODE - WFC-5A-1, DET. PROD. LJO EOS / W. FICKELI, 14	MES0	2
C	*****	MES0	3
C	CONTENTS	MES0	4
C	1. MAIN PROGRAM MES0	MES0	5
C	2. UTILITY	MES0	6
C	3. CALCULATION SECTIONS AND PRINT	MES0	7
C	4. CALCULATION CONTROLS	MES0	8
C	5. HEAD CONTROL (CON)	MES0	9
C	6. OUT OF PLACE	MES0	10
C	EQPS PACKAGE (SEC. 3)	MES0	11
C	HEAP (SEC.2)	MES0	12
C	7. DUMMIES	MES0	13
C		MES0	14
C	*****	MES0	15
C	1. MAIN PROGRAM	MES0	16
C	*****	MES0	17
	PROGRAM MES0(INP, OUT, FSETY=OUT, FSETIY=INP	MES0	18
	1. JOIN	MES0	19
	X)	MES0	20
C	***** COMMON *****	MES0	21
2	COMMON / (4000)	MES0	22
2	DIMENSION	MES0	23
	1 BS (60) ,CONT (20)	MES0	24
	2, KON (60)	MES0	25
2	EQUIVALENCE	MES0	26
	1 (7(400) ,BS) , (2(460) ,CONT)	MES0	27
	2 (2(1600) , KON)	MES0	28
C	***** LOCAL *****	MES0	29
2	DIMENSION EHS(40) ,ECONT(10)	MES0	30
	DATA EHS/	MES0	31
	1 1M , 3HPAS, 4HSALT, 3HFUB, 1M	MES0	32
	2, 3HUIP, 3HUIS, 3HUTG, 1M , 3HUEP	MES0	33
	3, 3HSEP, 3HTIP, 3HAIP, 3HEQP, 1M	MES0	34
	4, 3HSAH, 3HTED, 2HPV, 2HCV, 4HTEST	MES0	35
	5, 4HCEC, 1M , 4HSPC, 5HSPEC1, 1M	MES0	36
	6, 4HCORE, 4HDBUG, 4HLOAD, 1M , 1M	MES0	37
	7, 1M , 1M , 1M , 4HFCRM, 4HRENY	MES0	38
	8, 4HJEND, 1M , 1M , 3HCCN, 1M	MES0	39
	*/	MES0	40
C		MES0	41
	DATA ECONT/	MES0	42
	1 1.98719, 8.31439E-5, 1.01325E-6, 4.184E-2, 0.426012	MES0	43
	2, 3LOUT	MES0	44
	*/	MES0	45
	DATA JOIN /5LJOIN/,OUT /3LOUT/	MES0	46
2	INTEGER OUT	MES0	47
C	***** EXECUTE *****	MES0	48
2	CALL SEPR	MES0	49
3	CALL HEADI (MES0	50
	1 9L*MES1 = 76AUG20*	MES0	51
5	CALL MOVE (EHS,BS,40)	MES0	52
10	CALL MOVE (ECONT,CONT,10)	MES0	53
C	--- DATA STATEMENT CANT LOAD BLANK COMMON	MES0	54
C	----- PRINT DECK -----	MES0	55
13	CALL HEAD (5LINPUT)	MES0	56
C	----- HEAD CONTROL -----	MES0	57
15	CALL CON(0.)	MES0	58

17	END	MESU	59
	C*****	MESU	60
	C# Z. UTILITY	* MESU	61
	C*****	MESU	62
	SUBROUTINE DRUG(A,B)	DRUG	2
	C OLD ERR ROUTINE	DRUG	3
	C CHANGE DRUG CALLS TO ERR CALLS AS NEEDED	DRUG	4
6	CALL ERR(A,B,4LPDRUG)	DRUG	5
7	RETURN	DRUG	6
10	END	DRUG	7
	SUBROUTINE ERR(ISUB,IMES,ERRD)	ERR	2
	C*****	ERR	3
	C ERROR CONTROL	ERR	4
	C ARGS = ROUTINE, MESSAGE, DATA (10 WORDS)	ERR	5
	C*****	ERR	6
10	COMMON /4000/	ERR	7
10	DIMENSION KON(60), CONT(20)	ERR	8
10	EQUIVALENCE (Z(440),CONT), (Z(1690),KON)	ERR	9
10	EQUIVALENCE (CONT(0),OUT), (KON(6),QERRGAT)	ERR	10
10	COMMON /SEPRC/ SEPRCA(16)	ERR	11
	C*****	ERR	12
10	DIMENSION ILAB(5)	ERR	13
	DATA ILAB/30H///// ERROR (ERR CALL) IN = 0H,0L	ERR	14
	C*****	ERR	15
10	ILAB(1)=ISUB	ERR	16
	C----- 1. CHECK GATE - WARN IF CLOSED	ERR	17
10	IF(QERRGAT.EQ.0.) GOTO 150	ERR	18
12	PRINT 130, ILAB	ERR	19
	130 FORMAT(/// 30X,4(0////*), * ERR RE-ENTERED FROM 0,5A10///)	ERR	20
21	150 QERRGAT = QERRGAT * 1.0	ERR	21
23	IF(QERRGAT.GT. 1.) CALL EXIT	ERR	22
	C----- 2. PRINT HEAD ARGS, ERR -----	ERR	23
26	CALL HEAD (ILAB)	ERR	24
32	CALL PRINT (IMES, 10, ERRD)	ERR	25
36	IF (ISUB.EQ.4LSEPR) CALL UMPPR(OUT,SEPRCA)	ERR	26
44	CALL TRACE	ERR	27
47	CALL ERR(1,ERR)	ERR	28
	C----- 3. TERMINAL LINE -----	ERR	29
51	PRINT 800	ERR	30
	800 FORMAT(///21(5H0***), * END OF RUN AFTER ERR* ///)	ERR	31
61	CALL CUR(1.)	ERR	32
63	END	ERR	33
	SUBROUTINE ERP(L)	ERP	2
	C DIAGNOSTIC COMMON PRINT	ERP	3
3	COMMON /4000/	ERP	4
3	EQUIVALENCE	ERP	5
	1 (7(920),CAR), (Z(460),CONT), (Z(1000),DER), (Z(1010),EMG)	ERP	6
	2 (7(1030),EMN), (Z(1170),EMX), (Z(1370),FPU), (Z(1390),FVN)	ERP	7
	3 (7(1410),FCR), (Z(1490),GOM), (Z(1470),GP), (Z(1590),ME)	ERP	8
	4 (7(1600),KAL), (Z(1620),NEH), (Z(1680),KIM), (Z(1690),KON)	ERP	9
	5 (7(1750),PT), (Z(1800),NOT), (Z(1820),SM), (Z(1840),SP)	ERP	10
	6 (7(1880),SUC), (Z(1900),SUCG), (Z(1920),TMEH), (Z(1970),IMG)	ERP	11
	7 (7(1990),TMS), (Z(2010),IP), (Z(2210),XMT), (Z(2240),XMU)	ERP	12
	8 (Z(2260),XPF), (Z(2660),APG), (Z(3060),XPR), (Z(3080),XPT)	ERP	13

	X*(Z(400),RS),(Z(400),CA),(Z(600),EV),(Z(310),FLAB)	ENT	14
	Y*(Z(153),GMT),(Z(400),KEV),(Z(1860),SPC)	ENT	15
3	CALL PRINT(1L,0,0)	ENT	16
6	CALL PRINT(L,0,0)	ENT	17
11	CALL POUT(1)	ENT	18
13	CALL POUT(2)	ENT	19
15	CALL POUT(3)	ENT	20
17	CALL PRINT(PALCAR = CC/CH/CM/CG/CS/CE , 60, CAR)	ENT	21
22	CALL PRINT(3LDER,10,DER)	ENT	22
25	CALL PRINT(4LCONT,10,CONT)	ENT	23
30	CALL PRINT(3LEMG,10,EMG)	ENT	24
33	CALL PRINT(3LEMN,10,EMN)	ENT	25
36	CALL PRINT(3LEMX,10,EMX)	ENT	26
41	CALL PRINT(3LFMU,10,FMU)	ENT	27
44	CALL PRINT(2LFN,10,FN)	ENT	28
47	CALL PRINT(3LF0B,40,F0B)	ENT	29
52	CALL PRINT(2LGM,30,GM)	ENT	30
55	CALL PRINT(2LGP,10,GP)	ENT	31
60	CALL PRINT(2LHE,10,HE)	ENT	32
63	CALL PRINT(2LHS,50,HS)	ENT	33
66	CALL PRINT(2LEA,80,EA)	ENT	34
71	CALL PRINT(2LEV,10,EV)	ENT	35
74	CALL PRINT(4LFLAB,10,FLAB)	ENT	36
77	CALL PRINT(3LGMT,10,GMT)	ENT	37
102	CALL PRINT(3LKEV,10,KEV)	ENT	38
105	CALL PRINT(3LSPC,10,SPC)	ENT	39
110	CALL PRINT(3LKAL,12,KAL)	ENT	40
113	CALL PRINT(3LKUN,40,KUN)	ENT	41
116	CALL PRINT(3LKEN,20,KEN)	ENT	42
121	CALL PRINT(3LKIM,10,KIM)	ENT	43
124	CALL PRINT(2LPT,10,PT)	ENT	44
127	CALL PRINT(4LRHOT,10,RHOT)	ENT	45
132	CALL PRINT(2LSM,20,SM)	ENT	46
135	CALL PRINT(2LSP,20,SP)	ENT	47
140	CALL PRINT(3LSUC,10,SUC)	ENT	48
143	CALL PRINT(4LSUCG,10,SUCG)	ENT	49
146	CALL PRINT(4LTHEM,40,THEM)	ENT	50
151	CALL PRINT(3LTMG,10,TMG)	ENT	51
154	CALL PRINT(3LTMS,20,TMS)	ENT	52
157	CALL PRINT(2LTP,40,TP)	ENT	53
162	CALL PRINT(3LXMT,20,XMT)	ENT	54
165	CALL PRINT(3LXMU,10,XMU)	ENT	55
170	CALL PRINT(3LXPF,10,XPF)	ENT	56
173	CALL PRINT(3LXPG,10,XPG)	ENT	57
176	CALL PRINT(3LXPR,10,XPR)	ENT	58
201	CALL PRINT(3LXPT,10,XPT)	ENT	59
204	RETURN	ENT	60
205	END	ENT	61

	SUBROUTINE FIO (H,FMT,N,A,KL)	FIG	2
C		FIG	3
C	H=HEAD ,WIT ,PRINT ,WUI	FIG	4
C	FMT=FORMAT	FIG	5
C	N=NUMBER OF WORDS OF ARRAY A FOR I.O.	FIG	6
C	FOR N=0,FMT IS HOLLERITH ARGUMENT LABEL	FIG	7
C	KL IS THE WORD LENGTH OF THE LABEL.	FIG	8
14	DIMENSION BS(4),FMT(60),A(10)	FIG	9
14	INTEGER H,FMT,BS	FIG	10
C		FIG	11

C		BS(1)=READ , BS(2)=KIT	FIG	12
C		BS(3)=PRINT , BS(4)=WOT	FIG	13
14		BS(1)=4=READ	FIG	14
14		BS(2)=3=KIT	FIG	15
14		BS(3)=5=PRINT	FIG	16
14		BS(4)=3=WOT	FIG	17
C			FIG	18
21		DO 24 J=1,4	FIG	19
23		I=J	FIG	20
23		IF (H.EQ.BS(I))GO TO 30	FIG	21
26	24	CONTINUE	FIG	22
30		WRITE(9,26)H	FIG	23
	26	FORMAT (14H0 F10 -BAD ARG= A6)	FIG	24
40		CALL EXIT(3)	FIG	25
45	30	IF (N)200,100,200	FIG	26
C		I.O. WITH NO DATA	FIG	27
46	100	GO TO (500,500,130,140),I	FIG	28
C			FIG	29
C			FIG	30
56	130	WRITE (2,150)(FMT(J),J=1,KL)	FIG	31
67		GO TO 500	FIG	32
C			FIG	33
C			FIG	34
73	140	WRITE (9,150)(FMT(J),J=1,KL)	FIG	35
104		GO TO 500	FIG	36
	150	FORMAT (12A6)	FIG	37
C		I.O. WITH DATA	FIG	38
110	200	GO TO (210,220,230,240),I	FIG	39
C			FIG	40
120	210	READ (2,FMT)(A(J),J=1,N)	FIG	41
132		GO TO 500	FIG	42
C			FIG	43
136	220	READ(10,FMT)(A(J),J=1,N)	FIG	44
150		GO TO 500	FIG	45
C			FIG	46
154	230	WRITE (2,FMT)(A(J),J=1,N)	FIG	47
166		GO TO 500	FIG	48
C			FIG	49
172	240	WRITE(9,FMT)(A(J),J=1,N)	FIG	50
204		GO TO 500	FIG	51
C			FIG	52
210	500	CONTINUE	FIG	53
210	510	CONTINUE	FIG	54
210	520	RETURN	FIG	55
211		END	FIG	56

C	SUBROUTINE FROTT(C,K)	FROTT	2
C		FROTT	3
C		FROTT	4
C		FROTT	5
C		FROTT	6
C		FROTT	7
C		FROTT	8
C		FROTT	9
C		FROTT	10
C		FROTT	11
C		FROTT	12
C		FROTT	13
C		FROTT	14
6	EQUIVALENCE (E1,KC1),(E2,KC2)	FROTT	14

6	DIMENSION C(10)	FRCUTT	15
6	8 E1=C(8)	FRCUTT	16
10	9 E2=C(9)	FRCUTT	17
12	10 IF (K)50,20,50	FRCUTT	18
13	20 CALL FRCUT (C)	FRCUTT	19
17	30 GO TO 210	FRCUTT	20
20	50 IF(KC1)100,60,100	FRCUTT	21
21	60 C(2)=C(5)	FRCUTT	22
23	70 GO TO 102	FRCUTT	23
24	100 C(2)=C(2)+C(6)	FRCUTT	24
26	102 KC1=KC1+1	FRCUTT	25
30	110 IF ((C(2)-C(7))*C(6)) 150,150,120	FRCUTT	26
34	120 KC2=1	FRCUTT	27
35	130 GO TO 200	FRCUTT	28
36	150 KC2=2	FRCUTT	29
37	200 C(8)=E1	FRCUTT	30
41	202 C(9)=E2	FRCUTT	31
43	210 RETURN	FRCUTT	32
44	END	FRCUTT	33
C*****		GEP	2
C*	3. CALCULATION SECTIONS	* GEP	3
C*****		GEP	4
SUBROUTINE GEP(K)		GEP	5
C	K=1 - CALCULATE PURE GAS EOS AT GIVEN T,P	GEP	6
C	K=2 - APPROXIMATE SAME BY LM EXPANSION	GEP	7
C	CALLED BY XIM	GEP	8
C	----- SPECS -----	GEP	9
C	K=1	GEP	10
C	REGULAR CALCULATION OF GAS EOS FOR PURE	GEP	11
C	SPECIES AT GIVEN T,P BY ITERATIVE SOLUTION	GEP	12
C	OF P(T,V)=P, WITH P(T,V) GIVEN BY GEM.	GEP	13
C	FOR CS OR 1-FLUID MIX, THIS CAN BE A MIXTURE	GEP	14
C	EOS VIA COMPOSITION DEPENDENCE OF THE	GEP	15
C	MEAN RSTAR AND TSTAR.	GEP	16
C	INPUT	GEP	17
C	P=TPER(1)	GEP	18
C	IMPLICIT FOR GEM -	GEP	19
C	T=TPER(1)	GEP	20
C	MEAN RSTAR, TSTAR = RSTA=GP(5), TSTA=GP(6)	GEP	21
C	KAL(5) = 1,2,3 FOR IDEAL,EQU, KW	GEP	22
C	OUTPUT	GEP	23
C	V=VR=GM(15) - VOLUME	GEP	24
C	IMPLICIT FROM GEM -	GEP	25
C	GM - STATE POINT	GEP	26
C	VARIABLES	GEP	27
C	PG=GM(16) - CALCULATED (GAS) PRESSURE	GEP	28
C	URL, URU - LOWER AND UPPER LIMITS ON ITERATION V	GEP	29
C	ROUTINES	GEP	30
C	GEM(2) - PURE-FLUID EOS AT T,P	GEP	31
C	FRCUTT - ITERATE	GEP	32
C	PLAN	GEP	33
C	SOLVE ITERATIVELY PG(V,T)=P FOR V(=VR) BY	GEP	34
C	FROOT ITERATION.	GEP	35
C	VARIABLE, FUNTION = LOG(V), LOG(P/PG)	GEP	36
C	SECOND GUESS - NEWTON-RAPHSON FROM DP/DV=GM(12)	GEP	37
C	K=2	GEP	38
C	INPUT	GEP	39
C		GEP	40

C	1,P=THER(1),(3)	GET	41
C	GM = STATE POINT FROM PREVIOUS K=1 CALCULATION	GET	42
C	(GEM(2) OUTPUT)	GET	43
C	EMX(2,...) = (GAS) MOLE FRACTIONS	GET	44
C	OUTPUT	GET	45
C	XMT = MIXTURE STATE POINT	GET	46
C	(NOTE = CHEMICAL POTENTIALS IN XMU ARE	GET	47
C	CALCULATED BY CALLER)	GET	48
C	VARIABLES	GET	49
C	EV = 1,2 = TSTAR AND RSTAR DISPLACEMENTS	GET	50
C	3,5 = EXPANSION COEFFICIENTS	GET	51
C		GET	52
3	COMMON Z(4000)	GET	53
3	DIMENSION	GET	54
	1,CAR (80),CONT (20),EV (20)	GET	55
	2,FOH (40),GM (40),KEN (60)	GET	56
	3,KON (6,10),THER (50),XMT (30)	GET	57
	4,GP(20)	GET	58
3	EQUIVALENCE	GET	59
	1,(Z(921),CAR),(Z(460),CONT),(Z(680),EV)	GET	60
	2,(Z(1410),FOH),(Z(1490),GM),(Z(1620),KEN)	GET	61
	3,(Z(1640),KON),(Z(1720),THER),(Z(2210),XMT)	GET	62
	4,(Z(1470),GP)	GET	63
3	DIMENSION CG(10),KCG(2)	GET	64
C		GET	65
3	EQUIVALENCE	GET	66
	1,(CAR(3),CG),(CG(4),KCG)	GET	67
	2,(CONT(2),R)	GET	68
	3,(FOH(2),VRU),(FOH(1),VKL)	GET	69
	4,(GM(15),VR),(GM(10),PG)	GET	70
	5,(THER(1),P),(THER(3),T)	GET	71
	6,(GP(5),RSTAR),(GP(6),TSTAR)	GET	72
	7,(XMT(16),RSTAR),(XMT(17),TSTAR)	GET	73
C		GET	74
C		GET	75
3	4 GO TO (10,300),K	GET	76
C	----- K=1 - REGULAR -----	GET	77
11	10 IF (VR) 20,12,0	GET	78
12	12 VR=10.0	GET	79
14	20 CG(4)=ALOG(VR)	GET	80
20	22 CALL COUT (3HGEF,1)	GET	81
24	40 KCG(1)=0	GET	82
C		GET	83
25	50 CALL FROTT (CG,KON(4,8))	GET	84
31	52 KEXIT=KCG(2)	GET	85
33	60 GO TO (150,PR,80,70),KEXI!	GET	86
43	70 CALL DRIG (3HGEF,1)	GET	87
47	72 GO TO 150	GET	88
50	80 CALL CBUG (3HGEF,2)	GET	89
54	82 GO TO 150	GET	90
50	88 IF (KON(4,8)) 92,90,92	GET	91
50	90 IF (KCG(1)-2)92,41,92	GET	92
60	91 CG(2)=CG(4)-CG(3)*PG/(VR*GM(12))	GET	93
65	92 VR=EXP(CG(2))	GET	94
71	93 IF (VRU-VR)94,94,90	GET	95
74	94 VR=VRU	GET	96
76	95 GO TO 90	GET	97
77	96 IF (VR=VKL) 97,97,98	GET	98
102	97 VR=VKL	GET	99
104	98 KEN(11)=KEN(11)+1	GET	100

```

104 100 CALL GEP(2)
111 105 IF (MG)104,110,110
113 106 IF (VHL-VR/3.)107,97,97
117 107 VR=VR/3.
121 108 GO TO 110
122 110 CG(3)=ALOG(PG/P)
130 112 CG(2)=ALOG(VR)
134 120 CALL DOUT (3MGEP,2)
140 130 GO TO 50
141 150 CALL DOUT (3MGEP,3)
145 160 GO TO 600
GEP 101
GEP 102
GEP 103
GEP 104
GEP 105
GEP 106
GEP 107
GEP 108
GEP 109
GEP 110
GEP 111
C----- K=2 - LM EXPANSION -----
146 200 EV(1)=TSTAT/TSTA-1.0
151 210 EV(2)=RSTAT/RSTA-1.0
GEP 112
GEP 113
GEP 114
C 400
GEP 115
C 410 E COMPUTE THERMO OUTPUT
GEP 116
154 412 EV(3)=GM(4)*EV(1)+3.0*GM(10)*EV(2)
GEP 117
161 420 EV(4)=-((GM(14)+P/GM(12))*EV(1)
GEP 118
1 430 +3.0*(GM(15)+P/GM(12))*EV(2)
GEP 119
172 430 EV(5)=(GM(8)+(T*GM(13)-P)*(GM(14)/R))*EV(1)
GEP 120
1 440 +3.0*(P*GM(14)/R-1.0)*EV(2)
GEP 121
206 500 XMT(1)=GM(15)+EV(4)
GEP 122
210 510 XMT(2)=GM(4)+EV(3)-(P/(R*1))*EV(4)-EV(5)
GEP 123
217 520 XMT(7)=P*XMT(1)/(R*1)-1.0
GEP 124
224 530 XMT(3)=XMT(2)+XMT(7)
GEP 125
227 540 XMT(5)=GM(5)+EV(3)
GEP 126
230 550 XMT(4)=XMT(5)-XMT(7)
GEP 127
232 560 XMT(6)=GM(11)-EV(5)
GEP 128
234 570 XMT(8)=XMT(1)-XMT/P
GEP 129
C 580 U
GEP 130
C
GEP 131
240 590 CALL DOUT (3MGEP,4)
GEP 132
C
GEP 133
244 600 RETURN
GEP 134
C
GEP 135
C SPECS (FOR PART 2)
GEP 136
C
GEP 137
C IN OUT EXASE
GEP 138
C
GEP 139
C NOTE - Z=PV/RT
GEP 140
C 1 P
GEP 141
C 2 MX
GEP 142
C 3 GM
GEP 143
C 4 1
GEP 144
C 5 2 ERP/RT
GEP 145
C 6 3 FRP/RT
GEP 146
C 7 4 SRP/H
GEP 147
C 8 5 ERP/RT
GEP 148
C 9 6 SRP/H
GEP 149
C 10 7 ZGP
GEP 150
C 11 8 VGP
GEP 151
C 12 9 7RP
GEP 152
C 13 10 SRP/H
GEP 153
C 14 11 D P/U VR
GEP 154
C 15 12 D P/U T
GEP 155
C 16 13 D VR/D T
GEP 156
C 17 14 VR
GEP 157
C
GEP 158
C XMU MUGP/RT
GEP 159
C
GEP 160

```


	SUBROUTINE GEM (K)	GEM	2
C	PURE GAS FOS AT GIVEN T,V	GEM	3
C	-----	GEM	4
C	K=1 PRELIM. READ INPUT PACKS AND FOR LJD	GEM	5
C	CALL GES (1,...) FOR PRELIMINARY PROCESSING (SETS UP GP).	GEM	6
C	CALLED BY CON	GEM	7
C	K=2: MAIN. CALCULATE STATE POINT; KAL(3)=	GEM	8
C	0 = IDEAL GAS; LOCAL	GEM	9
C	9 = KW EOS; CALL HKW	GEM	10
C	OTHER = LJD EOS; CALL GES(2,...)	GEM	11
C	-----	GEM	12
C	MAIN (K=2) SPECS	GEM	13
C	INPUT	GEM	14
C	T=TEMP(3)	GEM	15
C	V=VR=GM(15)	GEM	16
C	ISTAVSTA=GP(6),(7) - ISTAV, VSTA. THESE ARE	GEM	17
C	COMPOSITION DEPENDENT FOR LM AND L-FLUID MIX.	GEM	18
C	KAL(3) - FOS CHOICE. SEE ABOVE	GEM	19
C	OUTPUT	GEM	20
C	GM = STATE POINT. GM IS REARRANGED AND	GEM	21
C	FILLER OUT HERE.	GEM	22
C	NOTES	GEM	23
C	1. NO IDEAL-GAS BRANCH IN PRELIM FOR THIS	GEM	24
C	CASE; GEM PACK SHOULD NOT BE ENTERED.	GEM	25
C	2. POOR LOGICAL ORGANIZATION: HKW WAS ADDED	GEM	26
C	LATE WITH BRANCH UNDER LJD. IDEAL	GEM	27
C	GAS, KW, AND LJD SHOULD ALL HAVE SAME LEVEL.	GEM	28
C	3. I DO NOT NOW (WF 1/75) UNDERSTAND WHY	GEM	29
C	TMS (IDEAL PART) IS USED IN CPM. IT SEEMS TO	GEM	30
C	ME IT SHOULD BE AN	GEM	31
C	IMPERFECTION QUANTITY LIKE THE OTHERS.	GEM	32
C	***** COMMONS *****	GEM	33
3	COMMON Z(4000)	GEM	34
3	DIMENSION	GEM	35
	1 CONT (20) ,GP (20) ,GM (40)	GEM	36
	2,KAL (20) ,KEN (6,10) ,KUN (6,10)	GEM	37
	3,TEMP (50) ,TMS (20)	GEM	38
3	DIMENSION KE(6)	GEM	39
3	EQUIVALENCE	GEM	40
	1 (Z(460) ,CONT) ,(Z(1470) ,GP) ,(Z(1490) ,GM)	GEM	41
	2,(Z(1600) ,KAL) ,(Z(1620) ,KEN) ,(Z(1690) ,KUN)	GEM	42
	3,(Z(1920) ,TEMP) ,(Z(1990) ,TMS)	GEM	43
C		GEM	44
C	LOCAL EQ	GEM	45
C		GEM	46
3	EQUIVALENCE (GP(A),TSTA),(GP(I),VSTA)	GEM	47
	1 ,(GM(1),TAU),(GM(2),THEIA),(GM(16),PG)	GEM	48
	2 ,(TEMP(3),T),(CONT(),K)	GEM	49
	3 ,(GM(15),VR)	GEM	50
C		GEM	51
3	EQUIVALENCE (GM(25),GAM),(GM(26),ALPH),(GM(27),DEL)	GEM	52
	1 ,(GM(28),CGAM),(GM(29),CPH),(GM(30),ULVUT)	GEM	53
C		GEM	54
C		GEM	55
3	100 GO TO (1000,2000),K	GEM	56
C	994	GEM	57
C	996 PRELIMINARY	GEM	58

	C 098			GEM	59
11	1000	CALL REAP (GEM	60
	1	KON0 POT (1-LJ,2-MCM,3-MK) *W (NUM 1) / N*H,AN,AM,R*,T*S		GEM	61
		1: *-P*KE)		GEM	62
14		CALL REAP(0,6,GP)		GEM	63
20	1010	KE(3)=0		GEM	64
21	1012	KE(4)=0		GEM	65
22	1020	KE(5)=KON(1,4)		GEM	66
24	1022	KE(6)=KON(2,4)		GEM	67
26	1024	IF (KE(1)-9) 1030,1025,1030		GEM	68
30	1025	KAL(3)=9		GEM	69
31	1026	VSTA=1.0		GEM	70
33	1027	I STA=1.0		GEM	71
35	1028	GO TO 3000		GEM	72
36	1030	CALL GES(1,KE,GP,GM)		GEM	73
43	1040	CALL PRIN(4HV*S,1,VSTA)		GEM	74
47	1050	KAL(1)=1		GEM	75
50	1060	GO TO 3000		GEM	76
	C1094			GEM	77
	C1096	MAIN		GEM	78
	C1098			GEM	79
51	2000	KEN(1)=KEN(1)+1		GEM	80
53	2002	E1 = V0		GEM	81
	C2004			GEM	82
	C2006	IDEAL		GEM	83
55	2010	IF (KAL(3)) 2200,2050,2200		GEM	84
56	2050	DO 2060 I=3,15		GEM	85
63	2060	GM(1)=0.0		GEM	86
65	2070	GM(3)=1.0		GEM	87
67	2080	GM(4)=1.0		GEM	88
71	2090	GM(14)=1.0		GEM	89
73	2100	GO TO 2300		GEM	90
	C2194			GEM	91
	C2196	LJU		GEM	92
74	2200	TAN=VR/VSTA		GEM	93
76	2210	THETA=T/I STA		GEM	94
100	2220	KE(5)=KON(1,4)		GEM	95
102	2230	KE(6)=KON(2,4)		GEM	96
	C			GEM	97
104	2234	IF (KAL(3)-9) 2240,2236,2240	KW	GEM	98
106	2236	CALL HKW(1)		GEM	99
111	2238	GO TO 2300		GEM	100
	C			GEM	101
112	2240	CALL GES (2,KE,GP,GM)		GEM	102
	C	REARRANGE AND FINISH GM		GEM	103
117	2300	GM(22)=GM(15)		GEM	104
121	2310	GM(21)=GM(14)		GEM	105
123	2320	GM(20)=GM(6)		GEM	106
125	2330	GM(19)=GM(13)		GEM	107
127	2340	GM(18)=GM(12)		GEM	108
131	2350	GM(17)=GM(5)		GEM	109
133	2352	VP = E1		GEM	110
135	2360	PG=GM(3)*R*T/VR		GEM	111
141	2370	GM(15)=VR		GEM	112
143	2380	GM(12)=(R*T/VR**2)*(GM(10)-GM(3))		GEM	113
150	2390	GM(13)=(2/VR)*GM(9)		GEM	114
153	2400	GM(14)=-GM(13)/GM(12)		GEM	115
155	2410	E1=GM(11)		GEM	116
157	2412	E2=GM(7)		GEM	117
161	2420	GM(11)=GM(8)		GEM	118

163	2430	GM(7)=GM(10)	GET	119
165	2440	GM(8)=GM(9)	GET	120
167	2450	GM(10)=GM(3)-1.0	GET	121
172	2460	GM(9)=VR-R*P/PG	GET	122
176	2470	GM(8)=E1	GET	123
200	2490	GM(5)=E2	GET	124
	C2496		GET	125
202	2500	KEN(1,4)=KE(3)	GET	126
204	2510	KEN(2,4)=KE(4)	GET	127
	C		GET	128
206	2514	CGAM=-VR*GM(12)/PG	GET	129
211	2520	CVR=IMS(7)-1.0+GM(8)	GET	130
215	2524	ULVDI=GM(14)/VR	GET	131
217	2530	GAM=CGAM*(1.0+CGAM*GM(3) * (1*ULVDI)**2/CVR)	GET	132
225	2534	HET=1.0/(CGAM*GM(3) * T*ULVDI/CVR)	GET	133
232	2540	ALPH=GAM*HET-1.0	GET	134
235	2544	CPR=CVR*GAM/CGAM	GET	135
	C2544		GET	136
240	2600	CALL DOUT (3HGEM,1)	GET	137
	C2944		GET	138
244	3000	RETURN	GET	139
245		END)	GET	140

		SUBROUTINE GES (K,L,GP,GM)	GES	2
	C		GES	3
	C	LJD CELL THEORY GAS EQN. STATE SUBROUTINE	GES	4
	C		GES	5
	C	REVISION 1. CORRECT MINOR ERROR =	GES	6
	C	POINTS 14 AND 16 USE A FOR 13 AND 15	GES	7
	C	W. F. 1/5/62	GES	8
	C		GES	9
	C	REVISION 2. CHANGE UBS. CALL ON NEG. KAP PRINT	GES	10
	C	W. F. 2/26/62	GES	11
	C		GES	12
	C		GES	13
12	10	DIMENSION A(8),Y(4),S(7),W(5),W1(5),W2(5),	GES	14
	1	C(4),GM(15),G(15),UP(7),L(6),E(10)	GES	15
12		EQUIVALENCE (G(1),IAU),(G(2),IMETA),(G(15),B),(W,X)	GES	16
	C 96		GES	17
	C 98	PREL.=MAIN BRANCH	GES	18
12	100	GO TO (200,1000),K	GES	19
20	200	Y(1)=0.94940693	GES	20
22	202	Y(2)=0.94457502	GES	21
24	204	Y(3)=0.85562120	GES	22
26	206	Y(4)=0.75541441	GES	23
30	208	Y(5)=0.61787624	GES	24
32	210	Y(6)=0.45001678	GES	25
34	212	Y(7)=0.24160755	GES	26
36	214	Y(8)=0.045012510	GES	27
40	220	A(1)=0.077152459	GES	28
42	222	A(2)=0.062253524	GES	29
44	224	A(3)=0.05158512	GES	30
46	226	A(4)=0.12462897	GES	31
50	228	A(5)=0.14959599	GES	32
52	230	A(6)=0.16015652	GES	33
54	232	A(7)=0.18260342	GES	34
56	234	A(8)=0.18945061	GES	35
60	240	u=0.276335	GES	36
62	242	BMAX=0.276335	GES	37

64	244	BUP=1.0667420	GE3	38
66	246	BDDWN=0.97778543	GE3	39
70	248	EPS=18.0	GE3	40
72	250	GP(7)=0.426012*GP(5)**3	GE3	41
75	250	CALL WR(1,L,GP)	GE3	42
102	310	GO TO 5000	GE3	43
	C 990		GE3	44
	C 992	MAIN ENTRY	GE3	45
	C 994	INITIAL	GE3	46
103	1000	TAU=GM(1)	GE3	47
104	1010	THETA=GM(2)	GE3	48
106	1012	L(3)=L(3)+1	GE3	49
110	1020	IF (TAU)1040,1040,1030	GE3	50
112	1030	IF (THETA)1040,1040,1050	GE3	51
114	1040	CALL DBUG(3HGES,1)	GE3	52
122	1050	CH(1)=TAU	GE3	53
124	1060	CALL WR (2,L,CH)	GE3	54
132	1070	KE1=0	GE3	55
133	1080	IF (L(5)) 4000,1200,4000	GE3	56
	C1190	FIND LIMIT	GE3	57
134	1200	W1=H*(1.0+Y(1))	GE3	58
137	1210	CALL WR (3,L,W1)	GE3	59
145	1220	IF ((W1(3)- ABS(CH(2)))/THETA-EPS) 1400,1400,1250	GE3	60
	C1238		GE3	61
	C1240	CHECK AND LOWER	GE3	62
153	1250	W2=H*(1.0+Y(3))	GE3	63
156	1260	CALL WR (3,L,W2)	GE3	64
164	1270	IF ((W2(3)- ABS(CH(2)))/THETA-EPS) 1600,1600,1300	GE3	65
172	1300	KE1=KE1+1	GE3	66
174	1310	DO 1320 I=1,5	GE3	67
201	1320	W1(I)=W2(I)	GE3	68
205	1330	B=R*H*DOWN	GE3	69
207	1340	IF (L(5)) 4100,1250,4100	GE3	70
	C1394		GE3	71
	C1396	RAISE	GE3	72
211	1400	IF (B-BMAX)1450,1410,1410	GE3	73
214	1410	W2=H*(1.0+Y(3))	GE3	74
217	1420	CALL WR (3,L,W2)	GE3	75
225	1430	GO TO 1600	GE3	76
226	1450	DO 1460 I=1,5	GE3	77
233	1460	W2(I)=W1(I)	GE3	78
237	1470	B=R*H*UP	GE3	79
241	1472	IF (L(5))4150,1474,4150	GE3	80
242	1474	KE1=KE1+1	GE3	81
244	1480	IF (B-BMAX) 1520,1520,1490	GE3	82
247	1490	B=BMAX	GE3	83
251	1500	W2=H*(1.0+Y(3))	GE3	84
254	1510	CALL WR (3,L,W2)	GE3	85
262	1520	W1=H*(1.0+Y(1))	GE3	86
265	1530	CALL WR(3,L,W1)	GE3	87
273	1540	IF ((W1(3)- ABS(CH(2)))/THETA-EPS) 1550,1600,1600	GE3	88
301	1550	IF (B-BMAX) 1450,1600,1600	GE3	89
	C1596	FINISH	GE3	90
304	1600	KE2=KE1+KE2	GE3	91
306	1610	L(4)=KE2/L(3)	GE3	92
	C1096		GE3	93
	C1098	INTEGRATE	GE3	94
312	2000	DO 2010 I=1,7	GE3	95
317	2010	S(I)=0.0	GE3	96
	C2048		GE3	97

323	2050	DO 2550	IG=1,16	GE5	98
325	2060	IF (IG-14)	2100,2070,2100	GE5	99
327	2070	DO 2080	I=1,5	GE5	100
334	2080	W(I)=W2(I)		GE5	101
340	2082	KE=17-IG		GE5	102
342	2090	GO TO 2400		GE5	103
343	2100	IF (IG-16)	2150,2110,2150	GE5	104
345	2110	DO 2150	I=1,5	GE5	105
352	2120	W(I)=W1(I)		GE5	106
356	2122	KE=17-IG		GE5	107
360	2130	GO TO 2400		GE5	108
		C		GE5	109
361	2150	IF (IG-8)	2160,2160,2200	GE5	110
364	2160	X=R*(1.0-Y(IG))		GE5	111
370	2170	KE=IG		GE5	112
372	2180	GO TO 2300		GE5	113
		C2198		GE5	114
373	2200	KE=17-IG		GE5	115
375	2210	X=R*(.1+.9*Y(KE))		GE5	116
		C2298		GE5	117
401	2300	CALL WR(J,L,W)		GE5	118
		C2398		GE5	119
			CALC. INTEGRANDS	GE5	119
407	2400	E(1)=A(KE)*W(2)*EXP(-W(3)/THETA)		GE5	120
421	2410	E(2)=W(4)*E(1)		GE5	121
423	2420	E(3)=W(7)*E(1)		GE5	122
425	2430	E(4)=W(4)*E(2)		GE5	123
427	2440	E(5)=W(7)*E(3)		GE5	124
431	2450	E(6)=W(7)*E(2)		GE5	125
433	2460	E(7)=W(5)*E(1)		GE5	126
		C2498		GE5	127
435	2500	DO 2510	I=1,7	GE5	128
442	2510	S(I)=E(I)+S(I)		GE5	129
		C		GE5	130
			---NOTE - SUM S(I) IS 1/2 INTEGRAL	GE5	130
		C2538		GE5	131
447	2540	IF (L(5))	4200,2550,4200	GE5	132
450	2550	CONTINUE		GE5	133
		C2994		GE5	134
		C2996		GE5	135
		C2998		GE5	136
			CALC OUTPUT	GE5	136
			INTEGRALS	GE5	137
452	3000	DO 3010	I=2,7	GE5	137
457	3010	S(I)=2(I)/S(I)		GE5	138
464	3020	TM=1./THETA		GE5	139
466	3030	S(1)=2.0*R*S(1)		GE5	140
471	3032	G(12)=TM*CH(3)		GE5	141
473	3040	G(7)=1.0+G(12)-TM*S(2)		GE5	142
477	3042	G(13)=-TM*CH(2)		GE5	143
501	3050	G(4)=G(13)+TM*S(3)		GE5	144
504	3052	G(14)=8.4857662*S(1)		GE5	145
506	3060	G(6)=1.0+G(13)-ALOG(G(14))		GE5	146
516	3070	IF (G(3))	3080,3080,3100	GE5	147
520	3080	CALL PRIN(14HG5 NEG. KAP S,1,G(3))		GE5	148
525		CALL PRIN(4HTAU5,1,TAU)		GE5	149
533	3090	GO TO 3110		GE5	150
534	3100	G(6)=G(6)-ALOG(G(3))		GE5	151
542	3110	E2=TM*TM		GE5	152
544	3120	G(9)=1.0-F2*(S(6)-S(3)*S(2))		GE5	153
551	3130	G(10)=TM*CH(4)+E2*(S(4)-S(2)**2-THETA*S(7))		GE5	154
560	3140	G(11)=E2*(S(5)-S(3)**2)		GE5	155
		C		GE5	156
563	3150	G(5)=G(4)+G(3)-1.0		GE5	157

567	3160	G(7)=G(6)+G(3)-1.0	GES	158
573	3170	G(8)=G(4)-G(6)	GES	159
	C		GES	160
575	3200	DO 3210 I=3,15	GES	161
602	3210	GM(I)=G(I)	GES	162
606	3220	IF(L(5)) 4300,5000,4300	GES	163
	C3094		GES	164
	C3096	DIAGNOSTIC PRINT	GES	165
	C3098		GES	166
610	4000	CALL PRIN (28H GES DIAG. -TAU,THE[A,B S,0,8)	GES	167
616	4010	E(1)=TAU	GES	168
620	4020	E(2)=THETA	GES	169
622	4030	E(3)=B	GES	170
624	4040	CALL PRIN (2H S,3,E)	GES	171
632	4050	GO TO 1200	GES	172
633	4100	CALL PRIN (2HRS,1,B)	GES	173
641	4110	GO TO 1250	GES	174
642	4150	CALL PRIN (2HRS,1,B)	GES	175
650	4160	GO TO 1474	GES	176
651	4200	DO 4210 I=1,7	GES	177
661	4210	E(I)=E(I)/A(KE)	GES	178
665	4220	E(N)=IG	GES	179
667	4230	E(N)=X	GES	180
671	4240	E(10)=W(3)	GES	181
673	4250	CALL PRIN(7MI,X,W S,3,E(8))	GES	182
700		CALL PRIN(7MINTS S,7,E)	GES	183
706	4260	GO TO 2550	GES	184
707	4300	CALL PRIN(7MG(OUT)S,15,G)	GES	185
712		CALL PRIN(7MS(INT)S,S)	GES	186
	C4090		GES	187
717	5000	RETURN	GES	188
720		END	GES	189

		SUBROUTINE WR(K,L,U)	WR	2
	C	GES CELL POTENTIAL	WR	3
10	20	DIMENSION CC(6),C(6),WN(6),WC(6),W(6)	WR	4
	1	,KFPS(2),NMAX(2),F(9),A(60),AL(30),D(7),L(6)	WR	5
10	30	EQUIVALENCE (WN,CC(7)),(KUNE,UNE),(KY,Y)	WR	6
	1	,(A(31),AL)	WR	7
10	200	GO TO (1000,2000,3000),K	WR	8
	C 090		WR	9
	C 094	PRELIM. ENTRY	WR	10
	C 096		WR	11
	C 098	SET POT. AND EQUIV. ANGS	WR	12
17	1000	DO 1004 I=1,6	WR	13
21	1002	* (I)=0.0	WR	14
23	1004	C(I)=0.0	WR	15
25	1006	M=30	WR	16
26	1010	GO TO (1020,1040,1060),L	WR	17
35	1020	KA=1	WR	18
36	1022	KR=1	WR	19
37	1030	GO TO 1100	WR	20
40	1040	KA=2	WR	21
41	1042	KR=2	WR	22
42	1050	GO TO 1100	WR	23
43	1060	KA=1	WR	24
44	1062	KR=2	WR	25
	C1070		WR	26
	C		WR	27

45	1100	FN=D(1)	WR	28
46	1110	FM=D(2)	WR	29
50	1120	AN=D(3)	WR	30
52	1130	AM=D(4)	WR	31
	C1140		WR	32
	C1144		WR	33
54	1200	IF (AN) 1400,1800,1210	WR	34
	C		WR	35
56	1210	G=FN	WR	36
60	1212	GB=FM	WR	37
62	1220	AG=AN	WR	38
64	1230	KB=KR	WR	39
66	1240	KQ=1	WR	40
	C1240		WR	41
	C1244		WR	42
67	1300	BB= 12.0*GB/(FN-FM)	WR	43
73	1310	AA=-AG*BB/2.0	WR	44
	C1320		WR	45
76	1330	GO TO (1350,1650),KB	WR	46
	C1344		WR	47
	C1348		WR	48
		LJ	WR	49
104	1350	J=(KQ-1)*M	WR	50
110	1352	KE1=J+M	WR	51
112	1360	A(KE1)=G*(G-1.0)/6.0	WR	52
117	1370	E=A(KE1)/4.0	WR	53
122	1380	E1=1.0E-7*E	WR	54
	C1384		WR	55
124	1400	DO 1480 I=2,M	WR	56
126	1410	KE=KE1+1-I	WR	57
131	1420	E2=2*(I-1)	WR	58
134	1440	E3=(G+E2)*((G+E2)-1.0)/((E2+3.0)*(E2+2.0))	WR	59
144	1450	A(KE)=E3*A(KE+1)	WR	60
147	1460	E=E3*E/4.0	WR	61
152	1470	IF (E1-E) 1480,1480,1510	WR	62
155	1480	CONTINUE	WR	63
	C1488		WR	64
160	1500	CALL FIO (3*WOT, 1 53H (140,12X,32H A=DIM. TOO SMALL, A30*1/4**30= 1PE15.7), 21,A(J+1),0)	WR	65
	C1508		WR	66
171	1510	WMAX(KQ)=1	WR	67
173	1520	KEPS(KQ)=-ALOG(1.0E-7*A(KE1)/A(KE))/0.6931	WR	68
	C1544		WR	69
206	1550	J=(KJ-1)*3	WR	70
211	1560	CC(J+1)=AA	WR	71
213	1570	CC(J+2)=-AA*G/3.0	WR	72
217	1580	CC(J+3)=-CC(J+2)*G/3.0	WR	73
223	1590	WN(J+1)=HH	WR	74
225	1600	WN(J+2)=-HH*G/3.0	WR	75
231	1610	WN(J+3)=-WN(J+2)*G/3.0	WR	76
235	1620	GO TO 1750	WR	77
	C1644		WR	78
	C1646		WR	79
		EXP	WR	80
236	1650	J=(KQ-1)*3	WR	81
241	1660	CC(J+1)=AA	WR	82
243	1670	CC(J+2)=-AA/3.0	WR	83
246	1680	CC(J+3)=AA/9.0	WR	84
251	1690	WN(J+1)=HH	WR	85
253	1700	WN(J+2)=-HH /3.0	WR	86
256	1710	WN(J+3)=HH /9.0	WR	87

	C1746			WR	88
261	1750	GO TO (1400,1900),KQ		WR	89
	C1746			WR	90
	C1748		ATTRACTIVE PART	WR	91
267	1800	IF (AM) 5000,5000,1810		WR	92
271	1810	G=FM		WR	93
273	1812	GB=FN		WR	94
275	1820	AG=AM		WR	95
277	1830	NB=KA		WR	96
301	1840	KQ=2		WR	97
302	1850	GO TO 1300		WR	98
	C1894			WR	99
303	1900	IF (L(6))4000,5000,4000		WR	100
	C1990			WR	101
	C1992			WR	102
	C1994		MAIN INITIAL ENTRY	WR	103
	C1996			WR	104
	C1998		REPULSIVE PART	WR	105
305	2000	IF (AN) 2500,2500,2010		WR	106
307	2010	G=FM		WR	107
311	2020	NB=KN		WR	108
313	2030	KQ=1		WR	109
	C2044			WR	110
	C2046		CALC.	WR	111
314	2050	GO TO (2060,2150),KR		WR	112
	C2054			WR	113
	C2058		LJ	WR	114
322	2060	E=D(1)*(-G/3.0)		WR	115
327	2070	J=(KQ-1)*3		WR	116
332	2080	DO 2110 I=1,3		WR	117
334	2090	KE=J+I		WR	118
336	2100	C(KE)=CC(KE)*E		WR	119
341	2110	*C(KE)=WN(KE)*E		WR	120
344	2120	GO TO 2450		WR	121
	C2144			WR	122
	C2146		EXP	WR	123
345	2130	I=D(1)*0.33333333		WR	124
	C2176			WR	125
351	2180	S=G*T		WR	126
353	2190	E= EAP(G-S)		WR	127
362	2200	J=(KQ-1)*3		WR	128
365	2210	DO 2240 I=1,3		WR	129
367	2220	KE=I+J		WR	130
371	2230	C(KE)=CC(KE)*E		WR	131
374	2240	*C(KE)=WN(KE)*E		WR	132
377	2250	C(J+2)=C(J+2)*S		WR	133
402	2260	C(J+3)=C(J+3)*(S*S-S)		WR	134
	C2296			WR	135
406	2300	J=(KQ-1)*4		WR	136
412	2310	A(J+1)=S		WR	137
414	2320	S1=1.0/S		WR	138
416	2330	A(J+2)=S1		WR	139
420	2340	A(J+3)=1.0+S1		WR	140
423	2350	A(J+4)=- (S+2.0+2.0*S1)		WR	141
430	2360	A(J+5)=2.0*(1.0+S1)		WR	142
435	2370	A(J+6)=S*S+2.0*S+4.0+4.0*S1		WR	143
444	2380	A(J+7)=2.0+3.0*S		WR	144
450	2390	A(J+8)=- (3.0*S+4.0+4.0*S1)		WR	145
456	2400	A(J+9)=S-S*S		WR	146
	C2444			WR	147

461	2450	GO TU (2400,2600),KQ		WR	148
	C2494			WR	149
	C2494.			WR	150
	C2496		ATTRACTIVE PART	WR	151
467	2500	IF (AM) 2400,2600,2510		WR	152
471	2510	G=FM		WR	153
473	2520	KB=KA		WR	154
475	2530	KQ=2		WR	155
476	2540	GO TU 2050		WR	156
	C2594			WR	157
	C2596		WHOLE	WR	158
477	2600	U(2)=C(1)-C(4)		WR	159
502	2610	U(3)=C(2)-C(5)		WR	160
505	2620	U(4)=C(3)-C(6)		WR	161
510	2630	IF (L(6)) 4100,5000,4100		WR	162
	C2990			WR	163
	C2992			WR	164
	C2994		MAIN ENTRY FOR CELL POTENTIAL	WR	165
	C2996			WR	166
	C2998		REPULSIVE PART	WR	167
512	3000	A=N(1)		WR	168
513	3002	U(2)=X**2		WR	169
515	3004	IF (AN) 3600,3600,3010		WR	170
517	3010	KB=KR		WR	171
521	3020	KQ=1		WR	172
	C3030			WR	173
	C3040		CALC.	WR	174
522	3050	GO TU (3060,3300),KB		WR	175
	C3054			WR	176
	C3056		LJ	WR	177
530	3060	UNF=1.0		WR	178
532	3070	Y=N(2)		WR	179
534	3080	KK=(KCNF-KY-1)/512		WR	180
541	3090	N=2+KEP5(KQ)/KK		WR	181
546	3100	NN=MIN(N,NMAX(KQ))		WR	182
552	3110	GO TU (3150,3200),KQ		WR	183
	C3144			WR	184
560	3150	KE=M+1-NN		WR	185
563	3160	F(1)=A(KE)*Y		WR	186
566	3162	KE=KE+1		WR	187
570	3170	DO 3180 I=KE,M		WR	188
575	3180	F(1)=(F(1)+A(I))*Y		WR	189
602	3190	GO TU 3250		WR	190
	C3194			WR	191
603	3200	KE=M+1-NN		WR	192
606	3210	F(4)=AL(KE)*Y		WR	193
611	3220	KE=KE+1		WR	194
613	3230	DO 3240 I=KE,M		WR	195
620	3240	F(4)=(F(4)+AL(I))*Y		WR	196
	C3244			WR	197
625	3250	J=(KQ-1)*3		WR	198
630	3260	W(J+1)=C(J+1)*F(J+1)		WR	199
633	3270	W(J+2)=C(J+2)*F(J+1)		WR	200
636	3280	W(J+3)=C(J+3)*F(J+1)		WR	201
641	3290	GO TU 3450		WR	202
	C3294			WR	203
	C3296		EXP	WR	204
642	3300	J=(KQ-1)*M		WR	205
646	3310	E=A(J+1)*X		WR	206
651	3320	E1=EXP(E)/2.0		WR	207

657	3730	E2=0.25/F1		WR	208
661	3740	FC=(E1+F2)		WR	209
663	3750	F5=(E1-E2)		WR	210
665	3760	IF (E=0.1)3370,3370,3450		WR	211
670	3770	E1=F*E		WR	212
672	3780	E2=E1*E1		WR	213
674	3790	FSS=1.0*E1/6.0+E2/120.0		WR	214
701	3400	GO TO 3452		WR	215
	C3444			WR	216
702	3450	FSS=F5/F		WR	217
704	3452	F5=X*F5		WR	218
	C3454			WR	219
706	3460	I=(K0-1)*3		WR	220
711	3462	F(I+1)=A(J+3)*FSS-A(J+2)*FC-1.0		WR	221
720	3470	F(I+2)=A(J+4)*FSS-F5+A(J+5)*FC+A(J+1)		WR	222
730	3480	F(I+3)=A(J+6)*FSS+A(J+7)*F5		WR	223
		1		WR	224
743	3490	J=I		WR	225
	C3494			WR	226
745	3500	W(J+1)=WC(J+1)*F(J+1)		WR	227
750	3510	W(J+2)=WC(J+2)*F(J+2)		WR	228
753	3520	W(J+3)=WC(J+3)*F(J+3)		WR	229
	C3544			WR	230
756	3550	GO TO (3600,3650),K0		WR	231
	C3594			WR	232
	C3596		ATTRACTIVE PART	WR	233
764	3600	IF (AM) 3610,3650,3610		WR	234
765	3610	K8=KA		WR	235
767	3620	KQ=P		WR	236
770	3630	GO TO 3650		WR	237
	C3644			WR	238
	C3646			WR	239
773	3650	U(3)=W(1)-W(4)		WR	240
774	3660	U(4)=W(2)-W(5)		WR	241
777	3670	U(5)=W(3)-W(6)		WR	242
1002	3680	IF(L(6))4200,5000,4200		WR	243
	C3992			WR	244
	C3994		DIAGNOSTIC PRINT	WR	245
	C3996			WR	246
	C3998		PRELIM	WR	247
1004	4000	CALL PRIN(13HPREL,WR CC3,6,CC)		WR	248
1007		CALL PRIN(3HWN5,6,WN)		WR	249
1014	4010	IF (L(1)-2)4020,4050,4020		WR	250
1016	4020	CALL PRIN(2HNS,30,A)		WR	251
1021		CALL PRIN(3HALS,30,AL)		WR	252
1026	4030	GO TO 5000		WR	253
	C4048		MAIN INITIAL	WR	254
1027	4100	CALL PRIN(13HMAIN WR C 3,6,C)		WR	255
1032		CALL PRIN(3HNC3,6,WC)		WR	256
1037	4120	IF (L(1)-1)4130, 4140,4130		WR	257
1041	4130	CALL PRIN(2HNS,9,A)		WR	258
1044		CALL PRIN(4HAL 3,9,AL)		WR	259
1051	4140	GO TO 5000		WR	260
	C4194		MAIN INTEGRATE	WR	261
1052	4200	CALL PRIN(2HFS,6,F)		WR	262
1055		CALL PRIN(13HW (WR ROUT) 3,6,W)		WR	263
1062	4210	GO TO 5000		WR	264
	C4994			WR	265
1063	5000	RETURN		WR	266
	C			WR	267

```

SUBROUTINE PKW(K)                                *K*          2
C KISTIAKOWSKY-WILSON EQUATION OF STATE          *K*          3
C ----- *K*          4
C K=1: EOS, CALLED FROM GEM(2)                   *K*          5
C K=2: MUS, CALLED FROM XIM(2)                   *K*          6
C K=1                                             *K*          7
C INPUT                                           *K*          8
C 1,V=TAU,THETA=GM(1),(2), (FOR KW,VSTAR=1STAR=1) *K*          9
C XI=EMX - (GAS) MOLE FRACTIONS                 *K*         10
C KI=XPG - COVOLUMES, NOTE: THIS ARRAY IS COVOLUMES *K*         11
C KR=KIM(1) - NO. SPECIES                       *K*         12
C OUTPUT                                          *K*         13
C AE = X*EXP(THETA*X)=7-1,LOCAL, USED BY K=2 ENTRY. *K*         14
C                                                *K*         15
C                FOR KW, KSTARIJ FOR LJO.        *K*         16
C K=2                                             *K*         17
C INPUT (SEE DEFINITIONS ABOVE)                 *K*         18
C AE FROM K=1                                    *K*         19
C GM FROM K=1                                    *K*         20
C KI=XPG                                         *K*         21
C NCIES                                          *K*         22
C 1. UNLIKE LJO, FOR WHICH MIX PART IS DONE IN XIM-XIMS, *K*         23
C FOR KW EVERYTHING IS DONE HERE.              *K*         24
C ----- *K*         25
3 COMMON Z(4000)                                *K*         26
3 DIMENSION                                     *K*         27
1 EMX ( 20),GM ( 40),GP ( 20) *K*         28
2 KIM ( 10),XMU ( 20),XMT ( 30) *K*         29
3 XPG ( 20, 20) *K*         30
3 EQUIVALENCE *K*         31
1 (Z( 1170),EMX ) ,(Z( 1490),GM ) ,(Z( 1470),GP ) *K*         32
2 (Z( 1681),KIM ) ,(Z( 2240),XMU ) ,(Z( 2210),XMT ) *K*         33
3 (Z( 2660),XPG ) *K*         34
C *K*         35
C KISTIAKOWSKY-WILSON EQUATION OF STATE *K*         36
C *K*         37
C *K*         38
3 EQUIVALENCE (GP(1),ALP),(GP(2),BET),(GP(3),TH) *K*         39
3 EQUIVALENCE (GM(1),V),(GM(2),I),(GM(12),X) *K*         40
3 EQUIVALENCE (XMT(1d),MK) *K*         41
3 EQUIVALENCE (KIM(1),KR) *K*         42
C *K*         43
C *K*         44
C *K*         45
3 GO TO (100,500)*K *K*         46
C ----- K=1, EOS ----- *K*         47
11 100 MK=0 *K*         48
12 110 DO 120 I=1,KR *K*         49
21 120 MK=MK+EMX(I+1)*XPG(I) *K*         50
C *K*         51
25 150 X=MK/(V*(T+TH)*ALP) *K*         52
34 160 E=EXP(THETA*X) *K*         53
42 170 AE=X*E *K*         54
C *K*         55
44 200 GM(3)=XF+1.0 *K*         56
47 210 GM(4)=ALP*THETA*E/(I+TH) *K*         57
53 212 GM(6)=(E-1.0)/BET-ALOG(GM(3)) *K*         58

```

62	220	GM(9)=GM(3)-(1.0+BETOX)*GM(4)	HKA	59
67	230	GM(10)=- (1.0+BETOX)*XE	HKA	60
73	240	GM(11)=GM(4)*(2.0-(1.0*ALP*(1.0+BETOX))*T/(T+TM))	HKA	61
105	250	GM(5)=GM(4)+XE	HKA	62
107	260	GM(7)=GM(6)+XE	HKA	63
111	270	GM(8)=GM(5)-GM(7)	HKA	64
	C		HKA	65
113	400	GO TO 2000	HKA	66
	C	----- K=2, MUS -----	HKA	67
114	500	DO 510 I=1,KR	HKA	68
123	510	AMII(I)=GM(5)+(XPG(I)/HK-1.0)*XE	HKA	69
	C		HKA	70
	C	520 NOTE= GEM MOVES F/R! FROM GM(7) TO GM(5)	HKA	71
	C		HKA	72
131	2000	RETURN	HKA	73
132		END	HKA	74

SUBROUTINE SEM (K,L)

	C		SEM	2
	C		SEM	3
	C	SOLID EQ. OF STATE ADAPTOR	SEM	4
	C		SEM	5
	C	REVISION 1 - FOR NEW SEMS CODE	SEM	6
	C	W.F. 10/61	SEM	7
	C		SEM	8
	C		SEM	9
	C	SEM	SEM	10
	C		SEM	11
6		COMMON 7(4000)	SEM	12
6		DIMENSION	SEM	13
		1 KEN (6, 10),KUN (6, 10),CAR (10, 8)	SEM	14
		2 CONT (20),EV (20),FUR (6, 10)	SEM	15
		3 KAL (20),KEV (20),SP (20)	SEM	16
		4 SPC (20),SM (20),TMS (20)	SEM	17
		5 THER (50)	SEM	18
6		DIMENSION CE(10)	SEM	19
6		EQUIVALENCE	SEM	20
		1 (7(1620),KEN) ,(Z(1690),KUN) ,(Z(920),CAR)	SEM	21
		2 (7(460),CONT) ,(Z(680),EV) ,(Z(1410),FUR)	SEM	22
		3 (Z(1600),KAL) ,(Z(900),KEV) ,(Z(1840),SP)	SEM	23
		4 (Z(1860),SPC) ,(Z(1820),SM) ,(Z(1990),TMS)	SEM	24
		5 (Z(1920),THER)	SEM	25
	C		SEM	26
	C	LOCAL EQ	SEM	27
	C		SEM	28
6		EQUIVALENCE (CAR(51),CE),(CONT(2),K)	SEM	29
		1 ,(THER(1),P),(THER(3),T),(SM(1),VS)	SEM	30
6		GO TO (1000,10),K	SEM	31
	C 994		SEM	32
	C 996	PRELIMINARY	SEM	33
	C 998		SEM	34
13	1000	CALL REAP (SEM	35
		1 540X G, CPR, AL, VU, TU, EOR / CO, C1, C2, C3, C4 5	SEM	36
		2 ,12,SP)	SEM	37
20	1001	KAL(4)=1	SEM	38
21	1002	IF (SP(2))1004,1003,1004	SEM	39
22	1003	KAL(4)=0	SEM	40
	C		SEM	41
23	1004	CALL SEMS(1)	SEM	42
27	1006	SM(9)=0.8	SEM	43

31	C			SEMS	44
		1010	CALL DOUT (3HSEM,1)	SEMS	45
36		1020	GO TO 300	SEMS	46
	C	1098		SEMS	47
	C			SEMS	48
	C		SES MAIN	SEMS	49
37		10	KEN(2)=KEN(2)+1	SEMS	50
41		20	IF (KAL(→)) 40,100,40	SEMS	51
	C			SEMS	52
42		40	CALL SEMS(2)	SEMS	53
	C			SEMS	54
46		50	GO TO 200	SEMS	55
	C			SEMS	56
	C		CALC. INCOMPRESSIBLE SOLID OUTPUT	SEMS	57
47		100	SM(9)=1.0	SEMS	58
51		102	SM(10)=1.0	SEMS	59
53		104	SM(1)=SP(4)	SEMS	60
55		106	SM(2)=0.0	SEMS	61
56		108	SM(3)=P+VS/(R*T)	SEMS	62
62		110	SM(4)=0.0	SEMS	63
63		112	SM(5)=SM(3)	SEMS	64
65		114	SM(6)=0.0	SEMS	65
66		116	SM(7)=SM(3)	SEMS	66
70		118	SM(8)=P	SEMS	67
72		200	CALL DOUT (3HSEM,2)	SEMS	68
77		300	RETURN	SEMS	69
	C			SEMS	70
			ARGS K=1, PREL.	SEMS	71
			K=2, MAIN	SEMS	72
			L=1, ISOTHERM	SEMS	73
			L=2, ISENTROPIC	SEMS	74
	C			SEMS	75
	C		SPECS	SEMS	76
			INPUT	SEMS	77
			SP SEPS INPUT (SEE SEPS)	SEMS	78
			SPC SEPS OUTPUT (SEE SEPS)	SEMS	79
			T TEMP	SEMS	80
			VS -SOLID VOL	SEMS	81
			OUTPUT	SEMS	82
			SM SES IMPERFECTION THERMO FNS-SEE SEPS	SEMS	83
			HERE E,K,A,F,S FURT,P=1 ATM HAVE BEEN	SEMS	84
			SUBTRACTED 10 FORM IMPERFECTION FNS.	SEMS	85
	C			SEMS	86
100			END	SEMS	87
				SEMS	
			SUBROUTINE SEMS (K)	SEMS	2
	C			SEMS	3
			NEW SES SUBROUTINE	SEMS	4
			*WITH SINGLE ITERATION FOR V(P,T)	SEMS	5
			INPUT = P,T	SEMS	6
			OUTPUT = V AND SES IMP. THERMO FNS	SEMS	7
			K=1 FOR PREL	SEMS	8
			K=2 FOR MAIN	SEMS	9
				SEMS	10
			W. F. =10/61	SEMS	11
				SEMS	12
				SEMS	13
				SEMS	14
3			COMMON Z(4000)	SEMS	15

3	DIMENSION								SEMS	16					
	1 CAR	(10,	8),	EV	(20),	FUB	(6, 10)	SEMS	17			
	2 KON	(6,	10),	SM	(20),	SP	(20)	SEMS	18			
	3 THER	(50)							SEMS	19			
3	DIMENSION	C(5),	CN(5),	CG(5),	CG1(5),	CS(10),	KCS(2)				SEMS	20			
3	EQUIVALENCE										SEMS	21			
	1	(Z(920),	CAR),	(Z(880),	EV),	(Z(1410),	FUB)	SEMS	22
	2	(Z(1690),	KON),	(Z(1820),	SM),	(Z(1840),	SP)	SEMS	23
	3	(Z(1920),	THER)								SEMS	24	
												SEMS	25		
												SEMS	26		
												SEMS	27		
3												SEMS	28		
												SEMS	29		
												SEMS	30		
												SEMS	31		
												SEMS	32		
												SEMS	33		
												SEMS	34		
												SEMS	35		
3												SEMS	36		
												SEMS	37		
												SEMS	38		
												SEMS	39		
												SEMS	40		
												SEMS	41		
												SEMS	42		
												SEMS	43		
												SEMS	44		
												SEMS	45		
												SEMS	46		
												SEMS	47		
3	20	GO TO	(100,	1000),	K							SEMS	48		
												SEMS	49		
												SEMS	50		
11	100	K=	2.31479E-5									SEMS	51		
13	112	A=	(4*SP(2)/(ALPH*V0))	*	(G/(G+1.0))							SEMS	52		
22	110	G1=	1.0/(3+1.0)									SEMS	53		
25	120	G2=	0.5+1.0/G									SEMS	54		
												SEMS	55		
31	150	CN(1)=	G1									SEMS	56		
33	160	DO	140	I=	2,4							SEMS	57		
35	170	FI=	I									SEMS	58		
36	180	CN(I)=	CN(I-1)*(G1-(FI-1.0))/FI									SEMS	59		
												SEMS	60		
45	200	DO	230	I=	1,5							SEMS	61		
47	210	FI=	I-1									SEMS	62		
52	220	CG(I)=	C(I)/(G+FI)									SEMS	63		
56	230	CG1(I)=	C(I)/(G+FI+1.0)									SEMS	64		
												SEMS	65		
64	250	E1=	0.0									SEMS	66		
65	260	E2=	0.0									SEMS	67		
66	270	DO	290	I=	1,5							SEMS	68		
70	280	E1=	E1+CG(I)									SEMS	69		
73	290	E2=	E2+CG1(I)									SEMS	70		
76	300	CONST=	0.5*E1-G2*E2									SEMS	71		
												SEMS	72		
102		GO TO	2000									SEMS	73		
												SEMS	74		
												SEMS	75		

	C		SEMS	76
103	1000	CS(4)=Y	SEMS	77
105	1020	CS(2)=Y*FORI	SEMS	78
107	1030	YU=1.0+ALPH*(T-T0)	SEMS	79
113	1040	KCS(1)=0	SEMS	80
	C		SEMS	81
	C	ITERATE ON Y=V/V0	SEMS	82
114	1100	CALL FRONTT (CS,KONI)	SEMS	83
120	1110	KEXIT=KCS(2)	SEMS	84
122	1120	GO TO (1500+1150+1130+1140)*KEXIT	SEMS	85
132	1130	CALL DBUG (4HSEMS,1)	SEMS	86
136	1132	GO TO 1500	SEMS	87
137	1140	CALL DBUG (4HSEMS,1)	SEMS	88
143	1142	GO TO 1500	SEMS	89
	C	FUNCTION	SEMS	90
144	1150	IF (CS(2)-YU) 1180+1180+1160	SEMS	91
147	1160	CS(2)=YU	SEMS	92
151	1170	GO TO 1200	SEMS	93
152	1180	IF (YL-CS(2)) 1200+1200+1190	SEMS	94
155	1190	CS(2)=YL	SEMS	95
	C		SEMS	96
157	1200	Y=CS(2)	SEMS	97
	C	CALC. P2(Y)	SEMS	98
161	1210	PH=C(5)	SEMS	99
163	1220	E1=C6(5)	SEMS	100
165	1230	E2=C61(5)	SEMS	101
167	1250	DU 1290 I=1,4	SEMS	102
171	1260	KE=5-I	SEMS	103
173	1270	PH=PH*Y+C(KE)	SEMS	104
176	1280	E1=E1*Y+C6(KE)	SEMS	105
201	1290	E2=E2*Y+C61(KE)	SEMS	106
	C		SEMS	107
206	1300	WEEG=(0.5-G2*Y)*PH	SEMS	108
212	1310	YG=Y*G	SEMS	109
	C		SEMS	110
216	1320	P2=- (G/Y)*WEEG+G*(G/Y)*	SEMS	111
	1	(0.5*E1-G2*Y*E2-CONST/YG)	SEMS	112
	C		SEMS	113
	C	CALC Y1, Y11, SEPARATE ON Y	SEMS	114
231	1350	IF (Y-1.0) 1700+1800+1800	SEMS	115
	C		SEMS	116
	C		SEMS	117
	C		SEMS	118
235	1400	CS(3)=2.0E-6*(TC-T)	SEMS	119
	C		SEMS	120
243	1470	CALL DOUT (4HSEMS,1)	SEMS	121
244	1480	GO TO 1100	SEMS	122
	C		SEMS	123
	C	CALCULATE OUTPUT	SEMS	124
245	1500	SM(1)=Y*V0	SEMS	125
247	1510	SM(7)=P*SM(1)/(R*T)	SEMS	126
253	1520	SM(7)=(1.0+1.0/G)*SM(7)+V0*WEEG/(R*T)-SM(2)*(1.0-[0/T)	SEMS	127
265	1530	SM(6)=SM(2)*ALOG(T1/T)	SEMS	128
274	1540	SM(5)=SM(3)-SM(6)	SEMS	129
276	1550	SM(2)=SM(3)-SM(7)	SEMS	130
300	1560	SM(4)=SM(5)-SM(7)	SEMS	131
302	1572	GO TO 2000	SEMS	132
	C		SEMS	133
	C		SEMS	134
	C	CALC. FN. FOR Y LESS THAN 1	SEMS	135

C		SEMS	136
303	1700 X=(P-P2)*YG*Y/A	SEMS	137
310	1710 YG1=1.0*X	SEMS	138
313	1720 Y11=CN(4)*X	SEMS	139
315	1730 DO 1740 I=1,3	SEMS	140
317	1732 KE=4-I	SEMS	141
321	1740 Y11=(Y11+CN(KE))*X	SEMS	142
326	1742 Y1=Y11+1.0	SEMS	143
C		SEMS	144
	CALC. T	SEMS	145
331	1750 T1=Y11/ALPH+T0	SEMS	146
334	1760 TC=T1*(YB1/Y1)/YG	SEMS	147
340	1770 GO TO 1400	SEMS	148
C		SEMS	149
	CALC. P.N. FOR Y OVER I	SEMS	150
C		SEMS	151
341	1800 X=P/A	SEMS	152
343	1810 YG1=1.0*X	SEMS	153
346	1820 Y11=CN(4)*X	SEMS	154
350	1830 DO 1850 I=1,3	SEMS	155
352	1840 KE=4-I	SEMS	156
354	1850 Y11=(Y11+CN(KE))*X	SEMS	157
361	1860 Y11=Y-1.0+Y*Y11	SEMS	158
365	1862 Y1=Y11+1.0	SEMS	159
C		SEMS	160
	CALC. T	SEMS	161
370	1870 T1=Y11/ALPH+T0	SEMS	162
373	1880 TC=T1*YG1*Y/(Y11+1.0)	SEMS	163
400	1890 GO TO 1400	SEMS	164
C		SEMS	165
401	2000 RETURN	SEMS	166
402	END	SEMS	167

	SUBROUTINE TIM (K)	TIM	2
C		TIM	3
C	ITF ADAPTOR	TIM	4
C		TIM	5
C	REVISION 1. FIX TIM FOR TMS REVISION 1	TIM	6
C	W.F. DEC. 61	TIM	7
C		TIM	8
C	TIM	TIM	9
3	COMMON Z(4000)	TIM	10
3	DIMENSION	TIM	11
	1 CONT (20) ,EA (200) ,EMX (20)	TIM	12
	2 ME (10) ,KEN (60) ,KIM (10)	TIM	13
	3 THER (50) ,TMS (20) ,TMG (20)	TIM	14
	4 TP (24,10)	TIM	15
3	DIMENSION KE(2),TH(5)	TIM	16
3	EQUIVALENCE	TIM	17
	1 (Z(460),CONT) ,(Z(480),EA) ,(Z(1170),EMX)	TIM	18
	2 (Z(1590),ME) ,(Z(1620),KEN) ,(Z(1680),KIM)	TIM	19
	3 (Z(1920),THER) ,(Z(1990),TMS) ,(Z(1970),TMG)	TIM	20
	4 (Z(2010),TP)	TIM	21
C	LOCAL E.N.DIM	TIM	22
3	EQUIVALENCE (KIM(2),KS),(KIM(4),KN),(CONT(3),ATM)	TIM	23
	1 ,(THER(1),P),(THER(3),T)	TIM	24
C		TIM	25
C	98	TIM	26
3	100 GO TO (1000,2000),K	TIM	27
C	996	TIM	28
C	998	TIM	29
	PRELIMINARY	TIM	30

11	1000 CALL HEAD (TIM	31
	1 6000X KS,KN/ T BOUNDS/ FIT COEFFS.-A1 TO AN,D,DEL,PF,MR...S		TIM	32
	2.,-2*KE)		TIM	33
14	CALL HEAD(0,2,TH(4))		TIM	34
20	1010 KS=KE(1)		TIM	35
22	1020 KN=KE(2)		TIM	36
24	1030 KE1=KN*F		TIM	37
26	1040 DO 1070 I=1,KS		TIM	38
30	1050 CALL HEAD(0,KE1,EA)		TIM	39
34	1060 DO 1070 J=1,KE1		TIM	40
44	1070 IP(I,J)=EA(J)		TIM	41
52	GO TO 3000		TIM	42
	C1096		TIM	43
	C1098	MAIN	TIM	44
52	2000 KEN(3)=KEN(3)+1		TIM	45
54	2010 TH(1)=T		TIM	46
56	2060 KE(1)=KS		TIM	47
60	2070 KE(2)=KN		TIM	48
62	2080 TH(2)=P/ATM		TIM	49
64	2090 TH(3)=HE(3)		TIM	50
	C2100		TIM	51
66	2110 CALL TIMS (KE,TH,TP,EMX,IMS,IMG)		TIM	52
74	2120 CALL DOUT (3HTIM,1)		TIM	53
	C2900		TIM	54
100	3000 RETURN		TIM	55
	C		TIM	56
	C		TIM	57
101	END		TIM	58
	SUBROUTINE TIMS (K,TH,A,X,G,F)		TIMS	2
C			TIMS	3
C		IDEAL GAS THERMO FNS SUBROUTINE	TIMS	4
C		REVISION 1.-CONST. CP EXTENSIONS	TIMS	5
C		W. F. DEC. 61	TIMS	6
C			TIMS	7
C		K(1)=KS, NO. OF SPECIES	TIMS	8
C		K(2)=KN, DEGREE OF FIT	TIMS	9
C		TH(1)=T IN DEGREES K.	TIMS	10
C		TH(2)=P/ATM.	TIMS	11
C		TH(3)=T SUB ZERO	TIMS	12
C		TH(4)=TMIN	TIMS	13
C		TH(5)=TMAX	TIMS	14
C		A - COEFFICIENT MATRIX (SEE WRITE-UP)	TIMS	15
C		X - MOLE FRACTIONS (X(1) FOR SOLID)	TIMS	16
C			TIMS	17
C		IDEAL GAS THERMODYNAMIC FUNCTIONS	TIMS	18
C		INPUT	TIMS	19
C		OUTPUT	TIMS	20
C		G - TOTAL THERMO FUNCTIONS FOR GAS,SOLID	TIMS	21
C		F - FREE ENERGIES AT 1,P	TIMS	22
C		RELATIVE TO ELEMENTS AT 0 KELVIN	TIMS	23
C			TIMS	24
16	COMMON 7(4000)		TIMS	25
16	DIMENSION K(2),TH(5),A (20,10),X(20),G(20),F(20)		TIMS	26
	1,EA(40),C(20),H(20),S(20),GI(20)		TIMS	27
16	EQUIVALENCE		TIMS	28
	1 (Z(480),EA)		TIMS	29
	1 , (EA(1),C), (EA(2),H), (EA(4),S)		TIMS	30
	2, (EA(6),GI)		TIMS	31

	C			TIMS	32
	C			TIMS	33
	C	2 E		TIMS	34
16		3	$\mu=1.98719E-3$	TIMS	35
20		4	$KS=K(1)$	TIMS	36
21		5	$N=K(4)$	TIMS	37
23		6	$T=TH(1)$	TIMS	38
25		7	$PLUG=ALOG(TH(2))$	TIMS	39
34		8	$T0=TH(3)$	TIMS	40
34			$TMIN=TH(4)$	TIMS	41
34			$TMAX=TH(4)$	TIMS	42
	C	9 I(E)		TIMS	43
41		10	DO 20 I=1,80	TIMS	44
46		20	EA(I)=0.0	TIMS	45
	C		BOUND T1 TO FIT RANGE	TIMS	46
53		30	IF(T-TMAX) 60,60,40	TIMS	47
56		40	I1=TMAX	TIMS	48
60		50	GO TO 110	TIMS	49
61		60	IF(T-TMIN) 70,70,90	TIMS	50
64		70	I1=TMIN	TIMS	51
66		80	GO TO 110	TIMS	52
67		90	I1=T	TIMS	53
	C	100 I	ALL SPECIES	TIMS	54
71		110	DO 200 I=1,KS	TIMS	55
	C	112 I(E)	J=N+1 FOR SERIES	TIMS	56
73		120	J=N	TIMS	57
75		130	FJ=J	TIMS	58
77		140	AIJ=A(I,J+1)	TIMS	59
103		150	$H(I)=(H(I)+A(I,J)*I)$	TIMS	60
107		160	$C(I)=(C(I)+(FJ+1.0)*AIJ)*T1$	TIMS	61
115		170	$S(I)=(S(I)+((FJ+1.0)/FJ)*AIJ)*T1$	TIMS	62
124		180	J=J-1	TIMS	63
126		190	IF (J) 130,210,130	TIMS	64
	C	200 E	ADD FIRST TERMS	TIMS	65
127		210	AIJ=A(I,1)	TIMS	66
132		220	$H(I)=H(I)+AIJ$	TIMS	67
135		230	$C(I)=C(I)+AIJ$	TIMS	68
140		240	$S(I)=S(I)+AIJ*ALOG(T1)+A(I,N+2)*PLUG$	TIMS	69
	C			TIMS	70
	C		ADD CONST CP FUNCTIONS OUTSIDE	TIMS	71
155		250	IF (T-T1) 260,290,260	TIMS	72
157		260	$H(I)=(T1*H(I)+C(I)*(T-T1))/T$	TIMS	73
165		270	$S(I)=S(I)+C(I)*ALOG(T/T1)$	TIMS	74
	C			TIMS	75
200		290	$F(I)=H(I)-S(I)+A(I,N+3)/(R*T)$	TIMS	76
	C	300 I(E)	MIXTURE SUMS	TIMS	77
213		310	DO 360 I=2,N5	TIMS	78
215		312	$XI=X(I)$	TIMS	79
217		320	$GI(2)=GI(2)+XI*(H(I)+A(I,N+3)/(R*T))$	TIMS	80
230		330	$GI(3)=GI(3)+XI*C(I)$	TIMS	81
230			$F*XI=0.0$	TIMS	82
234			IF(XI.GT.0.0) F*XI=XI*ALOG(XI)	TIMS	83
244		340	$GI(4)=GI(4)+XI*S(I)-F*XI$	TIMS	84
251		350	$GI(5)=GI(5)+XI*A(I,N+4)$	TIMS	85
257		360	$GI(6)=GI(6)+XI*(H(I)-(T0/T)*A(I,N+5)+A(I,N+4)/(R*T))$	TIMS	86
	C	370 E		TIMS	87
301		380	$GI(1)=GI(2)-1.0$	TIMS	88
	C	400 E	PURE PHASE	TIMS	89
304		410	$GI(7)=H(I)+A(I,N+3)/(R*T)$	TIMS	90
312		420	$GI(8)=C(I)$	TIMS	91

314	430	GI(9)=S(1)+PLOG	TIMS	92
316	440	GI(10)=F(1)-PLOG	TIMS	93
320	450	GI(11)=A(1,N+4)	TIMS	94
323	460	GI(12)=H(1)-(T0/T)*A(1,N+5)+GI(11)/(R*T)	TIMS	95
334	470	F(1)=GI(0)	TIMS	96
	C 500	I(E) STONE GI	TIMS	97
336	610	DO 520 I=1,12	TIMS	98
343	620	G(I)=GI(I)	TIMS	99
350	600	RETURN	TIMS	100
351		END	TIMS	101

		SUBROUTINE XIM (K,L)	XIM	2
C		GAS (MIXTURE) EQUATION OF STATE AT T, P, XI	XIM	3
C		K=1 PEAC INPUT DATA (PKEL.)	XIM	4
C		K=2 MAIN CALCULATION	XIM	5
C		L SPECIFIES PORTION OF EQ CODE FROM	XIM	6
C		WHICH XIM IS CALLED (SEE *WRITEUP)	XIM	7
C		INPUT	XIM	8
C		T,P=THEM(3),(1)	XIM	9
C		XI = (GAS) MOLE FRACTIONS	XIM	10
C		OUTPUT	XIM	11
C		XMT = MIXTURE STATE	XIM	12
C		XMU = MU#S	XIM	13
C		ROUTINES	XIM	14
C		XIMS = DETAILED CALCULATIONS FOR LH, CS, 1-FLUID.	XIM	15
C		CALLS GEP(2) IN MIDDLE FOR REF. STATE FOR MU#S	XIM	16
C		GEP(1/2) = PURE STATE POINT (REGULAR/LH EXPANSION)	XIM	17
C		-----	XIM	18
C		REVISION 1 - ADD KW EQ N. OF STATE	XIM	19
C		M.F. 9/61	XIM	20
C			XIM	21
C			XIM	22
C			XIM	23
C		XIM	XIM	24
			XIM	25
5		COMMON 7(4000)	XIM	26
6		DIMENSION	XIM	27
		1 CONT (20),EA (200),EMX (20)	XIM	28
		2 GP (20),GM (40),GMT (3, 20)	XIM	29
		3 KAL (20),KIM (10),THEM (50)	XIM	30
		4 XIT (30),XMU (20),XPF (20)	XIM	31
		5 XPG (20, 20),XPK (20),XPT (20)	XIM	32
		6 KEN(6,10)	XIM	33
6		DIMENSION KE(2),E1(6)	XIM	34
		1 SXG(20),SXF(20)	XIM	35
6		EQUIVALENCE	XIM	36
		1 (7(460),CONT) ,(Z(480),EA) ,(Z(1170),EMX)	XIM	37
		2 (Z(1470),GP) ,(Z(149),GM) ,(Z(1530),GMT)	XIM	38
		3 (Z(1670),KAL) ,(Z(1680),KIM) ,(Z(1920),THEM)	XIM	39
		4 (Z(2210),XMT) ,(Z(2240),XMU) ,(Z(2260),XPF)	XIM	40
		5 (Z(2660),XPG) ,(Z(3060),XPK) ,(Z(3080),XPT)	XIM	41
		6 (Z(1620),KEN)	XIM	42
C			XIM	43
C		LOCAL EQ, DIM	XIM	44
C			XIM	45
6		EQUIVALENCE	XIM	46
		1 (CONT(7),R) ,(GP(5),RSTA) ,(GP(6),TSTA) ,(GP(7),VSTA)	XIM	47
		2 (KIM(1),KR) ,(THEM(1),P) ,(THEM(3),T)	XIM	48
		3 (XMT(16),RSTAT) ,(XMT(17),TSTAT) ,(XMT(18),VSTAT)	XIM	49

	4*(EA(21),SXG),(EA(41),SXF)	XIP	50
C		XIP	51
6	80 GO TO (100,800),K	XIP	52
C	-----PRELIM-----	XIP	53
14	100 CALL READ (XIP	54
	154HDX KR,KAL/ SCH,SCT,R*REF,T*REF,N,M/ (R*)/ (T*) S	XIP	55
	1 *-2*KE)	XIP	56
17	CALL READ(0,6,E1)	XIP	57
22	CALL READ(0,KE,XPR)	XIP	58
25	CALL READ(0,KE,XPT)	XIP	59
32	110 KR=KE(1)	XIP	60
34	120 KAL(5)=KE(2)	XIP	61
36	130 DO 150 I=1,KR	XIP	62
40	140 XPR(I)=XPR(I)*E1(1)	XIP	63
43	150 XPT(I)=XPT(I)*E1(2)	XIP	64
C	160	XIP	65
46	170 DO 200 I=1,KR	XIP	66
50	180 DO 200 J=1,KR	XIP	67
52	140 XPR(I,J)=(XPR(I)+XPR(J))/2.0	XIP	68
60	200 XPR(I,J)=SQRT(XPR(I)*XPR(J))	XIP	69
C	208	XIP	70
75	210 XMT(11)=E1(3)	XIP	71
77	220 XMT(12)=E1(4)	XIP	72
101	230 XMT(13)=E1(5)	XIP	73
103	240 XMT(14)=E1(6)	XIP	74
105	250 IF (KAL(4)-9) 300,260,300	XIP	75
107	260 DO 270 I=1,KR	XIP	76
115	270 XPR(I)=E1(3)*CONT(5)*XPR(I)*J	XIP	77
121	300 GO TO 6000	XIP	78
C	-----MAIN-----	XIP	79
122	800 KE=KAL(5)+1	XIP	80
124	802 KEV(4)=KEV(4)+1	XIP	81
C	CHECK FOR KIASIOWSKY-WILSON	XIP	82
126	804 IF (KAL(5)-9) 810,806,810	XIP	83
130	806 CALL GEP(1)	XIP	84
134	808 CALL HKW(2)	XIP	85
C		XIP	86
140	809 GO TO 1100	XIP	87
C		XIP	88
141	810 GO TO (1000,2000,3000,4000,4000),KE	XIP	89
C	-----	XIP	90
C	840 NU MIX (ZERO)	XIP	91
C	848	XIP	92
152	1000 GO TO (1020,6000,1100),L	XIP	93
C	1010 NU MIX-ONE	XIP	94
161	1020 CALL GEP(1)	XIP	95
165	1030 DO 1040 I=1,KR	XIP	96
172	1040 XMT(I)=GM(5)	XIP	97
174	1050 GO TO 6000	XIP	98
C	1098 NU MIX-THREE	XIP	99
C	MIXTURE=REF. FLUID	XIP	100
175	1100 XMT(1)=GM(15)	XIP	101
177	1110 XMT(2)=GM(4)	XIP	102
201	1120 XMT(3)=GM(17)	XIP	103
203	1130 XMT(4)=GM(20)	XIP	104
205	1140 XMT(5)=GM(5)	XIP	105
207	1150 XMT(6)=GM(11)	XIP	106
211	1160 XMT(7)=GM(10)	XIP	107
213	1170 XMT(8)=GM(9)	XIP	108
215	1180 GO TO 6000	XIP	109

	C-----		XIM	110
	C1990	IDEAL MIXING (ONE)	XIM	111
	C1998		XIM	112
216	2000	GO TO (2070,6000,2200),L	XIM	113
	C2010		XIM	114
	C2020	IDEAL -ONE	XIM	115
225	2030	DO 2110 I=1,KR	XIM	116
227	2040	ISTA=XPT(I)	XIM	117
231	2050	RSTA=XPR(I)	XIM	118
233	2060	VSTA=CONT(5)*RSTA**3	XIM	119
236	2070	CALL GEP(1)	XIM	120
242	2080	GMT(1,I)=GM(15)	XIM	121
245	2090	GMT(2,I)=GM(17)	XIM	122
250	2100	GMT(3,I)=GM(5)	XIM	123
253	2110	AMT(I)=GM(5)	XIM	124
257	2120	GO TO 6000	XIM	125
	C	IDEAL -THREE	XIM	126
260	2200	XMT(1)=0.0	XIM	127
261	2210	AMT(3)=0.0	XIM	128
262	2220	AMT(5)=0.0	XIM	129
263	2230	DO 2290 I=1,KR	XIM	130
265	2240	AMT(1)=EMX(I+1)*GM(1,I)+XMT(1)	XIM	131
271	2250	AMT(3)=EMX(I+1)*GM(2,I)+XMT(3)	XIM	132
275	2260	AMT(5)=EMX(I+1)*GM(3,I)+XMT(5)	XIM	133
	C2270		XIM	134
303	2280	AMT(7)=XMT(1)/(R*T) -1.0	XIM	135
310	2290	XMT(2)=XMT(3)-XMT(7)	XIM	136
312	2300	AMT(4)=XMT(5)-XMT(7)	XIM	137
314	2310	AMT(6)=XMT(3)-XMT(5)	XIM	138
316	2320	AMT(8)=XMT(1)-R*T/P	XIM	139
322	2330	GO TO 6000	XIM	140
	C-----		XIM	141
	C3040	LH (TWO)	XIM	142
	C3048		XIM	143
323	3000	GO TO (3010,3100,3400),L	XIM	144
	C3004		XIM	145
	C3006	LH-ONE	XIM	146
332	3010	RSTA=XMT(11)	XIM	147
334	3020	ISTA=XMT(12)	XIM	148
336	3030	VSTA=CONT(5)*RSTA**3	XIM	149
341	3040	CALL GEP(1)	XIM	150
	C		XIM	151
	C	LH-TWO	XIM	152
345	3100	CALL XIMS (1)	XIM	153
351	3120	GO TO 6000	XIM	154
	C3148	LH-THREE	XIM	155
352	3400	CALL GEP(2)	XIM	156
354		GO TO 6000	XIM	157
	C-----		XIM	158
	C	CS (THREE) AND ONE FLUID (FOUR)	XIM	159
356	4000	GO TO (4010,4100,6000),L	XIM	160
	C4004		XIM	161
	C4006	CS, 1-FLUID - ONE	XIM	162
365	4010	CALL XIMS (0)	XIM	163
371	4020	ISTA=ISTAT	XIM	164
373	4030	RSTA=RSTAT	XIM	165
375	4040	VSTA=VSTAT	XIM	166
377	4050	CALL GEP(1)	XIM	167
	C	CS, 1-FLUID - TWO	XIM	168
403	4100	CALL XIMS (1)	XIM	169

405	GO TO 6000	XIM	170
	C	XIM	171
407	6000 CALL DOUT(3HXIM,1)	XIM	172
414	6010 RETURN	XIM	173
	C	XIM	174
415	END	XIM	175
	SUBROUTINE XIMS (K)	XIMS	2
	C THIS ROUTINE HAD HAD PUNCHES IN COL 73; REMOVED FOR PHOTOSTORE	XIMS	3
	C	XIMS	4
	C PERFORM DETAILED CALCULATIONS FOR XIM	XIMS	5
	C	XIMS	6
	C	XIMS	7
	C XIMS	XIMS	8
	C	XIMS	9
3	COMMON 7(4000)	XIMS	10
3	DIMENSION	XIMS	11
	1 XPF (20,20), XPG (20,20), CUNT (20)	XIMS	12
	2,EA (200), EMAX (20), GM (40)	XIMS	13
	3,GP (20), KAL (20), KIM (10)	XIMS	14
	4,XMU (20), XMT (30), EV (20)	XIMS	15
3	DIMENSION BILK(15)	XIMS	16
3	DIMENSION SXG(20),SXF(20),SMN(20),STN(20)	XIMS	17
3	EQUIVALENCE	XIMS	18
	1 (7(2260),XPF) ,(Z(2060),XPG) ,(Z(460),CUNT)	XIMS	19
	2,(7(430),EA) ,(Z(1170),EMAX) ,(Z(1490),GM)	XIMS	20
	3,(Z(147),GP) ,(Z(1000),KAL) ,(Z(1680),KIM)	XIMS	21
	4,(Z(2240),XMU) ,(Z(2410),XMT) ,(Z(680),EV)	XIMS	22
	C	XIMS	23
3	EQUIVALENCE (KIM(1),KR),(KIM(2),KS),(KIM(3),KC),(KIM(4),KN)	XIMS	24
3	EQUIVALENCE (XMT(10),RSTAT),(XMT(17),TSTAT),(XMT(18),VSTAT)	XIMS	25
	1 (GP(5),RSTA),(GP(6),TSTA),(GP(7),VSTA)	XIMS	26
	C	XIMS	27
	C 704 TO 7090 (N,MFOR ONE FLUID)	XIMS	28
3	EQUIVALENCE (XMT(1),BILK(4))	XIMS	29
	C	XIMS	30
3	EQUIVALENCE	XIMS	31
	1(EA(21),SXG),(EA(41),SXF),(EA(61),SMN),(EA(81),STN)	XIMS	32
	C	XIMS	33
	C 90 CALCULATE BAR= T0*RP / MOD II.4	XIMS	34
3	100 DO 130 I=1,KR	XIMS	35
5	120 SXF(I)=0.0	XIMS	36
7	130 SXG(I)=0.0	XIMS	37
12	140 TSTAT=0.0	XIMS	38
13	150 RSTAT=0.0	XIMS	39
	C 190 L-BRANCH= CS OR 1-FLUID	XIMS	40
14	200 NQ=KAL(5)	XIMS	41
16	210 GO TO (1500,300,300,400),NQ	XIMS	42
	C 290 CS(OR LH)	XIMS	43
26	300 DO 350 I=1,KR	XIMS	44
30	310 DO 330 J=1,KR	XIMS	45
32	320 SXF(I)=EMX(J+1)*XPF(I,J)+SXF(I)	XIMS	46
37	330 SXG(I)=EMX(J+1)*XPG(I,J)+SXG(I)	XIMS	47
45	340 TSTAT=EMX(I+1)*SXF(I)+TSTAT	XIMS	48
50	350 RSTAT=EMX(I+1)*SXG(I)+RSTAT	XIMS	49
55	360 GO TO 700	XIMS	50
	C 390 ONE-FLUID	XIMS	51
56	400 EV(11)=0.0	XIMS	52
57	410 EV(12)=0.0	XIMS	53

```

50 400 DO 550 I=1,KR
62 410 DO 530 J=1,KR
64 420 SXF(I)=FMX(J+1)*XPF(I,J)*XPG(I,J)**HILK(14) +SXF(I)
77 430 SXG(I)=FMX(J+1)*XPF(I,J)*XPG(I,J)**HILK(15) +SXG(I)
113 440 EV(11)=FMX(I+1)*SAF(I)+EV(11)
116 450 EV(12)=FMX(I+1)*SXG(I)+EV(12)
123 460 E3=1.0/(HILK(14)-HILK(15))
126 470 E4=HILK(14)*E3
130 480 E5=HILK(15)*E3
132 490 TSTAT=EV(12)**E4/EV(11)**E5
142 500 RSTAT=(EV(11)/EV(12))**E5
C
147 700 VSTAT=CONT(5)*RSTAT**3
C 800
C 810
152 1000 IF (K)1010,1500,1010
C
153 1010 CALL GEP(2)
C1090
C
156 1100 GO TO (1500,1150,1400,1300),KW
166 1150 DO 1160 I=1,KR
175 1160 AMU(I)=GM(5)
1
+GM(4)*(2.0*(SXF(I)/XMT(12))-1.0)-(TSTAT/TSTA-1.0)
2
+3.0*GM(10)*(2.0*(SXG(I)/XMT(11))-1.0)-(RSTAT/RSTA-1.0)
216 1170 GO TO 1500
C1190
217 1200 DO 1220 I=1,KR
221 1210 STN(I)=2.0*(SXF(I)/TSTAT-1.0)
224 1220 SRN(I)=2.0*(SXG(I)/RSTAT-1.0)
234 1230 GO TO 1400
C1290
235 1300 DO 1320 I=1,KR
237 1310 STN(I)=-2.0*E3*(HILK(15)*SAF(I)/EV(11)
1
-HILK(14)*SXG(I)/EV(12))
251 1320 SRN(I)=2.0*E3*(SXF(I)/EV(11)-SXG(I)/EV(12))
C1390
261 1400 DO 1410 I=1,KR
270 1410 AMU(I)=XMT(5)+3.0*AMT(7)*SRN(I)+XMT(2)*STN(I)
277 1500 RETURN
300 END

```

```

XIPS 54
XIPS 55
XIPS 56
XIPS 57
XIPS 58
XIPS 59
XIPS 60
XIPS 61
XIPS 62
XIPS 63
XIPS 64
XIPS 65
XIPS 66
XIPS 67
XIPS 68
XIPS 69
XIPS 70
XIPS 71
XIPS 72
XIPS 73
XIPS 74
XIPS 75
XIPS 76
XIPS 77
XIPS 78
XIPS 79
XIPS 80
XIPS 81
XIPS 82
XIPS 83
XIPS 84
XIPS 85
XIPS 86
XIPS 87
XIPS 88
XIPS 89
XIPS 90
XIPS 91
XIPS 92
XIPS 93
XIPS 94

```

```

SUBROUTINE EWP
C
C          EW PRELIMINARY
C          NSVISION 1 ERROR IN STATEMENT S20
C          LOOP GOES 1C KS, NOT 10
C          *F. 3/60
C
C          EGP
C
1  COMMON Z(4000)
1  DIMENSION
1  EPAL ( 20, 6),EPA ( 20),EPA1 ( 20)
2  EPC ( 10),EPW ( 10),FLAB ( 12, 8)
3  KAL ( 20),KIM ( 10),KUN ( 6, 10)
1  DIMENSION KEPA(20),KEPA1(20),KEPAL(20,6),KEPC(10)
1  DIMENSION KE1(12),L(12)
1  EQUIVALENCE
1  (Z(1210),EPAL ),(Z(1190),EPA ),(Z(1330),EPA1 )

```

```

EGP 2
EGP 3
EGP 4
EGP 5
EGP 6
EGP 7
EGP 8
EGP 9
EGP 10
EGP 11
EGP 12
EGP 13
EGP 14
EGP 15
EGP 16
EGP 17
EGP 18

```

	2*(Z(1350),EPC) ,(Z(1360),EPC) ,(Z(3100),FLAH)	EQU	19
	3*(Z(1600),KAL) ,(Z(1680),KIM) ,(Z(1690),KON)	EQU	20
C		EQU	21
1	EQUIVALENCE (KIM(2),KS), (KIM(3),KC)	EQU	22
	2 , (EPA,KEPA), (EPAL,KEPAL), (EPAL,KEPAL)	EQU	23
	3 , (EPC,KEPC)	EQU	24
C		EQU	25
1	EQUIVALENCE (FLAH(49),L)	EQU	26
C		EQU	27
C		EQU	28
1	80 KAL(6)=1	EQU	29
2	100 CALL READ (EQU	30
	1 30H0X C,S,P,PP,PHI / CAP Q S	EQU	31
	2 ,=6,KEPC)	EQU	32
5	CALL READ(0,KEPC,EPC)	EQU	33
10	110 KC=KEPC(1)	EQU	34
12	120 KS=KEPC(2)	EQU	35
14	130 READ(10,140) (KEL(I),I=1,12)	EQU	36
	140 FORMAT (12A6)	EQU	37
22	150 DO 160 I=1,KS	EQU	38
24	160 READ(10,170) L(I),(KEPAL(I,J),J=1,KC)	EQU	39
	170 FORMAT (A6,11I6)	EQU	40
46	180 READ(10,200) (KEPA(I),I=1,KS)	EQU	41
55	190 READ(10,200) (KEPA1(I),I=1,KS)	EQU	42
	200 FORMAT (12I6)	EQU	43
C		EQU	44
64	200 WRITE(9,310) (KEL(I),I=1,KS)	EQU	45
	210 FORMAT (6I0 ,12A6/)	EQU	46
73	220 DO 330 I=1,KS	EQU	47
75	230 WRITE(9,340) L(I),(KEPAL(I,J),J=1,KC)	EQU	48
	1 ,KEPA(I),KEPA1(I)	EQU	49
	240 FORMAT (6H ,A6,11I6)	EQU	50
C		EQU	51
124	500 DO 510 I=1,10	EQU	52
131	510 EPC(I)=KEPC(I)	EQU	53
133	520 DO 530 I=1,KS	EQU	54
135	530 EPA(I)=KEPA(I)	EQU	55
140	540 EPAL(I)=KEPAL(I)	EQU	56
144	550 DO 570 I=1,KS	EQU	57
146	560 DO 570 J=1,KC	EQU	58
156	570 EPAL(I,J)=KEPAL(I,J)	EQU	59
163	580 KAL(6)=1	EQU	60
C		EQU	61
164	600 CALL EQPS(KON(1,8),EPC,EPC,EPAL,EPAL(1,2),EPA,EPAL)	EQU	62
C		EQU	63
174	1000 RETURN	EQU	64
C		EQU	65
175	END	EQU	66
	SUBROUTINE EQM	EQU	2
C	EQUILIBRIUM COMPOSITION AND STATE AT T,P	EQU	3
C	INPUT	EQU	4
C	P,T=TEMP(1),(3), IMPLICIT FOR GEP VIA XIM=XIMS	EQU	5
C	SM = STATE OF SOLID	EQU	6
C	IMG = IDEAL STATE	EQU	7
C	OUTPUT	EQU	8
C	XI=EMX = (GAS) MOLE FRACTIONS	EQU	9
C	XMT = GAS (MIXTURE) STATE	EQU	10
C	VARIABLES	EQU	11


```

C      F-TILDE=EMG - FREE ENERGIES FROM EQMS          FQM      12
C      EMN - PHASE MOLE NUMBERS FROM EQMS            FQM      13
C      KSTAT=XMT(16),(17) - KSTAR-BAN                FQM      14
C      KSTA+TSTA=GP - KSTAR FOR GP                     FQM      15
C      ROUTINES                                         FQM      16
C      XIM - MIXTURE EOS VIA GEP, INCLUDING MU*5       FQM      17
C      EQMS - COMPOSITION AT FIXED F-TILDE            FQM      18
1      COMMON 7(4000)                                   FQM      19
1      DIMENSION                                       FQM      20
1      1 EMG (          20),EMN (          20),EMX (          20) FQM      21
1      2 FOH (          6, 10),GP (          20),GM (          40) FQM      22
1      3 KAL (          20),KEN (          6, 10),KEV (          20) FQM      23
1      4 KIM (          10),KOM (          0, 10),SM (          20) FQM      24
1      5 TMG (          20),XMU (          20),XMT (          30) FQM      25
1      7 EA(200),FV(20)                                FQM      26
1      EQUIVALENCE                                     FQM      27
1      1 (7( 1010),FOH ) ,(Z( 1030),EMN ) ,(Z( 1170),EMX )      FQM      28
1      2 (7( 1410),FOH ) ,(Z( 1470),GP ) ,(Z( 1490),GM )      FQM      29
1      3 (7( 1000),KAL ) ,(Z( 1020),KEN ) ,(Z( 900),KEV )      FQM      30
1      4 (7( 1600),KIM ) ,(Z( 1690),KOM ) ,(Z( 1820),SM )      FQM      31
1      5 (7( 1970),TMG ) ,(Z( 2240),XMU ) ,(Z( 2210),XMT )      FQM      32
1      7 (7(480),EA),(Z(480),EV)                          FQM      33
C      EQUIVALENCE (FOH(15),EPS),(KIM(2),KS)              FQM      34
1      EQUIVALENCE (GP(5),KSTA),(XMT(16),KSTAT)          FQM      35
1      EQUIVALENCE (GM (15) , VM)                          FQM      36
C      100 KEN(5)=KEN(5)+1                                FQM      37
C      100 KEN(5)=KEN(5)+1                                FQM      38
C      100 KEN(5)=KEN(5)+1                                FQM      39
3      200 CALL XIM(2,1)                                  FQM      40
6      210 EMG(1)=TMG(1)+SM(5)                           FQM      41
C      200 CALL DOUT (3HEQM,1)                            FQM      42
C      200 CALL DOUT (3HEQM,1)                            FQM      43
10     200 CALL DOUT (3HEQM,1)                            FQM      44
C      500 DO 520 I=1,KS                                  FQM      45
13     510 EMG(I+1)=TMG(I+1)+XMU(I)                       FQM      46
15     520 EA(I)=EMX(I)                                    FQM      47
C      600 IF (KAL(6)) 800,2000,800                       FQM      48
24     600 IF (KAL(6)) 800,2000,800                       FQM      49
C      800 F EV(1)=KAL(6)                                  FQM      50
25     810 NEV(1)=KOM(2,7)                                 FQM      51
27     820 NEV(2)=KOM(3,7)                                 FQM      52
31     830 NEV(3)=0                                        FQM      53
33     840 NEV(4)=0                                        FQM      54
C      900 KEN(13)=KEN(13)+1                              FQM      55
34     900 KEN(13)=KEN(13)+1                              FQM      56
C      900 CALL EQMS (KEV,EMX,EMN,EMG)                   FQM      57
36     900 CALL EQMS (KEV,EMX,EMN,EMG)                   FQM      58
C      910 DO 920 I=1,6                                    FQM      59
42     920 KEV(I+7)=KEV(I+6)                              FQM      60
50     920 KEV(I+7)=KEV(I+6)                              FQM      61
C      950 CALL DOUT (3HEQM,2)                            FQM      62
52     950 CALL DOUT (3HEQM,2)                            FQM      63
C      1000 EV=0.0                                         FQM      64
55     1010 DO 1050 I=1,KS                                 FQM      65
56     1020 EV=EV+ABS(EMX(I)-EA(I))                       FQM      66
60     1030 IF (KEN(13)-1) 1050,1050,1040               FQM      67
64     1040 EMX(I)=(EMX(I)+EA(I))/2.0                    FQM      68
67     1050 CONTINUE                                       FQM      69
73     1050 CONTINUE                                       FQM      70
73     1050 CONTINUE                                       FQM      71

```

76	C		EQU	72
		1070 CALL DOUT (3HEQM,3)	EQU	73
	C		EQU	74
		INNER CONVERGENCE TEST	EQU	74
101		1100 IF (EV-FUR(16)) 1300,1300,1110	EQU	75
104		1110 CALL XIM(2,2)	EQU	76
107		1120 GO TO 500	EQU	77
	C		EQU	78
		OUTER CONVERGENCE TEST	EQU	78
110		1100 IF ((KAL(5)-3)*(KAL(5)-4)) 2000,1310,2000	EQU	79
114		1110 IF (ABS(RSTA-RSTAT)-EPS) 1320,200,200	EQU	80
121		1120 VR=X*MT(1)	EQU	81
	C		EQU	82
		CALC FINAL THERMU	EQU	83
123		2000 CALL XIM(2,3)	EQU	84
126		2004 CALL DOUT (3HEQM,3)	EQU	85
	C		EQU	86
131		3000 RETURN	EQU	87
	C		EQU	88
		END	EQU	89
132			EQU	90
	C	*****	MES	2
	C	4. CALCULATION 4UNHOLS	MES	3
	C	*****	MES	4
		SUBROUTINE MES	MES	5
	C		MES	6
		MIXTURE EQUATION OF STATE CONTROL	MES	7
		CALCULATE EQUATION OF STATE AT	MES	8
		GIVEN T AND P	MES	9
			MES	10
		REPLACE (CALL SEM) BY (CALL SEP)	MES	11
		IF SEP REQUIRES IJEN. FOR V(P,T),	MES	12
		INPUT	MES	13
		THER(1),(2) = P,T (IMPLICIT)	MES	14
		OUTPUT = SEE COUT	MES	15
			MES	16
		MES	MES	17
			MES	18
1		COMMON 7(4000)	MES	19
1		DIMENSION KEN(60)	MES	20
			MES	21
1		EQUIVALENCE	MES	22
		1 (7(1620),KEN)	MES	23
	C		MES	24
1		KEN(11)=0	MES	25
1		KEN(12)=0	MES	26
1		KEN(13)=0	MES	27
1		KEN(6)=KEN(6)+1	MES	28
1		KEN(17)=KEN(14)+1	MES	29
6		CALL DOUT (3HMES,1)	MES	30
	C		MES	31
10		CALL TIM(2)	MES	32
12		CALL SEM (2,1)	MES	33
14		CALL EQM	MES	34
15		CALL TIM(2)	MES	35
17		CALL COUT	MES	36
	C		MES	37
20		CALL DOUT (3HMES,2)	MES	38
22		RETURN	MES	39
	C		MES	40
		END	MES	41

	SUBROUTINE COUT	COUT	2
C	CALCULATE MES OUTPUT	COUT	3
C	CALLED FROM MES	COUT	4
C		COUT	5
C	INPUT - ECS ROUTINES OUTPUT	COUT	6
C	EMN(1), EMN(2) = NS, NG	COUT	7
C	TMS = IDEAL	COUT	8
C	THER(1), (3) = P, T	COUT	9
C	XMT = GAS	COUT	10
C	SM = SOLID	COUT	11
C	HE = INITIAL	COUT	12
C	EMS = MOLE FRACTIONS	COUT	13
C	EMG = MU SUM I PRIME (IMPERF. CHEM. POTENTIALS)	COUT	14
C	OUTPUT	COUT	15
C	REST OF EMN - PHASE COMPOSITION	COUT	16
C	THER = THERMO FUNCTIONS	COUT	17
C	FN = MOLE NUMBERS	COUT	18
C	FMU = CHEM. POTENTIALS	COUT	19
1	COMMON / (4000)	COUT	20
1	DIMENSION	COUT	21
	1 CONT (20), EMG (20), EMN (20)	COUT	22
	2*EMX (20), EV (20), FN (20)	COUT	23
	3*FMU (20), HE (10), KIM (10)	COUT	24
	4*SM (20), THER (50), TMS (20)	COUT	25
	5*XMT (30)	COUT	26
1	EQUIVALENCE	COUT	27
	1 (Z(450), CONT) , (Z(1410), EMG) , (Z(1030), EMN)	COUT	28
	2*(Z(1170), EMX) , (Z(680), EV) , (Z(1390), FN)	COUT	29
	3*(Z(1370), FMU) , (Z(1570), HE) , (Z(1680), KIM)	COUT	30
	4*(Z(1820), SM) , (Z(1920), THER) , (Z(1990), TMS)	COUT	31
	5*(Z(2210), XMT)	COUT	32
C		COUT	33
1	EQUIVALENCE (CONT(2),R), (CONT(4),CALMB)	COUT	34
1	EQUIVALENCE (THER(1),P), (THER(3),T)	COUT	35
1	EQUIVALENCE (THER(5),U), (THER(8),V), (THER(9),E)	COUT	36
1	EQUIVALENCE (THER(11),M), (THER(11),A), (THER(12),F)	COUT	37
1	EQUIVALENCE (THER(13),S), (THER(15),VM)	COUT	38
1	EQUIVALENCE (KIM(2),KS)	COUT	39
1	EQUIVALENCE (HE(5),V0), (HE(7),MU)	COUT	40
1	EQUIVALENCE (SM(1),VS)	COUT	41
1	EQUIVALENCE (EMN(4),XG), (EMN(5),XS), (EMN(6),BY)	COUT	42
1	EQUIVALENCE (TMS(2),HGID), (TMS(4),SGID), (TMS(6),HMGID)	COUT	43
	1 (TMS(7),HSID), (TMS(9),SSID), (TMS(12),HMSID)	COUT	44
	2 (TMS(5),HFG), (TMS(11),MFS)	COUT	45
1	8 EMN(3)=F(1)(2)+EMN(1)	COUT	46
3	10 AG=EMN(1)/EMN(3)	COUT	47
5	20 AS=EMN(2)/EMN(3)	COUT	48
7	30 VM=XG*XMT(1)+XS*VS	COUT	49
13	40 THER(21)=P*VM/(R*T)	COUT	50
17	50 THER(17)=XG*(HGID+XMT(3))+XS*(HSID+SM(3))	COUT	51
25	60 THER(20)=XG*(SGID+XMT(6))+XS*(SSID+SM(6))	COUT	52
33	70 THER(16)=THER(17)-THER(21)	COUT	53
35	80 THER(19)=THER(17)-THER(20)	COUT	54
37	90 THER(18)=THER(19)-THER(21)	COUT	55
41	100 BN=EMN(3)/HE(4)	COUT	56
43	110 EV=BN*R*T	COUT	57
46	120 V=BN*VM	COUT	58

```

50 130 E=FV*THEX(16)
52 140 M=FV*THEX(17)
54 150 A=FV*THEX(18)
56 160 F=FV*THEX(19)
60 170 S=HNR*THEX(20)
63 172 THEX(14)=EV*(XG*(HMGID+XMI(J))+XS*(HMSID+SM(3)))
72 190 THEX(2)=V/V0
74 200 Q=-HNR*CAL*H*(XG*HFG+XS*HF)+MU*HNR*HE(3)
105 210 THEX(7)=J/CALMB
107 220 FN(1)=EMN(2)
111 230 DO 240 J=2,KS
117 240 FN(I)=EMN(I)*EMN(1)
121 250 DO 260 I=1,KS
123     E1=0
123     IF (EMX(I).NE.0) E1=ALOG(EMX(I))
133 260 FMU(I)=FMG(I)*E1
135 270 FMU(I)=EMG(I)
C
137 300 RETURN
C     SPECS
C     INPUT
C     P,T,ROUTINE OUTPUTS
C     OUTPUT
C     THERE REF.STATE IS ELEMENTS AT 0 K.
C     HOLE NUMBERS
140 END

```

```

C SURROUTINE POUT(K)
C
C
C     PRINT OUTPUT
C
C     K=1 PRINT LABELS
C     K=2 MAIN PRINT
C     K=3 DIFFERENTIALION PRINT
C
C     PRINT POINT NUMBER AND P,V,T,KHO ON LINE
C
C
C     REVISION 1. ADD PUNCH OUTPUT (KAL(11) ON)
C     * F. 10/16/61
C
C     POUT
C
3     COMMON Z(4000)
3     DIMENSION
1     EMN ( 20),FN ( 20),GM ( 40)
2     HE ( 10),KAL ( 20),KEN ( 6, 10)
3     SM ( 20),THEX ( 50),XMT ( 30)
4     FLAB ( 12, 8),KIM(10)
3     EQUIVALENCE
1 (7( 1030),EMN ) ,(2( 1390),FN ) ,(2( 1490),GM )
2,(2( 1590),HE ) ,(2( 1600),KAL ) ,(2( 1620),KEN )
3,(7( 1620),SM ) ,(2( 1920),THEX ) ,(2( 2210),XMT )
4,(2( 3100),FLAB ) ,(2(1680),KIM)
C
3     EQUIVALENCE (KIM(2),KS)

```

	C		POUT	34
3		10 GO TO (100,180,300),K	POUT	35
	C	96 LABELS	POUT	36
	C	98	POUT	37
12		100 WRITE(9,7100)	POUT	38
17		120 WRITE(9,7120)	POUT	39
24		140 WRITE(9,7130)	POUT	40
30		IF(0.EQ.0) GO TO 400	POUT	41
	C	--- SKIP PUNCH	POUT	42
32		142 IF (KAL(11)) 400,150,400	POUT	43
	C		POUT	44
33		150 WRITE(9,7150) ((FLAB(J,I),J=1,12),I=1,4)	POUT	45
50		160 WRITE(9,7160)	POUT	46
55		162 WRITE(9,7162) (FLAB(I,5),I=1,KS)	POUT	47
65		164 WRITE(9,7164)	POUT	48
72		170 GO TO 400	POUT	49
	C	176 REG. PRINT	POUT	50
	C	178	POUT	51
73		180 KEM(9)=KEM(9)+1	POUT	52
75		200 WRITE(9,7200) KEM(9)	POUT	53
		1 . (THER(I),I=1,5),HE(1),THER(7)	POUT	54
		2 . THER(8),THER(9),THER(13), (EMN(I),I=1,3),EMN(7)	POUT	55
124		230 WRITE(9,7210) THER(15),THER(16),	POUT	56
		1 THER(20),THER(21), (FN(I),I=1,3),XMT(1),XMT(2),	POUT	57
		2 XMT(6),XMT(7), (FN(I),I=4,6),GM(15),GM(4),GM(11),	POUT	58
		3 GM(10), (FN(I),I=7,9),SM(1),SM(2),SM(6),SM(7), (FN(I),I=10,12)	POUT	59
		4 , (XMT(I+15), I=1,3)	POUT	60
210		240 CALL DOUT (4HPOUT,1)	POUT	61
213		IF(0.EQ.0) GO TO 400	POUT	62
	C	--- SKIP PUNCH	POUT	63
215		242 IF (KAL(11)) 400,250,400	POUT	64
	C		POUT	65
216		250 WRITE(9,7250)	POUT	66
		1,HE(1),THER(1),THER(2),THER(3),THER(4),THER(5)	POUT	67
		2,THER(8),THER(9),XMT(16),XMT(18),XMT(17),THER(7)	POUT	68
		3,EMN(2),EMN(1),EMN(3),SM(1),XMT(1),THER(15)	POUT	69
		4,(FN(I),I=1,12)	POUT	70
271		260 GO TO 400	POUT	71
	C	276 DIFF. PRINT	POUT	72
	C	298	POUT	73
272		300 WRITE(9,7300) (THER(I),I=22,25)	POUT	74
301		310 CALL DOUT (4HPOUT,2)	POUT	75
304		IF(0.EQ.0) GO TO 400	POUT	76
	C	---SKIP PUNCH	POUT	77
306		312 IF (KAL(11)) 400,320,400	POUT	78
	C		POUT	79
307		320 WRITE(9,7320)	POUT	80
		1 THER(22),THER(23),THER(24),THER(25),THER(27)	POUT	81
326		400 RETURN	POUT	82
		7100 FORMAT (1H0,7X,13HOUTPUT LABELS//12X,1H1,6X,	POUT	83
		11HP,14X,4 HV/V0,11X,1HT,14X,1HU,14X,1HU,14X,3HRHO,12X,4HGCAL	POUT	84
		2/12X,1HP,6X,1HV,14X,1HE,14X,1HS,14X,2HNS,13X,2HNS,13X,1HN,14X	POUT	85
		36HSUPSAT)	POUT	86
	C		POUT	87
		7120 FORMAT (12X,1H3,6X,1HV,14X,4HE/RT,11X,3HS/R,12X,5HPV/RT,	POUT	88
		110X,2HN1,13X,2HN2, 3X,2HN3 / 12X,1H4,6X,11HUO, FOR GAS,	POUT	89
		249X,6HN4,6S,NS/12X,1HS,6X,12HUO, FOR REF.,48X,8HN7,NS,N9	POUT	90
		3/12X,1H6,6X,13HDU, FOR SOLID,47X,11HN10,N11,N12)	POUT	91
	C		POUT	92
		7130 FORMAT (12X,1H7,6X,5HRBAR*,10X,5HTBAR*,10X,5HVBAR*,10X	POUT	93

	1	,5HGAMMA,10X,5HALPHA,10X,4MBETA,11X,1HC)	POUT	94
C			POUT	95
C			POUT	96
	7200	FORMAT (1H0,6HP0IN1 12,3X	POUT	97
	1	,3M1 1P/E15.7/12X,3H2 7E15.7)	POUT	98
C			POUT	99
	7210	FORMAT (12X,3H3 1P7E15.7/12X,3H4 7E15.7/12X,	POUT	100
		13H5 7E15.7/12X3H6 7E15.7 / 2X,3H7 3E15.7)	POUT	101
C			POUT	102
	7200	FORMAT (1H+,14X,45X, 1P4E15.7)	POUT	103
C			POUT	104
C		PUNCH FORMATS	POUT	105
	7150	FORMAT	POUT	106
	1	(2H51 11A6,AB / (2H50 11A6,AB))	POUT	107
327	7160	FORMAT (POUT	108
		1*H501 3*H50 4X,1HP 11X,4HV/V0 8X,1HT 11X,1HU 11X,1MU	POUT	109
		2/4H5 2 1HV 11X,1HE 11X,4HKBAR 8X,4HVBAR 8X,4HTBAR 8X,1MU	POUT	110
327	7162	FORMAT (1H5 6A12)	POUT	111
327	7164	FORMAT (POUT	112
		1/4H5 5HGAMMA 7X,5HALPHA 7X,4MBETA 8X,1HC 11X,6HCJ FN	POUT	114
		7)	POUT	115
327	7250	FORMAT (2H50 1PE11.4 ,5E12.4 / (1H5 6E12.4))	POUT	116
327	7320	FORMAT (2H5 1PE11.4 ,5E12.4)	POUT	117
327		END	POUT	118

		SUBROUTINE MESC(KG,ASUC)	MESC	2
C			MESC	3
C		CALCULATE MIXTURE EQUATION OF STATE	MESC	4
C		AT GIVEN T AND	MESC	5
C		P FOR KG=1	MESC	6
C		V FOR KG=2	MESC	7
C		S FOR KG=3	MESC	8
C		E FOR KG=4	MESC	9
C			MESC	10
C		ITERATE ON T UNDER CONTROL OF FROOT,	MESC	11
C		USING MES FOR FUNCTION CALCULATION	MESC	12
C			MESC	13
C			MESC	14
C		ALL USE SAME FROOT CALL,	MESC	15
C		BRANCH ON FUNCTION	MESC	16
C			MESC	17
C		REVISION 1.CALC INTEGRAL PDV ON ISE	MESC	18
C		*. F. 1/3/62	MESC	19
C		MESC	MESC	20
	6	COMMON Z(4000)	MESC	21
	6	DIMENSION	MESC	22
		1,KEN (60),KON (6*10),CAR (80)	MESC	24
		2,FOH (60),THER (50)	MESC	25
		5,CONT(20),HE(10)	MESC	26
6		DIMENSION ASUC (10)	MESC	27
C		ASUC - INITIAL STATE ON CURVE - SEE SUC	MESC	28
6		EQUIVALENCE	MESC	29
		1 (Z(1620),KEN) ,(Z(1690),KON) ,(Z(920),CAR)	MESC	30
		2 (Z(1410),FOH) ,(Z(1420),THER)	MESC	31
		5 (Z(460), CONT),(Z(1590),HE)	MESC	32
C			MESC	33
6		DIMENSION CM(10),KCM(2)	MESC	34

6	EQUIVALENCE (CAR(21),CM), (CM(8),KCM)	MESC	35
6	EQUIVALENCE (THEK(8),V), (THER(13),S), (THER(9),L)	MESC	36
6	EQUIVALENCE (THER(3),T)	MESC	37
C		MESC	38
6	4 KEN(14)=0	MESC	39
7	6 KEN(8)=KEN(8)+1	MESC	40
11	8 KEN(19)=KEN(16)+1	MESC	41
13	10 IF (KG=1) 30,15,30	MESC	42
15	15 I=ASUC(1)	MESC	43
16	20 CALL MES	MESC	44
21	25 GO TO 200	MESC	45
22	30 KCM(1)=0	MESC	46
23	35 CM(4)=T	MESC	47
25	40 CM(2)=T*FOR(9)	MESC	48
27	45 CALL FRGOTT (CM,KON(3,8))	MESC	49
34	46 KEXIT=KCM(2)	MESC	50
36	50 GO TO (200,80,70,60), KEXIT	MESC	51
46	60 CALL DBUG (4HMESC,1)	MESC	52
53	62 GO TO 200	MESC	53
56	70 CALL DBUG (4HMESC,2)	MESC	54
61	72 GO TO 200	MESC	55
62	80 T=CM(2)	MESC	56
64	CALL MES	MESC	57
65	I*KG-1	MESC	58
70	GO TO (40,100,110),I	MESC	59
76	90 CM(3)=V-ASUC(3)	MESC	60
100	95 GO TO 120	MESC	61
101	100 CM(3)=((EXP((S/ASUC(4))*ALOG(ASUC(1))))/ASUC(1))-1.	MESC	62
116	105 GO TO 120	MESC	63
117	110 CM(2)=E-ASUC(5)	MESC	64
121	120 CALL DOUT (4HMESC,1)	MESC	65
126	125 GO TO 45	MESC	66
C		MESC	67
127	200 IF (KG=3) 220,210,220	MESC	68
131	210 THER(4)=(HE(8)-THER(9))/CONT(4)	MESC	69
C		MESC	70
134	220 CALL DOUT (4HMESC,2)	MESC	71
141	300 RETURN	MESC	72
142	END	MESC	73

	SUBROUTINE HUG	HUG	2
C	DETONATION HUGONIOT POINT	HUG	3
C	NCIES	HUG	4
C	1. SPECIAL SECOND GUESS - FROM FIRST	HUG	5
C	ARG AND FUNC AND SLOPE SAVED IN FOR(D)	HUG	6
C	FROM PREVIOUS ITER	HUG	7
1	COMMON Z(4000)	HUG	8
1	DIMENSION	HUG	9
1	1 CAR (10,8), KEN (6,10), KON (6,10)	HUG	10
1	2, FOR (60), HE (10), THER (50)	HUG	11
1	DIMENSION CM(10), KCM(2)	HUG	12
1	EQUIVALENCE	HUG	13
1	1 (Z(920), CAR) , (Z(1620), KEN) , (Z(1690), KON)	HUG	14
1	2, (Z(1410), FOR) , (Z(1590), HE) , (Z(1920), THER)	HUG	15
C		HUG	16
C		HUG	17
1	EQUIVALENCE (THER(1),P), (THER(3),T), (THER(4),U)	HUG	18
1	EQUIVALENCE (THER(5),V), (THER(6),V), (THER(14),MK)	HUG	19
1	EQUIVALENCE (HE(2),P0), (HE(6),V0), (HE(7),M0)	HUG	20

1	EQUIVALENCE (FOB(21),TL),(FOB(22),TU)	HUG	21
1	EQUIVALENCE (CAR(11),CH),(CH(8),KCH)	HUG	22
C		HUG	23
C	CALCULATE HUGONIOT POINT AT GIVEN P,	HUG	24
C	ITERATE ON T UNDER CONTROL OF FROUT,	HUG	25
C	USING MES IN FUNCTION CALCULATION	HUG	26
C		HUG	27
C	TL AND TU ARE BOUNDS ON ITERATION T	HUG	28
C		HUG	29
1	4 KEN(14)=0	HUG	30
2	6 KEN(15)=KEN(15)+1	HUG	31
4	8 KEN(7)=KEN(7)+1	HUG	32
6	10 IF (T)20,12,20	HUG	33
7	12 T=3000.0	HUG	34
11	20 CH(4)=T/1000.	HUG	35
13	30 KCH(1)=0	HUG	36
14	40 CALL FROUTT (CH,KON(2,8))	HUG	37
17	42 NEXIT=KCH(2)	HUG	38
21	50 GO TO (150,72,70,60),KEXIT	HUG	39
31	60 CALL DBUG (3HHUG,1)	HUG	40
34	62 GO TO 150	HUG	41
35	70 CALL DBUG (3HHUG,2)	HUG	42
40	71 GO TO 150	HUG	43
41	72 IF (KON (2,8)) 81,75,81	HUG	44
42	75 IF (KCH(1)=2) 81,76,81	HUG	45
44	76 CH(2)=CH(4)-CH(5)/PCB(8)	HUG	46
47	81 I=CH(5)*1000.	HUG	47
51	82 IF (TU-T) 83,83,85	HUG	48
54	83 I=TU	HUG	49
56	84 GO TO 90	HUG	50
57	85 IF (T-TL) 86,90,90	HUG	51
62	86 T=TL	HUG	52
64	90 CALL MES	HUG	53
65	92 U=V0*SQRT((P-P0)/(V0-V))	HUG	54
75	94 U=SQRT((P-P0)*(V0-V))	HUG	55
104	95 CH(2)=T/1000.	HUG	56
106	100 CH(3)=20.*P*((H-H0)/((P-P0)*V0)-0.5*(1.0+V/V0))	HUG	57
121	110 CALL DOUT (3HHUG,1)	HUG	58
124	120 GO TO 40	HUG	59
125	150 IF (KCH(1)=2) 200,200,151	HUG	60
130	151 FOR(8)=(CH(7)-CH(3))/(CH(6)-CH(2))	HUG	61
134	200 RETURN	HUG	62
C		HUG	63
C		HUG	64
135	END	HUG	65
C		GAMM	2
C	SUBROUTINE GAMM(K1,K2)	GAMM	3
C		GAMM	4
C	CALCULATE EQUATION OF STATE DERIVATIVES	GAMM	5
C	RYNUMERICAL DIFFERENCING OF P AND T	GAMM	6
C	USING MES FOR EQ. OF STATE POINTS	GAMM	7
C		GAMM	8
C	INPUT	GAMM	9
C	(1) K1=1 - DIFFERENTIATE WITH CURRENT CONDITION	GAMM	10
C	(FIXED OR EQUILIBRIUM COMPOSITION)	GAMM	11
C	(2) K2=1 - DIFFERENTIATE AT FIXED COMPOSITION	GAMM	12
C		GAMM	13
C	(3) THER (1) P CENTER POINT QUANTITIES	GAMM	14


```

C          (3) T          GAMM 15
C          (2) V          GAMM 16
C          (21) PV/RT     GAMM 17
C
C          (4) EMN       (3) N          GAMM 18
C          (3) N          GAMM 19
C          (4) EMN       (3) N          GAMM 20
C          OUTPUT
C          SUCG          (1) GAMMA      GAMM 21
C          (2) ALPHA     GAMM 22
C          (3) BETA      GAMM 23
C          (4) C (SOUND SPEED)      GAMM 24
C          (5) CJ FJUNCTION          GAMM 25
C          =((V/VOI)/(GAM/(GAM+1-P/PO)) )*(GAM-1) GAMM 26
C          (6) CAP GAMMA (ISOTHERMAL) GAMM 27
C          (7) CP/M      GAMM 28
C          (8) (C LN V/U T) (CONSTANT P) GAMM 29
C
C          ABOVE OUTPUT IS FORMED FOR EITHER GAMM 30
C          OR BOTH CONDITIONS AND PLACED IN GAMM 31
C          APPROPRIATE IHER LOCATIONS GAMM 32
C
C          DATA)
C          FOH           (13) H = H* = PCOR GAMM 33
C          FOH           (14) DEL = T* = IC*(1.0+DEL) GAMM 34
C          DER           (1) PC          GAMM 35
C          (2) VC        GAMM 36
C          (3) TC        GAMM 37
C          (4) PC*VC/R*TC GAMM 38
C          (5) V+        GAMM 39
C          (6) V-        GAMM 40
C          (7) H+        GAMM 41
C          (8) H-        GAMM 42
C          E2           SAVE NC        GAMM 43
C          GAMM          GAMM 44
C          GAMM          GAMM 45
C          GAMM          GAMM 46
C          GAMM          GAMM 47
C          GAMM          GAMM 48
C          GAMM          GAMM 49
C          GAMM          GAMM 50
C          COMMON Z(4000) GAMM 51
C          DIMENSION    GAMM 52
C          1 DER ( 10) ,EMN ( 20) ,FOH ( 60) GAMM 53
C          2,HF ( 10) ,KAL ( 20) ,IHER ( 50) GAMM 54
C          3,SUCG ( 20) GAMM 55
C          EQUIVALENCE GAMM 56
C          1 (7( 1000),DER ) ,(Z( 1030),EMN ) ,(Z( 1410),FOH ) GAMM 57
C          2,(7( 1500),HF ) ,(Z( 1000),KAL ) ,(Z( 1920),IHER ) GAMM 58
C          3,(Z( 1900),SUCG ) GAMM 59
C          EQUIVALENCE (IHER(1),P)*(IHER(3),T)*(IHER(8),V) GAMM 60
C          18 SAVE CENTER VALUES GAMM 61
C          20 DER(1)=P GAMM 62
C          30 UEP(2)=V GAMM 63
C          10 UEP(3)=T GAMM 64
C          14 UEP(4)=IHER(21) GAMM 65
C          16 UEP(5)=EMN(3) GAMM 66
C          78 MAIN CODE /TEST ARGS. GAMM 67
C          GAMM 68
C          GAMM 69
C          20 IF (K2) 110,400,110 GAMM 70
C          21 IF (KAL(6)) 200,400,200 GAMM 71
C          158 DIFF. AT FIX. COMP. GAMM 72
C          22 200 LM=KAL(6) GAMM 73
C          24 210 KAL(6)=0 GAMM 74

```

25	220	K=1		GAMM	75
26	230	GO TO 1000		GAMM	76
	C 248		SET OUTPUT	GAMM	77
27	200	THEX(26)=SUCG(1)		GAMM	78
31	210	THEX(30)=SUCG(2)		GAMM	79
33	220	THEX(29)=SUCG(4)		GAMM	80
35	230	THEX(28)=SUCG(5)		GAMM	81
37	240	NAL(6)=LM		GAMM	82
41	250	CALL DOUT (4HGAMM,1)		GAMM	83
	C 298		DIFF. AT EQ.COMP.	GAMM	84
46	200	IF (K1)410,600,410		GAMM	85
47	410	K=2		GAMM	86
51	420	GO TO 1000		GAMM	87
	C 448		SET OUTPUT	GAMM	88
51	500	THEX(22)=SUCG(1)		GAMM	89
53	510	THEX(23)=SUCG(2)		GAMM	90
55	520	THEX(24)=SUCG(3)		GAMM	91
57	530	THEX(25)=SUCG(4)		GAMM	92
61	540	THEX(27)=SUCG(5)		GAMM	93
63	550	CALL DOUT (4HGAMM,1)		GAMM	94
	C 598			GAMM	95
70	400	RETURN		GAMM	96
	C 944			GAMM	97
	C 946		DIFFERENCE SUBROUTINE	GAMM	98
	C 948		DELTA P	GAMM	99
71	1000	P=FOR(13)*DER(1)		GAMM	100
73	1004	I=DER(3)		GAMM	101
75	1010	CALL MES		GAMM	102
100	1020	DER(5)=V		GAMM	103
102	1030	P=DER(1)/FOR(13)		GAMM	104
104	1040	CALL MES		GAMM	105
107	1050	DER(6)=V		GAMM	106
111	1060	SUCG(6)=-2.0*ALOG(FCB(13))/ALOG(DER(5)/DER(6))		GAMM	107
	C1096			GAMM	108
	C1098		DELTA T	GAMM	109
124	1100	P=DER(1)		GAMM	110
125	1104	I=DER(3)*(1.0+FOR(14))		GAMM	111
131	1110	CALL MES		GAMM	112
134	1120	DER(5)=V		GAMM	113
136	1130	DER(7)=THEX(17)*T*EMN(3)		GAMM	114
141	1140	I=DER(3)*(1.0+FCB(14))		GAMM	115
144	1150	CALL MES		GAMM	116
147	1160	DER(6)=V		GAMM	117
151	1170	DER(8)=THEX(17)*T*EMN(3)		GAMM	118
154	1180	SUCG(7)=(DER(7)-DER(8))/(2.0*DER(3)*FCB(14)*E2)		GAMM	119
162	1190	SUCG(8)=ALOG(DER(5)/DER(6))/(2.0*DER(3)*FUB(14))		GAMM	120
	C1246			GAMM	121
	C1248		CALC. OUTPUT	GAMM	122
174	1200	I=DER(3)		GAMM	123
176	1202	V=DER(2)		GAMM	124
200	1204	E1=DER(4)*T*SUCG(8)/SUCG(7)		GAMM	125
204	1210	SUCG(1)=SUCG(6)/(1.0-SUCG(6)*E1)*T*SUCG(d)		GAMM	126
211	1220	SUCG(3)=1.0/(SUCG(4)*E1)		GAMM	127
214	1230	SUCG(2)=SUCG(1)*SUCG(3)-1.0		GAMM	128
217	1240	SUCG(4)=SQRT(SUCG(1)*DER(1)*DER(2))		GAMM	129
226	1250	SUCG(5)=(V/DE(6))/(SUCG(1)/(SUCG(1)+1.0-DE(2)/DER(1)))		GAMM	130
234	1260	SUCG(5)=SUCG(5)*(-SUCG(1))-1.0		GAMM	131
	C			GAMM	132
242	1400	GO TO (300,500),K		GAMM	133
	C			GAMM	134

250	C	END	GAMM	135
			GAMM	136
		SUBROUTINE PV(ICPY)	PV	2
	C		PV	3
	C	CALCULATE ISOTHERM, ISOCORE, ISENTROPE,	PV	4
	C	OR CONSTANT-ENERGY POINTS	PV	5
	C	AT VALUES OF P IN PI ARRAY	PV	6
	C	(FOR KAL(8)=1,2,3,4)	PV	7
	C	INPUT	PV	8
	C	SUC(1), (2) = TC, PC (INITIAL POINT)	PV	9
	C	KAL(1), KAL(2) = DIFF SWITCHES	PV	10
	C	KAL(4) = 1,2,3,4 FOR CONSTANT T, V, S, E	PV	11
	C	PT = PRESSURE TABLE	PV	12
	C	OUTPUT	PV	13
	C	PRINTED POINT OUTPUT	PV	14
	C	-----	PV	15
	C	REVISION 1. LEAVE P CORRECT ON EXIT	PV	16
	C	FOR RESTART OPTION	PV	17
	C	W. F. 3/1/64	PV	18
	C		PV	19
	C	PV	PV	20
		COMMON Z(4000)	PV	21
3		DIMENSION	PV	22
3		1 KAL (20) ,KEN (60) ,PT (50)	PV	23
		2,SUC (20) ,THER (50)	PV	24
3		EQUIVALENCE	PV	25
		1 (7(1600),KAL) ,(Z(1620),KEN) ,(Z(1750),PT)	PV	26
		2*(Z(1880),SUC) ,(Z(1920),THER)	PV	27
	C		PV	28
3		EQUIVALENCE (THER(1),P),(THER(3),T)	PV	29
3		EQUIVALENCE (THER(8),V),(THER(9),E),(THER(13),S)	PV	30
	C		PV	31
3		8 KEN(16)=0	PV	32
	C		PV	33
		12 CALL POUT (1)	PV	34
4		14 I=SUC(1)	PV	35
7		16 P=SUC(2)	PV	36
11		18 CALL MES	PV	37
13		20 CALL POUT(2)	PV	38
15		22 SUC(3)=V	PV	39
21		24 SUC(4)=S	PV	40
22		26 SUC(5)=E	PV	41
24		28 IF (KAL(1)+KAL(2)) 70,112,70	PV	42
26		30 CALL GAMM (KAL(1),KAL(2))	PV	43
30		32 CALL POUT(3)	PV	44
33		34 I=I+1	PV	45
37		36 IF (PT(I)) 200,200,116	PV	46
40		38 P=PT(I)	PV	47
42		40 CALL MESC (KAL(8),SUC)	PV	48
44		42 CALL POUT(2)	PV	49
50		44 IF (KAL(1)+KAL(2)) 130,140,130	PV	50
53		46 CALL GAMM (KAL(1),KAL(2))	PV	51
55		48 CALL POUT(3)	PV	52
61		50 I=I+1	PV	53
64		52 GO TO 114	PV	54
66		54 RETURN	PV	55
67		56 END	PV	56
70			PV	57

	SUBROUTINE TED	TEL	2
C		TEL	3
C	DETONATION HUGONIOT CONTROL	TEL	4
C	CALCULATE DET. HUG. POINTS AT P VALUES	TEL	5
C	FOUND IN PT ARRAY	TEL	6
C		TEL	7
C	INPUT	TEL	8
C	KAL(1), KAL(2) - DIFF SWITCHES	TEL	9
C	PT - PRESSURE TABLES	TEL	10
C	OUTPUT	TEL	11
C	PRINTED POINT OUTPUT	TEL	12
C	-----	TEL	13
C		TEL	14
C	REVISION 1. LEAVE P CORRECT ON EXIT	TEL	15
C	FOR RESTART OPTION	TEL	16
C	W. F. 3/1/62	TEL	17
C		TEL	18
C	TED	TEL	19
C		TEL	20
1	COMMON 7(4000)	TEL	21
1	DIMENSION	TEL	22
	1 KAL (20) ,PT (50)	TEL	23
	2, THER (50)	TEL	24
1	EQUIVALENCE	TEL	25
	1 (7(1600), KAL) , (2(1/50), PT)	TEL	26
	2 * (2(1920), THER)	TEL	27
C		TEL	28
1	EQUIVALENCE (THER(1), P)	TEL	29
C		TEL	30
C	SET T_GUESS ON FIRST ENTRY	TEL	31
1	12 CALL POUT(1)	TEL	32
3	20 I=1	TEL	33
4	30 IF (PT(I)) 200, 200, 40	TEL	34
6	40 P=PT(I)	TEL	35
10	50 I=I+1	TEL	36
12	60 CALL HUG	TEL	37
13	70 CALL POUT(2)	TEL	38
15	80 IF (KAL(1)+KAL(2)) 100, 30, 100	TEL	39
17	100 CALL GAMM (KAL(1), KAL(2))	TEL	40
22	150 CALL POUT(3)	TEL	41
24	180 GO TO 30	TEL	42
25	200 RETURN	TEL	43
C		TEL	44
26	END	TEL	45

	SUBROUTINE CJ	CJ	2
C		CJ	3
C	CALCULATE CJ LOCUS AT VALUES OF RHO ZERO	CJ	4
C	IN ROT TABLE	CJ	5
C		CJ	6
C	ITERATE ON P ALONG HUGONIOT UNTIL	CJ	7
C	CJ CONDITION IS SATISFIED	CJ	8
C	INPUT	CJ	9
C	KAL(1), KAL(2) - DIFF SWITCHES	CJ	10
C	ROT - INITIAL-DENSITY TABLE	CJ	11
C	OUTPUT	CJ	12
C	PRINTED POINT OUTPUT	CJ	13
C	-----	CJ	14

C		CONST. V DEL. P CALCD FROM Q, GAMMA	CJ	15
C		*. F. 11/21/61	CJ	16
C			CJ	17
C		REVISION 2. SAVE INITIAL E FOR INTEGRAL PUV	CJ	18
C		*. F. 1/3/62	CJ	19
C			CJ	20
C			CJ	21
C	CJ		CJ	22
1		COMMON 7(4000)	CJ	23
1		DIMENSION	CJ	24
		1 CAR (10, 8), HE (10), KAL (20)	CJ	25
		2, KON (6, 10), ROT (20), THER (50)	CJ	26
		3, KEN(60)	CJ	27
1		DIMENSION CC(10), KCC(2)	CJ	28
1		EQUIVALENCE	CJ	29
		1 (7(920), CAR) , (2(1590), HE) , (2(1600), KAL)	CJ	30
		2, (7(1690), KON) , (2(1800), ROT) , (2(1920), THER)	CJ	31
		3, (7(1620), KEN)	CJ	32
C			CJ	33
C			CJ	34
1		EQUIVALENCE (CAR(1), CC), (CC(8), KCC)	CJ	35
1		EQUIVALENCE (HE(6), V0), (HE(2), P0), (HE(1), RHO)	CJ	36
1		EQUIVALENCE (THER(1), P), (THER(22), GAM), (THER(26), GAM0)	CJ	37
1		EQUIVALENCE (THER(8), V)	CJ	38
1		EQUIVALENCE (THER(6), Q)	CJ	39
1		6 KEN(15)=0	CJ	40
1		8 KEN(16)=0	CJ	41
2			CJ	42
C	10	W+Q+E INPUT, OUTPUT LABEL	CJ	43
3	30	CALL POUT(1)	CJ	44
5	40	I=1	CJ	45
C	50	M1+E SET UP FROOT	CJ	46
6	60	RHO=ROT(1)	CJ	47
10	65	HE(1)=RHO	CJ	48
12	70	V)=1./RHO	CJ	49
14	72	IF(P) 8., 74., 80	CJ	50
15	74	P=0.3	CJ	51
17	80	CC(4)=P	CJ	52
21	100	KCC(1)=0	CJ	53
C	110	W(G2, G3, G4, G5) FROOT	CJ	54
22	120	CALL FROOT(CC, KON (1,8))	CJ	55
25	130	KEXIT=KCC(2)	CJ	56
27	140	GO TO (365, 200, 180, 160), KEXIT	CJ	57
C	150	M5+0 FROOT ERROR EXIT 1	CJ	58
37	160	CALL DBUG (PHCJ, 1)	CJ	59
42	170	GO TO 365	CJ	60
43	180	CALL DBUG (PHCJ, 1)	CJ	61
46	190	GO TO 365	CJ	62
47	200	IF (KON(1,8)) 260, 204, 260	CJ	63
50	204	IF (KCC(1)-2) 260, 210, 260	CJ	64
52	210	E1=GAM	CJ	65
54	220	IF (GAM) 240, 230, 240	CJ	66
55	230	E1=GAM0	CJ	67
57	240	E2=V0*E1/(E1+1.0-P0/P)	CJ	68
64	250	CC(2)=P*(V/F2)*E1	CJ	69
C			CJ	70
72	260	IF (KCC(1)-2) 280, 280, 262	CJ	71
75	262	E1=GAM	CJ	72
77	284	IF (GAM) 268, 266, 268	CJ	73
100	286	E1=GAM0	CJ	74

102	208 IF (CC(2)=0.5*RH0*Q*(E1-1.0)) 270,280,280	CJ	75
111	270 CC(2)=0.5*RH0*Q*(E -1.0)	CJ	76
	C	CJ	77
116	280 P=CC(2)	CJ	78
120	282 KEN(15)=0	CJ	79
121	284 CALL HUG	CJ	80
	C	CJ	81
122	286 IF (KAL(7)) 320,290,320	CJ	82
123	290 CALL GAMM(1.0)	CJ	83
124	300 CC(3)=THER(27)	CJ	84
130	310 GO TO 340	CJ	85
131	320 CALL GAMM(n,1)	CJ	86
134	330 CC(3)=THER(28)	CJ	87
136	340 CALL DOUT (2MCJ,1)	CJ	88
141	350 GO TO 120	CJ	89
	C 350 H2+Q*G*Q	CJ	90
		OUTPUT POINT	
142	365 P=CC(2)	CJ	91
144	370 CALL HUG	CJ	92
	C	CJ	93
		SAVE INITIAL E FOR ISE INTEGRAL	
145	380 ME(8)=THER(9)-THER(4)**2/2.0	CJ	94
151	390 CALL POUT(2)	CJ	95
153	420 CALL GAMM(KAL(1),KAL(2))	CJ	96
154	430 CALL POUT(3)	CJ	97
	C 440 E+C(G1)	CJ	98
		NEXT KNO VALUE	
160	450 I=I+1	CJ	99
162	460 IF (ROT(I)) 60,470,60	CJ	100
164	470 RETURN	CJ	101
	C	CJ	102
	C	CJ	103
	C	CJ	104
	C	CJ	105
165	END	CJ	106
	C*****	CUN	2
	C* S. READ CONTROL	CUN	3
	C*****	CUN	4
	SUBROUTINE CON (ACON)	CUN	5
	C*****	CUN	6
	C INPUT AND CONTROL	CUN	7
	C BRANCH ON EACH CON WORD TO READ INPUT PACK	CUN	8
	C EXECUTE ON TED,PV,CJ	CUN	9
	C-----	CUN	10
	C MAIN CONTROL = CON(ACON)	CUN	11
	C READ INPUT AND EXECUTE AS DIRECTED	CUN	12
	C CALLED FROM	CUN	13
	C 1. MAIN PROGRAM MESU = ACON=0	CUN	14
	C 2. ERR = ACON=1 = SKIP THRU NEXT READ ON INP.	CUN	15
	C THEN REGULAR (NEXT RUN)	CUN	16
	C REVISION 1. = ADD PUNCH OUTPUT	CUN	17
	C * F. 10/18/61	CUN	18
	C REVISION 2 = ADD TO,PC OPTION TO PV	CUN	19
	C * FICKETT 11/20/61	CUN	20
	C REVISION 3. = ADD MEND AND TIME PRINTS	CUN	21
	C W.F. 3/8/62	CUN	22
	C	CUN	23
	C	CUN	24
	C***** COMMONS *****	CUN	25
		CUN	26
3	COMMON Z(4000)	CUN	27

```

1 DIMENSION ( ) CUN 28
1 1 HS ( 40),CAM ( 10, 8),CUNT ( 20) CUN 29
2 2 EMX ( 20),EMX ( 20),EMX ( 20) CUN 30
3 3 FLAB ( 12, 0),FUB ( 6, 10),ME ( 10) CUN 31
4 4 KAL ( 20),KIM ( 10),KUN ( 6, 10) CUN 32
5 5 PT ( 50),RUT ( 20),SUC ( 20) CUN 33
6 6 THER(40) CUN 34
EQUIVALENCE
1 1 (7( 400),MS ) ,(2( 420),CAM ) ,(2( 440),CUNT ) CUN 35
2 2 (7( 1030),EMX ) ,(2( 1170),EMX ) ,(2( 1390),EM ) CUN 36
3 3 (7( 3100),FLAB ) ,(2( 1410),FUB ) ,(2( 1590),ME ) CUN 37
4 4 (7( 1000),KAL ) ,(2( 1580),KIM ) ,(2( 1690),KUN ) CUN 38
5 5 (7( 1700),PT ) ,(2( 1400),RUT ) ,(2( 1880),SUC ) CUN 39
6 6 (2(1920), THER) CUN 40
C***** LOCALS ***** CUN 41
1 LOGICAL I,NE CUN 42
3 DIMENSION E(20),AE(12) CUN 43
7 EQUIVALENCE (KIM(2),KS) CUN 44
3 EQUIVALENCE (HS(27),HLANK),(HS(38),FOHM),(HS(39),HCCQ) CUN 45
4 EQUIVALENCE (HS(2),CPAS),(HS(30),END) CUN 46
7 EQUIVALENCE (HS(24),HCORE),(HS(27),HUB00) CUN 47
1 EQUIVALENCE (RS(33),DULLAM) CUN 48
3 EQUIVALENCE (HS(35),HREN0) CUN 49
3 EQUIVALENCE ( E(1) , CW1 ) , ( E(2) , CW ) CUN 50
C CUN 51
3 EQUIVALENCE (FLA(1),KUNLAB),(FLA(13),MELAB) CUN 52
3 EQUIVALENCE (FLA(20),CURLAB),(FLA(37),SPELAB) CUN 53
C CUN 54
3 EQUIVALENCE (THER(1),P),(THER(3),T) CUN 55
3 EQUIVALENCE (KON(4), WERHGT) CUN 56
C CUN 57
3 DIMENSION R,NLAB(12),MELAB(12),CURLAB(12),SPELAB(12) CUN 58
C***** EXECUTE ***** CUN 59
1 IF (ACCN.EQ.0) GO TO 10 CUN 60
C----- 1. SCAN TO REWD ----- CUN 61
4 20 CALL FIC (3HWIT,AM(1246),12,E,0) CUN 62
10 IF (NE(CM,HREN0)) GO TO 20 CUN 63
C----- 2. BEGIN RUN ----- CUN 64
15 70 CONTINUE CUN 65
15 WERHGT=1. CUN 66
16 80 CALL FIC (3HWIT,13M(246,6410,46) , 4, E, 0) CUN 67
23 90 CALL FIC (3HWIT,14M(11440, 6410, 46) , 4, E, 0) CUN 68
27 IF (NE(CM,HCON)) CUN 69
1 CALL ERR(3LCON, 14LHAD INPUT PACK,E) CUN 70
C CUN 71
C SEARCH FOR CUN BRANCH CUN 72
40 8200 GO H320 [I]=1.36 CUN 73
42 8310 IF (CUN(I)) 8320,H350,H320 CUN 74
C CUN 75
C CUN 76
C CUN 77
45 8320 CONTINUE CUN 78
47 CALL ERR(3HCON, 13MHAD CUN CAMU , E) CUN 79
C8348 CUN 80
54 8350 GO TO (100,200,300,400,500,600 CUN 81
1 ,700,800,900,1000,1100,1200 CUN 82
2 ,1300,1400,1500,1600,1700,1800 CUN 83
3 ,1900,2000,2100,2200,2300,2400 CUN 84
4 ,2500,2600,2700,2800,2900,3000 CUN 85
5 ,3100,3200,3300,3400,3500,3600),I CUN 86
C CUN 87

```

123	C	100 GO TO H1		CUN	88
124	C	198	PAS	CUN	89
124	C	200 CONTINUE	ZERO COMMON	CUN	90
124	C	210 I=1,2900		CUN	91
131		CONT(I)=1.0		CUN	92
133		CALL HEAD(F(1))		CUN	93
135		CALL HEAD(9LBEGIN,KCN)		CUN	94
141	C	220 GO 272 I=1,96		CUN	95
147		252 FLA(I)=BLANK		CUN	96
147		254 GO 200 I=1,10		CUN	97
154		260 NUMLAB(I)=E(I+2)		CUN	98
156		GO TO 80		CUN	99
156	C	300 CONTINUE	SATI	CUN	100
156		CALL HEAD(CUN	101
156		1501DIFF,FXDIFF,GAS,SOLID,MIX,EW,CJ,PV		CUN	102
156		2* =12,KE)		CUN	103
162		302 GO 308 I=1,12		CUN	104
164		304 IF (ABS(C(1,KE(I))) > 308.306,306)		CUN	105
170		306 KAL(I)=F(I)		CUN	106
172		308 CONTINUE		CUN	107
174		310 GO TO H6		CUN	108
175	C	398	FUB	CUN	109
175		400 CALL HEAD(CUN	110
175		10L*, FROOT EPS(CC,CH,CM,CG,CS,C)/RATIOS/UP,DT,EPSTN,CUT/ FROOT		CUN	111
175		2 BOLDUSE		CUN	112
175		2 .30,FC(1)		CUN	113
201		410 GO 424 I=1,5		CUN	114
211		420 CAR(I)=FOM(I)		CUN	115
214		430 GO TO H8		CUN	116
215		500 GO TO H8		CUN	117
216	C	598	DIP	CUN	118
216		600 K0(I)=1		CUN	119
217		610 CALL DIP1		CUN	120
221		620 GO TO H8		CUN	121
222	C	698	DIS	CUN	122
222		700 CALL HEAD (1,-7,KE)		CUN	123
225		710 GO 720 I=1,7		CUN	124
235		720 K0(I+KE)=KE(I+1)		CUN	125
237		730 GO TO H8		CUN	126
240	C	798	DIG	CUN	127
240		800 CALL HEAD (0,-1,KE)		CUN	128
244		820 K0(KE,0)=1		CUN	129
246		830 CALL HEAD (0,1,CAR(5,KE))		CUN	130
254		840 GO TO H8		CUN	131
255	C	898	EMPTY	CUN	132
255		900 GO TO H1		CUN	133
256	C	998	GEM	CUN	134
256		1000 CALL GEM(1)		CUN	135
261		1010 GO TO H8		CUN	136
262	C	1098	SEM	CUN	137
262		1100 CALL SEM(1,1)		CUN	138
266		1110 GO TO H8		CUN	139
267	C	1198	TIM	CUN	140
267		1200 CALL TIM(1)		CUN	141
272		1210 GO TO H1		CUN	142
				CUN	143
				CUN	144
				CUN	145
				CUN	146
				CUN	147

	C1298		XIP	CUN	148
273	1400	CALL XI-1 (1,0)		CUN	149
277	1410	GO TO B7		CUN	150
	C1298		EQ	CUN	151
300	1400	CALL EQP		CUN	152
302	1410	GO TO B8		CUN	153
	C1498		EMPTY	CUN	154
303	1500	GO TO B8D		CUN	155
	C1498		SAM	CUN	156
304	1400	CALL HEAD(14LSAM - INPUT PART 2)		CUN	157
306		CALL REAP (33H KS/ RHO, P0, 10, M0, MFE/ NI S -1, KS)		CUN	158
311		CALL REAP(0,5,HE)		CUN	159
314		CALL REAP(0,KS,FN)		CUN	160
320	1410	HE(6)=1.0/HE(1)		CUN	161
322	1420	HE(7)=HE(5)*CONT(4)/HE(4)		CUN	162
325	1430	EMN(2)=FN(1)		CUN	163
327	1432	EMN(3)=0.0		CUN	164
330	1434	GO 1436 I=1,KS		CUN	165
334	1436	EMN(3)=EMN(3)+FN(I)		CUN	166
337	1440	EMN(1)=EMN(7)-EMN(2)		CUN	167
341	1442	EMN(4)=EMN(1)/EMN(3)		CUN	168
343	1444	EMN(5)=EMN(2)/EMN(3)		CUN	169
345	1450	GO 1452 I=1,KS		CUN	170
353	1452	EMX(1)=FN(I)/EMN(1)		CUN	171
	C			CUN	172
356	1460	GO 1462 I=1,10		CUN	173
363	1462	MELAB(I)=E(I*2)		CUN	174
365	1470	GO TO B8		CUN	175
	C1498		TED	CUN	176
376	1700	CALL HEAD(14LTEC - HUGONIUT)		CUN	177
370		CALL REAP (11H P-TABLE 3, 0, PT)		CUN	178
	C			CUN	179
374	1710	CALL TED		CUN	180
376	1720	GO TO B8		CUN	181
	C1798		PV	CUN	182
377	1900	CALL HEAD(SLLOCUS)		CUN	183
401		CALL REAP(CUN	184
		150.1 BRANCH (1-T,2-V,3-S,4-E) / TC,PC/ P-TABLE 3		CUN	185
		2, -2, KAL(2))		CUN	186
404		CALL REAP(0,2,SUC)		CUN	187
407		CALL REAP(0,0,PT)		CUN	188
	C			CUN	189
	C			CUN	190
413	1850	IF(KAL(9)) 1852,1860,1852		CUN	191
414	1852	SUC(1)=T		CUN	192
416	1854	SUC(2)=0		CUN	193
	C			CUN	194
420	1900	CONTINUE		CUN	195
420		CALL PV		CUN	196
422	1970	GO TO B8		CUN	197
	C1998		CJ	CUN	198
423	1900	CALL HEAD(2LCLJ)		CUN	199
425		CALL REAP (16H CJ RHO-TABLE 3, 0, RUT)		CUN	200
	C			CUN	201
431	1910	CALL CJ		CUN	202
433	1920	GO TO B1		CUN	203
	C1998		TEST	CUN	204
434	2000	CALL TEST		CUN	205
436	2010	GO TO B8		CUN	206
	C2098		CHEC	CUN	207

437	2100	CALL CHEC		CUN	208
441	2110	GO TO 80		CUN	209
	C2198		EMPTY	CUN	210
442	2200	GO TO 80		CUN	211
	C2298		SPEC	CUN	212
443	2200	CALL SPEC		CUN	213
445	2210	GO TO 80		CUN	214
	C2298		SPEC1	CUN	215
446	2400	CALL SPEC1		CUN	216
450	2410	GO TO 80		CUN	217
	C2498		EMPTYIES	CUN	218
451	2500	GO TO 80		CUN	219
	C		CORE	CUN	220
452	2400	E(2)=E(4)		CUN	221
454	2410	E(1)=E(5)		CUN	222
456	2420	CALL CORE (E(3))		CUN	223
461	2430	GO TO 80		CUN	224
	C2498		DEBUG	CUN	225
462	2700	CALL ERP(4HCONS)		CUN	226
465	2710	GO TO 80		CUN	227
	C2798		LOAD	CUN	228
466	2800	GO TO 80		CUN	229
	C2898		EMPTYIES	CUN	230
467	2900	GO TO 80		CUN	231
470	3000	GO TO 80		CUN	232
471	3100	GO TO 80		CUN	233
472	3200	GO TO 80		CUN	234
473	3300	GO TO 80		CUN	235
	C		FORM	CUN	236
474	3400	CALL FIO (3HWOT,4H(A6),1,E(3),0)		CUN	237
502	3410	POL=E(4)-HLANK		CUN	238
504	3420	IF (POL) 3430,3440,3430		CUN	239
505	3430	CALL FIO (5HPRINT,7H(A6),1,E(3),0)		CUN	240
	C			CUN	241
513	3440	IF (E(6)-DOLLAR) 3470,3450,3470		CUN	242
515	3450	DO 3460 I=1,6		CUN	243
522	3460	SPELAB(I)=E(I+6)		CUN	244
524	3470	GO TO 80		CUN	245
	C			CUN	246
	C			CUN	247
	C		REND = END OF RUN	CUN	248
525	3500	GO TO 80		CUN	249
	C		JEND = END OF JOB	CUN	250
526	3600	CONTINUE		CUN	251
526		CALL MEANE (7HJOHENS)		CUN	252
530		CALL EXIT		CUN	253
532	4000	RETURN		CUN	254
	C			CUN	255
	C		LOAD BUTTON	CUN	256
	C			CUN	257
	C			CUN	258
	C			CUN	259
533		END		CUN	260
	C	*****		EQFS	2
	C4	6. OUT OF PLACE		* EQFS	3
	C	*****		EQFS	4
	C4	*****		EQFS	5
	C	BRINKLEY-METHOD EQUILIBRIUM-COMPOSITION PKG.		EQFS	6
	C	TRANSCRIBED TO FORTRAN BY PAUL BIRD, GMX-7.		EQFS	7
	C	FROM FICKEIT'S ORIGINAL LUNGHAND VERSION.		EQFS	8

C	NOTES -	EQPS	9
C	1. CHANGES WHEN INCORPORATED INTO REVISED MES	EQPS	10
C	(MARKED KERSHNER 3/17/70)	EQPS	11
C	A. MAKE AVECT LOCAL, FILLED FROM ARGS EPA, EPA1	EQPS	12
C	IN EQPS	EQPS	13
C	9. EMUL(2) REPLACED BY EMUL(7). IN EQMS	EQPS	14
C	*****	EQPS	15
	SUBROUTINE EQPS(KRP,CSP,QATOM,ALPHA,ALPHA12,EPA,EPA1)	EQPS	16
C		EQPS	17
C		EQPS	18
17	DIMENSION CSP(6),QATOM(6),ALPHA(20,6),AVECT(20,2),RALPHA(101,6),	EQPS	19
	1ALPT(6,101),KRP(2)	EQPS	20
17	DIMENSION QBAR(6),NAVEC(100),XNUMAT(100,6),XNU(100),	EQPS	21
	1QBAR(6),NAVECS(100),XNUMATS(100,6),XNUS(100)	EQPS	22
17	DIMENSION EPA(1),EPA1(1)	EQPS	23
C		EQPS	24
17	COMMON /EQUIR/QBAR,NAVEC,XNUMAT,XNU,SUMQ,NS,NC,ND,NP,NPHI,ND1,	EQPS	25
	1QBAR,NAVECS,XNUMATS,XNUS,SUMS	EQPS	26
C		EQPS	27
C		EQPS	28
C	*****	EQPS	29
C	MAKE AVECT LOCAL. KERSHNER 3/17/70	EQPS	30
C	*****	EQPS	31
17	DO 12 I=1,20	EQPS	32
24	AVECT(I,1)=EPA(I)	EQPS	33
24	AVECT(I,2)=EPA1(I)	EQPS	34
24	12 CONTINUE	EQPS	35
C	DEFINE CONTROL CONSTANTS AND REORDER ALPHA ACCORDING TO A-VECTOR	EQPS	36
33	NC=CSP(1)	EQPS	37
33	NS=CSP(2)	EQPS	38
33	NPHI=CSP(4)	EQPS	39
33	ND=NS-NC	EQPS	40
33	ND1=ND+1	EQPS	41
33	NPHI1=NPHI+1	EQPS	42
45	IF(NPHI1.EQ.1.AND.KRP.EQ.0)GO TO 30	EQPS	43
52	NP=CSP(3)	EQPS	44
54	13 KV=1	EQPS	45
55	14 NCMP=NC-NP	EQPS	46
57	IF(NCMP.LE.0)CALL DEBUG(2)	EQPS	47
62	DO 1 I=1,NS	EQPS	48
73	NAVEC(I)=AVECT(I,KV)	EQPS	49
73	NAV=NAVEC(I)	EQPS	50
74	DO 1 J=1,NC	EQPS	51
111	1 RALPHA(NV,J)=ALPHA(I,J)	EQPS	52
122	DO 2 J=1,NC	EQPS	53
131	2 RALPHA(NS+1,J)=QATOM(J)	EQPS	54
133	CALL MATTRA(NS+1,NC,RALPHA,101,ALPT,6)	EQPS	55
C	TRANSPOSE ALPHA MATRIX	EQPS	56
C	SOLVE FOR NU-MATRIX	EQPS	57
141	CALL LSS(NC,ND1,6,ALPT,ALPT(1,NC+1),DET)	EQPS	58
C	TEST FOR ZERO DETERMINANT. EXIT FOR NEW A-VECTOR	EQPS	59
151	IF(DET.EQ.0.0)CALL DEBUG(2)	EQPS	60
C	TRANSPOSE FOR NU-MATRIX AND SMALL Q	EQPS	61
157	CALL MATTRA(NC,ND+1,ALPT(1,NC+1),6,XNUMAT,100)	EQPS	62
175	SUMQ=0.0	EQPS	63
175	DO 3 J=1,NCMP	EQPS	64
211	3 SUMQ=SUMQ+XNUMAT(NU+1,J)	EQPS	65
214	DO 4 J=1,NC	EQPS	66

232	4	QBAR(J)=XNUMAT(ND+1,J)/SUMQ	EQFS	67
234		DO 5 I=1,ND	EQFS	68
241		XNU(I)=0.0	FQFS	69
243		DO 4 J=1,NCMP	EQFS	70
252	5	XNU(I)=XNU(I)+XNUMAT(I,J)	EQFS	71
	C	PHIN1 NU=MATRIX AND NHAR	EQFS	72
263		WRITE(9,6)(QBAR(J),J=1,NCMP)	EQFS	73
271		WRITE(9,7)(XNUMAT(I,J),J=1,NC)	FQFS	74
	6	FORMAT(1H0,5X,4HQBAR,5X,6E15.7)	EQFS	75
	7	FORMAT(1H0,5X,6HNUMAT,3X,6E15.7)	FQFS	76
	8	FORMAT(10X,13,2X,6E15.7)	EQFS	77
		IF(ND.LF.1)GO TO 90	FQFS	78
317		DO 9 I=2,ND	EQFS	79
321	9	WRITE(9,8)I,(XNUMAT(I,J),J=1,NC)	FQFS	80
323		GO TO (10,15),NPHI1	EQFS	81
352	10	IF(NPHI1.EQ.1.AND.NP.EQ.1)GO TO 11	EQFS	82
360	11	NP=0	EQFS	83
367		KV=2	EQFS	84
370		GO TO 14	EQFS	85
372	15	GO TO (16,10),KFLAG	EQFS	86
373	16	DO 17 I=1,ND	EQFS	87
401		XNUS(I)=XNU(I)	EQFS	88
403		DO 17 J=1,NC	EQFS	89
405	17	XNUMATS(I,J)=XNUMAT(I,J)	EQFS	90
415		XNUS(ND1)=NP	EQFS	91
425		DO 18 I=1,NS	EQFS	92
430	18	NAVECS(I)=NAVEC(I)	EQFS	93
435		SUMUS=SUM(I)	EQFS	94
437		DO 19 J=1,NC	EQFS	95
440	19	WBARS(J)=QBAR(J)	EQFS	96
451		KFLAG=2	EQFS	97
453		GO TO (20,21),NPS	EQFS	98
454	20	NP=0	FQFS	99
465		KV=2	EQFS	100
465		GO TO 22	EQFS	101
467	21	NP=1	EQFS	102
470		KV=1	EQFS	103
472	22	XN1(ND1)=NP	EQFS	104
475		GO TO 14	EQFS	105
475	30	NP=COMP(5)	EQFS	106
475		NPS=NP+1	EQFS	107
501		GO TO (31,33),NPS	EQFS	108
506	31	NP=1	EQFS	109
506		KV=1	EQFS	110
510	32	KFLAG=1	EQFS	111
511		GO TO 14	EQFS	112
512	33	NP=0	EQFS	113
512		KV=2	EQFS	114
514		GO TO 32	EQFS	115
515		END	EQFS	116

		SUBROUTINE EQMS(KBERR,XCOMP,EMOL,FDAG)	FQFS	2
C			EQMS	3
C			EQMS	4
		DATA ITERCYC,EXPLIM,EPSILON/99,600.,1.0E-10/	EQMS	5
C			EQMS	6
12		DIMENSION XCOMP(100),EMOL(7),FDAG(100)	EQMS	7
C		*****	EQMS	8

	C EMCL(2) REPLACED BY EMCL(7). 2/10/76	FUMS	9
	C*****	FUMS	10
12	DIMENSION XLNKI(100),RXCOMP(100),RFDAG(100),XLNXJ(6),A(6,6),F(6),	EQMS	11
	IM(6)	FUMS	12
12	DIMENSION QBAR(6),NAVEC(100),XNUMAT(100,6),XNU(100),	FUMS	13
	UBARS(6),NAVECS(100),XNUMATS(100,6),XNUS(100)	EQMS	14
	C	FUMS	15
12	EQUIVALENCE (F,M)	FUMS	16
	C	FUMS	17
12	COMMON ZEQUIH/QBAR,NAVEC,XNUMAT,XNU,SUMQ,NS,NC,ND,NP,NPHI,ND1,	EQMS	18
	UBARS,NAVECS,XNUMATS,XNUS,SUMS	FUMS	19
	C	FUMS	20
	C	FUMS	21
	C SET CONSTANTS	FUMS	22
12	1000 NPFLAG=1	EQMS	23
13	1001 ITERCO=0	FUMS	24
13	NCMP=NC-10	FUMS	25
	C REORDER MOLE FRACTIONS AND FREE ENERGIES	FUMS	26
16	DO 1 I=1,NS	EQMS	27
23	NAV=NAVEC(I)	EQMS	28
23	RXCOMP(NAV)=XCOMP(I)	FUMS	29
23	1 RFDAG(NAV)=FIDAG(I)	EQMS	30
30	IF(NPHI.EQ.1.AND.NP.EQ.0)RFDAG(NS)=EXPLIM	EQMS	31
	C CALCULATE LNKI	FUMS	32
43	DO 2 I=1,ND	EQMS	33
45	XLNKI(I)=-RFDAG(I+NC)	FUMS	34
50	DO 2 J=1,NC	EQMS	35
57	2 XLNKI(I)=XLNKI(I)+XNUMAT(I,J)*RFDAG(J)	FUMS	36
	C	FUMS	37
	C CALCULATE LN XJ	EQMS	38
67	3 DO 4 J=1,NCMP	FUMS	39
71	4 XLNXJ(J)=ALOG(RXCOMP(J))	EQMS	40
	C CALCULATE MOLE FRACTIONS OF DEPENDENT SPECIES	FUMS	41
102	DO 6 I=1,ND	EQMS	42
103	XLNXI=XLNKI(I)	FUMS	43
105	DO 5 J=1,NCMP	FUMS	44
115	5 XLNXI=XLNXI+XNUMAT(I,J)*XLNXJ(J)	EQMS	45
120	IF(XLNXI.GT.0.0)XLNXI=0.0	FUMS	46
125	IF(XLNXI.LT.-EXPLIM)XLNXI=-EXPLIM	EQMS	47
131	6 RXCOMP(I+NC)=EXP(XLNXI)	FUMS	48
	C SET UP ITERATION LOOP	FUMS	49
143	IF(ITERCO.EQ.0)GO TO 11	EQMS	50
144	IF(ITERCO.GT.ITERCYC)GO TO 20	FUMS	51
	C TEST FOR CONVERGENCE	FUMS	52
147	DO 7 J=1,NCMP	EQMS	53
150	IF(ABS(H(J)).GT.EPSILON)GO TO 11	FUMS	54
155	7 CONTINUE	EQMS	55
	C PASSED CONVERGENCE TEST	FUMS	56
	C	EQMS	57
	C CALCULATE NUMBER OF MOLES	FUMS	58
157	RNCH=1.0	EQMS	59
160	DO 8 I=1,ND	FUMS	60
170	8 RNCH=RNCH+RXCOMP(I+NC)*(XNU(I)-1.0)	EQMS	61
176	EMOL(1)=SUMQ/RNCH	FUMS	62
	C CALCULATE XC AND MOLES OF SOLID FOR NP=1	EQMS	63
176	EMOL(2)=0.0	FUMS	64
201	IF(NP.NE.1)GO TO 81	FUMS	65
203	XC=QBAR(NC)	EQMS	66
205	DO 80 I=1,NC	FUMS	67
220	80 XC=XC-(XNUMAT(I,NC)-UBAR(NC)*(XNU(I)-1.0))*RXCOMP(I+NC)	EQMS	68

231	RXCMP(NC)=XC	FUMS	69
231	EMOL(2)=(C*EMOL(1)	EUMS	70
	C RESTORE MOLE FRACTION ORDER	FUMS	71
234	81 DO 9 I=1,NS	FUMS	72
243	NAV=NAVEC(I)	FUMS	73
243	9 XCMP(I)=RXCMP(NAV)	FUMS	74
247	IF(NPHI.EQ.1)GO TO 22	FUMS	75
	C EXIT WITH COMPUTED EQUILIBRIUM COMPOSITION	FUMS	76
253	10 RETURN	FUMS	77
	C	FUMS	78
	C ENTRY TO CALCULATE CORRECTIONS TO MOLE FRACTIONS	FUMS	79
254	11 DO 13 J=1,NCMP	FUMS	80
256	SUMF=0.0	FUMS	81
257	DO 12 I=1,NO	FUMS	82
272	12 SUMF=SUMF+(XNUMAT(I,J)-QBAR(J)*(XNU(I)-1.0))*RXCMP(I+NC)	FUMS	83
303	13 F(J)=QBAR(J)-RXCMP(J)-SUMF	FUMS	84
311	DO 14 J=1,NCMP	FUMS	85
313	DO 14 JP=1,NCMP	FUMS	86
314	A(I,JP)=0.0	FUMS	87
317	IF(J.EQ.JP)A(J,JP)=RXCMP(J)	FUMS	88
322	DO 14 I=1,NO	FUMS	89
340	14 A(I,JP)=A(J,JP)+(XNUMAT(I,J)-QBAR(J)*(XNU(I)-1.0))*RXCMP(I+NC)*	FUMS	90
	XNUMAT(I,JP)	FUMS	91
357	CALL LSS(4,CMP,1.6,A,F,DET)	FUMS	92
363	IF (DET.EQ.0.0)GO TO 20	FUMS	93
367	DO 17 J=1,NCMP	FUMS	94
370	RXCMP(J)=RXCMP(J)*(1.0+F(J))	FUMS	95
373	IF(RXCMP(J).LT.EPSILON)RXCMP(J)=EPSILON	FUMS	96
377	17 CONTINUE	FUMS	97
402	ITERCC=ITERCC+1	FUMS	98
403	GO TO 3	FUMS	99
404	20 CALL DEBUG(1)	FUMS	100
406	GO TO 1000	FUMS	101
	C TEST FOR PREVIOUS SOLUTION FOR PHI = 1	FUMS	102
411	24 IF(NPHI.EQ.2)GO TO 10	FUMS	103
414	IF(NP.EQ.1)GO TO 40	FUMS	104
	C CALCULATION TEST FOR 1-PHASE SOLUTION	FUMS	105
	C SELECT NON-ZERO ELEMENTS OF 2-PHASE NO	FUMS	106
416	DO 50 I=1,NO	FUMS	107
417	IF(XNUMATS(I,NC).NE.0.0)GO TO 51	FUMS	108
422	50 CONTINUE	FUMS	109
424	CALL DEBUG(2)	FUMS	110
	C LOCATED SPECIES FORMED FROM SOLID	FUMS	111
430	51 ISP=1	FUMS	112
432	DO 52 I=1,NS	FUMS	113
437	NAV=NAVECS(I)	FUMS	114
437	RXCMP(NAV)=XCMP(I)	FUMS	115
437	52 FFDAG(NAV)=FFDAG(I)	FUMS	116
444	ZLNKI=-FFDAG(ISP+NC)	FUMS	117
447	DO 53 J=1,NC	FUMS	118
462	53 ZLNKI=ZLNKI+XNUMATS(ISP,J)*FFDAG(J)	FUMS	119
465	ALNS=ALOG(RXCMP(ISP+NC))-ZLNKI	FUMS	120
472	NCM1=NC-1	FUMS	121
474	DO 54 J=1,NCM1	FUMS	122
500	54 ALNS=XLNS-XNUMATS(ISP,J)*ALOG(RXCMP(J))	FUMS	123
514	EMOL(7)=XLNS	FUMS	124
	C*****	FUMS	125
	C EMOL(7) SFT 2/10/76	FUMS	126
	C*****	FUMS	127
	C TEST FOR SUPERSATURATION	FUMS	128

515	IF (ALNS.LT.0.0)GO TO 10	FGPS	129
	C EXCHANGE FOR 2-PHASE SOLUTION	EGPS	130
	C	FGPS	131
	C EXCHANGE A-VECTORS, ETC., FOR CHANGE IN NUMBER OF PHASES	EGPS	132
515	30 NPHFLAG=2	EGPS	133
517	DO 31 I=1,N0	FGPS	134
521	DO 31 J=1,NC	FGPS	135
530	XNUMSV=XNUMATS(I,J)	FGPS	136
530	XNUMATS(I,J)=XNUMAT(I,J)	FGPS	137
530	31 XNUMAT(I,J)=XNUMSV	FGPS	138
541	DO 32 J=1,NC	FGPS	139
540	QBARSV=QBARS(J)	EGPS	140
540	QBARS(J)=QBARSV	FGPS	141
540	32 QBARS(J)=QBARSV	FGPS	142
551	DO 33 I=1,N3	FGPS	143
561	NAV=NAVECS(I)	EGPS	144
561	NAVECS(I)=NAVEC(I)	FGPS	145
561	33 NAVEC(I)=NAV	EGPS	146
564	DO 34 I=1,N01	EGPS	147
574	XNUMSAV=XNUMS(I)	EGPS	148
574	XNUMS(I)=XNUM(I)	EGPS	149
574	34 XNUM(I)=XNUMSAV	EGPS	150
577	SUMMSAV=SUMMS	FGPS	151
577	SUMMS=SUM(I)	FGPS	152
577	SUMG=SUMMSAV	EGPS	153
577	NP=XNUM(N01)	FGPS	154
605	GO TO 1001	FGPS	155
	C TEST FOR SATISFACTORY 2-PHASE SOLUTION	EGPS	156
	C +0 IF (XC.GT.0.0)GO TO 10	FGPS	157
	C SIML. 40 REPLACED BY THE FOLLOWING TWO STATEMENTS.	EGPS	158
	C KERSHAER 2/10/76	FGPS	159
610	40 EMOL(7)=XC	EGPS	160
612	IF (XC.GT.0.0)GO TO 10	EGPS	161
	C NO SOLID PHASE. GO TO 1-PHASE SOLUTION	FGPS	162
614	GO TO 30	EGPS	163
614	END	FGPS	164

	SUBROUTINE MATTRA(N,M,A,IA,B,IB)	MATTRA	2
16	DIMENSION A(IA,M),B(IB,N)	MATTRA	3
16	DO 1 J=1,M	MATTRA	4
17	DO 1 I=1,N	MATTRA	5
20	1 B(J,I)=A(I,J)	MATTRA	6
37	RETURN	MATTRA	7
40	END	MATTRA	8

	SUBROUTINE LSS (N,M,I,A,B,DET)	LSS	2
	C MODIFIED FOR FORTRAN IV MUG	LSS	3
16	DIMENSION A(I,N), B(I,M)	LSS	4
16	DOUBLE PRECISION S1,S2,CU,PRU	LSS	5
16	IN=N	LSS	6
16	MM=M	LSS	7
16	SN=1.	LSS	8
21	DO 9 J=1,NN	LSS	9
23	L=J-1	LSS	10
24	IF (J.EQ.NN) GO TO 7	LSS	11
31	T=ABS(A(J,J))	LSS	12
31	M1=J	LSS	13
31	M2=J+1	LSS	14

34		DO 1 K=M2,NN	LSS	15
35		A=ABS(A(K,J))	LSS	16
41		IF (X.LE.T) GO TO 1	LSS	17
44		T=X	LSS	18
44		M1=K	LSS	19
46	1	CONTINUE	LSS	20
51		IF (M1.EQ.J) GO TO 4	LSS	21
53		DO 2 K=1,MM	LSS	22
63		T=A(J,K)	LSS	23
63		A(J,K)=A(M1,K)	LSS	24
63	2	A(M1,K)=T	LSS	25
67		SN=-SN	LSS	26
70		IF (MM.E.0) GO TO 4	LSS	27
76		DO 3 K=1,MM	LSS	28
106		T=B(J,K)	LSS	29
106		B(J,K)=B(M1,K)	LSS	30
106	3	B(M1,K)=T	LSS	31
116	4	IF (A(J,J).EQ.0.) GO TO 13	LSS	32
122		DO 6 K=M2,NN	LSS	33
124		S1=0.	LSS	34
124		S2=0.	LSS	35
127		IF (L.E.N.) GO TO 5	LSS	36
130		S1=OUTPRO(L,A(J,1),I,A(1,N),1)	LSS	37
150	5	A(J,K)=(A(J,K)-S1)/A(J,J)	LSS	38
177		S2=OUTPRO(J,A(K,1),I,A(1,M2),1)	LSS	39
217	6	A(K,M2)=(A(K,M2)-S2	LSS	40
232	7	IF (MM.LE.0) GO TO 9	LSS	41
234		IF (A(J,J).EQ.0.) GO TO 13	LSS	42
240		DO 8 K=1,MM	LSS	43
241		S1=0.	LSS	44
242		IF (L.E.N.) GO TO 8	LSS	45
243		S1=OUTPRO(L,A(J,1),I,B(1,K),1)	LSS	46
263	8	B(J,K)=(B(J,K)-S1)/A(J,J)	LSS	47
315	9	CONTINUE	LSS	48
320		DET=A(1,1)*SN	LSS	49
321		IF (DET.EQ.0.) GO TO 13	LSS	50
322		IF (N.EG.1) GO TO 15	LSS	51
324		DO 10 J=2,NN	LSS	52
332	10	DET=DET*A(J,J)	LSS	53
335		IF (DET.EQ.0.) GO TO 13	LSS	54
341		IF (MM.E.0) GO TO 15	LSS	55
342		M3=NN-1	LSS	56
344		DO 12 J=1,MM	LSS	57
346		DO 11 L=1,M3	LSS	58
347		M1=NN-L	LSS	59
347		S1=0.	LSS	60
347		M2=M1+1	LSS	61
347		N=NN-M2+1	LSS	62
355		S1=OUTPRO(K,A(M1,M2),I,B(M2,J),1)	LSS	63
374	11	B(M1,J)=B(M1,J)-S1	LSS	64
407	12	CONTINUE	LSS	65
411		GO TO 15	LSS	66
412	13	DET=0.0	LSS	67
413	15	RETURN	LSS	68
414		END	LSS	69

14	DOUBLE FUNCTION OUTPRO(N,X,IX,Y,IY)	OUTPRO	2
14	DIMENSION X(IX,N),Y(IY,N)	OUTPRO	3
14	DOUBLE OX,DY,SUM	OUTPRO	4

14	SUM=0.0	COIPRO	5
15	DO 1 I=1,N	COIPRO	6
24	UX=X(1,I)	COIPRO	7
24	UY=Y(1,I)	COIPRO	8
24	1 SUM=SUM+UX*UY	COIPRO	9
46	DOTPRG=SUM	COIPRO	10
50	RETURN	COIPRO	11
52	END	COIPRO	12

	SUBROUTINE REAP(LABEL,N,A)	REAP	2
	C*****	REAP	3
	C THIS ROUTINE IS DESIGNED TO READ AND PRINT SPECIFIED	REAP	4
	C ARRAYS.	REAP	5
	C	REAP	6
	C KERSHNER 2/13/76	REAP	7
10	C*****	REAP	8
	10 DIMENSION LABEL(10),A(N)	REAP	9
	C*****	REAP	10
	C FORMAT STATEMENTS.	REAP	11
	C*****	REAP	12
	10 FORMAT(12I6)	REAP	13
	20 FORMAT(6E12.7)	REAP	14
	30 FORMAT(5X,12I8)	REAP	15
	40 FORMAT(5X,1P5E13.5)	REAP	16
	50 FORMAT(2X,1G10)	REAP	17
10	CALL PRINT(LABEL,0,0)	REAP	18
	C*****	REAP	19
	C THEN BRANCH ON N TO READ AND PRINT ARRAY A.	REAP	20
	C*****	REAP	21
12	IF(N)100,110,120	REAP	22
	C*****	REAP	23
	C NEGATIVE N, USE 12I6 FORMAT.	REAP	24
	C*****	REAP	25
15	100 CONTINUE	REAP	26
15	NP=-N	REAP	27
16	READ(10,10)(A(I),I=1,NP)	REAP	28
26	PRINT 10,(A(I),I=1,NP)	REAP	29
40	RETURN	REAP	30
	C*****	REAP	31
	C ZERO N, STOP AFTER READING BLANK FIELD.	REAP	32
	C*****	REAP	33
41	110 CONTINUE	REAP	34
41	J=1	REAP	35
41	K=6	REAP	36
43	120 READ(10,20)(A(I),I=J,K)	REAP	37
55	DO 130 L=J,K	REAP	38
61	IF(A(L).EQ.0.0)GO TO 140	REAP	39
62	130 CONTINUE	REAP	40
64	PRINT 40,(A(I),I=J,K)	REAP	41
75	J=K+1	REAP	42
76	K=J+5	REAP	43
101	GO TO 120	REAP	44
104	140 A(L)=0.0	REAP	45
106	PRINT 40,(A(I),I=J,L)	REAP	46
120	RETURN	REAP	47
	C*****	REAP	48
	C POSITIVE N, USE E12.7 FORMAT.	REAP	49
	C*****	REAP	50
121	150 CONTINUE	REAP	51
121	READ(10,20)(A(I),I=1,N)		

14	SUM=0.0	COIPRO	5
15	DO 1 I=1,N	COIPRO	6
24	UX=X(1,I)	COIPRO	7
24	UY=Y(1,I)	COIPRO	8
24	1 SUM=SUM+UX*UY	COIPRO	9
45	DOTPRC=SUM	COIPRO	10
50	RETURN	COIPRO	11
52	END	COIPRO	12

	SUBROUTINE REAP(LABEL,N,A)	REAP	2
	C*****	REAP	3
	C THIS ROUTINE IS DESIGNED TO READ AND PRINT SPECIFIED	REAP	4
	C ARRAYS.	REAP	5
	C	REAP	6
	C*****	REAP	7
10	DIMENSION LABEL(10),A(N)	REAP	8
	C*****	REAP	9
	C FORMAT STATEMENTS.	REAP	10
	C*****	REAP	11
	10 FORMAT(1P16)	REAP	12
	20 FORMAT(AE12.7)	REAP	13
	30 FORMAT(5X,1P18)	REAP	14
	40 FORMAT(5X,1P5E13.5)	REAP	15
	50 FORMAT(2X,10A10)	REAP	16
10	CALL PRIN (LABEL,0,0)	REAP	17
	C*****	REAP	18
	C THEN BRANCH ON N TO READ AND PRINT ARRAY A.	REAP	19
	C*****	REAP	20
12	IF (N)100,110,120	REAP	21
	C*****	REAP	22
	C NEGATIVE N, USE 1216 FORMAT.	REAP	23
	C*****	REAP	24
15	100 CONTINUE	REAP	25
15	NP=-N	REAP	26
16	READ (10,10) (A(I),I=1,NP)	REAP	27
26	PRINT 10, (A(I),I=1,NP)	REAP	28
40	RETURN	REAP	29
	C*****	REAP	30
	C ZERO N, STOP AFTER READING BLANK FIELD.	REAP	31
	C*****	REAP	32
41	110 CONTINUE	REAP	33
41	J=1	REAP	34
41	K=6	REAP	35
43	120 READ(10,20) (A(I),I=J,K)	REAP	36
55	DO 130 L=J,K	REAP	37
61	IF (A(L).EQ.0.0) GO TO 140	REAP	38
62	130 CONTINUE	REAP	39
64	PRINT 40, (A(I),I=J,K)	REAP	40
74	J=K+1	REAP	41
76	K=J+5	REAP	42
101	GO TO 120	REAP	43
104	140 A(L)=0.0	REAP	44
106	PRINT 40, (A(I),I=J,L)	REAP	45
120	RETURN	REAP	46
	C*****	REAP	47
	C POSITIVE N, USE E12.7 FORMAT.	REAP	48
	C*****	REAP	49
121	150 CONTINUE	REAP	50
121	READ(10,20) (A(I),I=1,N)	REAP	51

131		PRINT 40,(A(I),I=1*N)	LEAP	52
143		RETURN	LEAP	53
144		END	LEAP	54
	C	*****	DUMMY	2
	C	7. DUMMIES	DUMMY	3
	C	*****	DUMMY	4
		SUBROUTINE DOUT	DUMMY	5
	C	THIS IS A DUMMY ROUTINE.	DUMMY	6
1		RETURN	DUMMY	7
2		END	DUMMY	8
		SUBROUTINE DIPI	DUMMY	9
	C	THIS IS A DUMMY ROUTINE.	DUMMY	10
1		RETURN	DUMMY	11
2		END	DUMMY	12
		SUBROUTINE TEST	DUMMY	13
	C	THIS IS A DUMMY ROUTINE.	DUMMY	14
1		RETURN	DUMMY	15
2		END	DUMMY	16
		SUBROUTINE CHEC	DUMMY	17
	C	THIS IS A DUMMY ROUTINE.	DUMMY	18
1		RETURN	DUMMY	19
2		END	DUMMY	20
		SUBROUTINE SPEC	DUMMY	21
	C	THIS IS A DUMMY ROUTINE.	DUMMY	22
1		RETURN	DUMMY	23
2		END	DUMMY	24
		SUBROUTINE SPEC1	DUMMY	25
	C	THIS IS A DUMMY ROUTINE.	DUMMY	26
1		RETURN	DUMMY	27
2		END	DUMMY	28
		SUBROUTINE CORE	DUMMY	29
	C	THIS IS A DUMMY ROUTINE.	DUMMY	30
1		RETURN	DUMMY	31
2		END	DUMMY	32
		SUBROUTINE DOM	DUMMY	33
	C	THIS IS A DUMMY ROUTINE.	DUMMY	34
1		RETURN	DUMMY	35
2		END	DUMMY	36
	C	CZZ	CZZ	2

APPENDIX D
COMMON STORE

The contents of the common arrays are listed in Table D-I.

•General Notes

- (1) If there is a principal routine dealing with an array, its name is given in parentheses at the end of the description line.
- (2) A few important equivalent names are given; these are denoted by a preceding equals sign.
- (3) A single subscript indicates a one-dimensional array (for example x_i); a double subscript indicates a two-dimensional array.
- (4) One-dimensional arrays containing species properties or compositions for the entire system list the solid as the first species. The mole fraction of the solid is $x_s = n_s/n$.
- (5) Unless otherwise stated, the units are cm-g- μ s or cm-mol- μ s.
- (6) Unless otherwise stated, all derivatives for the system are at chemical equilibrium.

•Particular Notes

- (1) GM - the prime here denotes imperfection quantities with respect to ideal gas at the same temperature and volume. See Sec. IV.C.
- (2) THER - the subscript o on quantities near the end of the array denotes a frozen-composition derivative.

TABLE D-I
COMMON STORE

CAR - matrix of FROOT arrays (columns)	DER - differentiation (GAMM)
1. CC - CJ	1. p
2. CH - Hugoniot	2. v
3. CM - constant-v, s, e contours	3. T
4. CG - gas EOS	4. v ₊
5. CS - solid EOS	5. v ₋
	6. H ₊
	7. H ₋
CONT - constants	
1. 1.98719 R(cal)	
2. 831439×10^{-5} R(Mbar-cm ³ /g)	EMG - \tilde{F}_i , "free energies" for equilibrium constants (EQMS)
3. 1.01325×10^{-6} atm to Mbar	
4. 0.04184 kcal to Mbar-cm ³	
5. $0.426012 (N/\sqrt{2}) \times 10^{-24}$	

EMN - phase mole numbers

1. n_g
2. n_s
3. $n = n_g + n_s$
4. $x_g = n_g/n$
5. $x_s = n_s/n$
6. n/M_0 (moles/gram)
7. $\ln \bar{s}$ (saturation index) or $-n_s$
(all solid evaporated)

EMX - x_j , mole fractions

FMU - μ_j' , imperfection chemical potentials

FN - n_j , mole numbers

FOB - knobs

- 1-6. FROOT ϵ 's
- 7-12. FROOT r 's
13. $\Delta_1 = \Delta \ln p$ (GAMM)
14. $\Delta_2 = \Delta T$ (GAMM)
15. ϵ , equilibrium outer (EQP)
16. ϵ , equilibrium inner (EQP)
- 17,18. ---
- 19-36. FROOT x_{\min} , x_{\max} in pairs

GM - pure-fluid gas state (sub g) (GEM)

1. $\tau = v/v^*$
2. $\theta = T/T^*$
3. $z = pV/RT$
4. E'/RT
5. F'/RT
6. $(z\theta)_\theta$
7. τz_τ
8. C_v/R
9. $z - RT/p$
10. $z-1$
11. S'/R
12. $(\partial p/\partial V)_T$
13. $(\partial p/\partial T)_V$
14. $(\partial V/\partial T)_p$
15. v
16. p
17. H'/RT
18. $(z-1)_\theta = \tau \chi_\tau/\theta$
19. $(E'/RT)_\theta = -\chi/\theta$
20. A'/RT
21. $V_f/V = 2\pi\sqrt{2} g(1)$ (V_f = free volume)
22. $b/2$ (integration limit)
23. ---

24. ---
25. γ
26. $p^{-1} (\partial E/\partial V)_p$
27. $1/\Gamma$
28. $-(\partial \ln p/\partial \ln V)_T$
29. C_p/R
30. $(\partial \ln V/\partial T)_p$

GP - gas EOS (GEM)

1. n
2. m
3. A_n
4. A_m
5. $r^* = RSTA$
6. $T^* = TSTA$
7. $V^* = VSTA$

HE - initial (unreacted) state (CON)

1. ρ_0 (g/cm³)
2. p_0 (Mbar)
3. T_0 (K)
4. M_0 (g/mole)
5. ΔH_{f_0} (kcal/mole relative to elements at T_0)
6. $v_0 = 1/\rho_0$
7. $h_0(T_0;T_0) = (n/M_0) \Delta H_{f_0}$
8. $e_j = \frac{1}{2} u_j^2$

KAL - option switches, see CON, SWIT

1. equilibrium differentiation
2. fixed composition differentiation
3. gas (0/9/other: ideal/KW/LJD)
4. solid (0 for incompressible)
5. mix 0 no-mix 3 - CS
1 ideal 4 One-Fluid
2 LH
6. composition (0/1 for fixed, equilibrium)
7. CJ (0/1 for equilibrium/frozen)
8. contour (1, 2, 3, 4 for constant-T, v, s, e)
9. T_c, p_c choice (0/1 for input/previous)
10. $z - 1$
11. punch output if $\neq 0$

KEN - entry and iteration counts

KIM - sizes

1. r = KR number of gas species
2. s = KS total number of species
3. c = KC number of elements
4. n = KN degree of ideal-function fit

KON - triggers and diagnostic switches

PT - input pressure table (PV, TED)

ROT - input ρ_0 table (CJ)

SM - solid state (sub s) (SEMS)

1. V
2. E'/RT
3. H'/RT
4. A'/RT
5. F'/RT
6. S'/R
7. $z = pV/RT$
8. p
9. $V/V_0 = Y$
10. T
11. T_1

SP - solid EOS (SEMS)

1. Γ
2. C_p/R
3. α
4. V_0
5. T_0
6. E_0/RT_0
7. ---
- 8-12. c_0 - c_4 - Hugoniot fit
- 13-20. working store

SUC - contour initial state (PV)

1. T_C
2. p_C
3. V_C
4. S_C
5. E_C

SUCG - derivatives working store (GAMM)

1. γ^{-1}
2. $p^{-1} (\partial e / \partial v)_p$
3. $1/\Gamma$
4. c
5. CJ function $j(p)$ [see THER (28)]
6. $-(\partial \ln p / \partial \ln v)_T$

7. C_p/R
8. $(\partial \ln v / \partial \ln T)_p$

THER - system state (COU)

1. p
2. v/v_0
3. T
4. u
5. D
6. q (Mbar - cm^3/g)
7. q (kcal/g)
8. v
9. e
10. h
11. a
12. f
13. s
14. $H(T;T_0)/RT$ - relative to elements at T_0
15. V
16. E/RT
17. H/RT
18. A/RT
19. F/RT
20. S/R
21. $z = pV/RT$
22. γ
23. $p^{-1} (\partial e / \partial v)_p$
24. $1/\Gamma$
25. c
26. γ_0 (frozen)
27. $j(p)$ equilibrium
28. $j(p)$ frozen
where $j(p)$ is the CJ function:

$$j(p) = \left\{ v/v_0 \left[(\gamma+1 - p_0/p) / \gamma \right] \right\}^{-\gamma}$$

29. c_0 (frozen)
30. $p^{-1} (\partial e / \partial v)_p$ frozen

TMG - F_i^j - ideal free energies

TMS - ideal functions (super i) (TIMS)

1. E_g/RT
 2. H_g/RT
 3. C_g/R
 4. S_g/R
 5. $\Delta_g(T_0)$
 6. $H_g(T;T_0)/RT$
 7. H_s/RT
 8. C_s/R
 9. S_s/R
 10. F_s/RT
 11. $\Delta_s(T_0)$
 12. $H_s(T;T_0)/RT$
- } relative to elements at T_0
- } relative to elements at T_0

TP - CON, TIP strings 3 ..., one row per species

XMT - gas mixture state (sub g) (XIM)

1. V
2. E'/RT
3. H'/RT
4. A'/RT
5. F'/RT
6. S'/R
7. $z-1$
8. $V-RT/p$
9. $\sum x_i x_j T_{ij}^*/T_r^*$ (for LH mix)
10. $\sum x_i x_j r_{ij}^*/r_r^*$ (for LH mix)
11. r_r^* (for LH mix)
12. T_r^* (for LH mix)
13. n (for One-Fluid mix)
14. m (for One-Fluid mix)
15. V_c^* (for One-Fluid mix)
16. $\bar{r}^* = RSTAT$ (from XIMS)
17. $\bar{T}^* = TSTAT$ (from XIMS)
18. $\bar{V}^* = VSTAT$ (from XIMS)

XMU μ_i'/RT , gas species only (XIM)

- XPF - T_{ij}^* (XIM)
- XPG - r_{ij}^* (XIM)
- XPR - r_i^* (XIM)
- XPT - T_i^* (XIM)

REFERENCES

1. W. Fickett, "Calculation of the Detonation Properties of Condensed Explosives," Phys. Fluids 6, 997-1006 (1963).
2. W. Fickett, "Detonation Properties of Condensed Explosives Calculated with an Equation of State Based on Intermolecular Potentials," Los Alamos Scientific Laboratory report LA-2712 (December 1962).
3. S. J. Jacobs, "Energy of Detonation," Naval Ordnance Laboratory report NAVORD 4366 (September 1956).